



**UNIVERSIDADE ESTADUAL DO CEARÁ
REDE NORDESTE DE BIOTECNOLOGIA
PROGRAMA DE PÓS-GRADUAÇÃO EM BIOTECNOLOGIA
DOUTORADO EM BIOTECNOLOGIA**

LUANA CARVALHO DA SILVA

**MICROCÁPSULAS DE ÓLEO DE PEQUI OBTIDAS POR COACERVAÇÃO
COMPLEXA: CARACTERIZAÇÃO, LIBERAÇÃO CONTROLADA E APLICAÇÃO
EM IOGURTE**

**FORTALEZA - CEARÁ
2021**

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IOGURTE

Tese apresentada ao Doutorado em Biotecnologia do Programa de Pós-graduação em Biotecnologia da Rede Nordeste de Biotecnologia da Universidade Estadual do Ceará, como requisito parcial para obtenção do título de doutora em Biotecnologia. Área de concentração: Recursos Naturais.

Orientador: Prof. Dr. Carlucio Roberto Alves

Co-orientadora: Profa. Dra. Roselayne Ferro Furtado

FORTALEZA - CEARÁ

2021

Dados Internacionais de Catalogação na Publicação
Universidade Estadual do Ceará
Sistema de Bibliotecas

Silva, Luana Carvalho da.

Microcápsulas de óleo de pequi obtidas por coacervação complexa: caracterização, liberação controlada e aplicação em iogurte [recurso eletrônico] / Luana Carvalho da Silva. - 2021.
143 f. : il.

Tese (DOUTORADO ACADÊMICO) - Universidade Estadual do Ceará, Faculdade de Veterinaria, Curso de Programa de Pós-graduação Em Biotecnologia Rede Nordeste de Biotecnologia, Fortaleza, 2021.

Orientação: Prof. Dr. Carlucio Roberto Alves.
Coorientação: Profª. Dra. Roselayne Ferro Furtado.

1. Óleo de pequi. 2. Goma de cajueiro. 3. Quitosana. 4. Gelatina. 5. Microencapsulação. 6. Iogurte. 7. Beta-caroteno. I. Título.

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Aprovada em: 16 de dezembro de 2021

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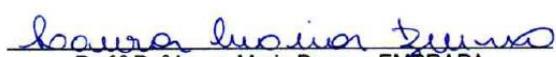
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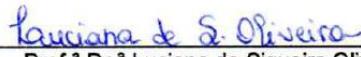
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AGRADECIMENTOS

À Deus pelo dom da minha vida e por me dar força e sustento nos momentos difíceis.

Ao meu orientador Prof. Dr. Carlucio Roberto Alves, pela orientação, compreensão e apoio durante todo este trabalho. Sua atenção e incentivo foram fundamentais para me impulsionar durante o doutorado.

À minha co-orientadora Dra. Roselayne Ferro Furtado, por toda sua contribuição durante minha vida acadêmica, conselhos e ensinamentos. Grata imensamente por toda paciência e incentivo, a senhora sempre servirá como inspiração por ser uma excelente pessoa e profissional.

Aos membros da banca examinadora, Profa. Dra. Luciana de Siqueira Oliveira, Profa. Dra. Selene Daiha Benevides, Profa. Dra. Luana Guabiraba Mendes e Profa. Dra. Laura Maria Bruno, por ter aceitado e concedido seu tempo para a correção deste trabalho.

À Universidade Estadual do Ceará, em especial ao programa de Pós-Graduação em Biotecnologia, pela oportunidade de realização deste doutorado.

As pesquisadoras do Laboratório de Embalagens-EMBRAPA, Dra. Selene Daiha Benevides e Dra. Maria do Socorro Rocha Bastos, pelos ensinamentos transmitidos.

À Embrapa por viabilizar meus estudos e pesquisa e aos técnicos, analistas e pesquisadores da Embrapa Agroindústria Tropical - CNPAT, em especial o Hilton, Márcia, Ionete e Adriano, pelos ensinamentos e disponibilidade dos equipamentos necessários para execução do projeto.

À Funcap, pelo apoio financeiro concedido.

Aos meus pais, Custódio Domingos e Maria de Fátima, os meus irmãos, sobrinhos, tios, primos e meus cachorros, por sempre estarem presentes em minha vida, pelo apoio incondicional e por sempre acreditarem em mim.

Aos meus companheiros do Laboratório de Embalagens Tiago, Nadya, Nayanne, Amanda, Marília, Lêonia, Maryana, pela companhia e ajuda, mesmo que indiretamente, ao decorrer do doutorado. Obrigada por serem uma família, fazendo com que os dias de laboratório sejam gratificantes. Em especial, grata pela linda amizade e parceria da Rachel, Gabi e Joana, que ajudaram na elaboração desta tese.

Aos meus amigos, principalmente Amilcar, Victor, Dayana, Karla Larissa, Neto, Ítalo e Bianca pela amizade e pelas palavras de apoio no decorrer desta pesquisa. Em especial, agradeço minha amiga Jasmille pela realização da arte das figuras no artigo de revisão.

A todos que não foram citados, mas que contribuíram de forma direta e indireta nesta pesquisa.

RESUMO

A adição de óleo vegetal em iogurte, como o óleo de pequi (*Caryocar coriaceum* Wittm.), tem se destacado para as indústrias alimentícias por estar associado ao aumento dos teores de ácidos graxos insaturados e adições de bioativos inexistentes, como os carotenoides. A microencapsulação pode ser usada para mascarar o forte sabor do óleo de pequi, além de proteger os compostos bioativos e promover sua liberação controlada. Por isso, o objetivo desse trabalho é caracterizar as microcápsulas de óleo de pequi, obtidas por coacervação complexa, utilizando como materiais de parede a goma de cajueiro/quitosana e goma de cajueiro/gelatina, e avaliar sua aplicação em iogurte. Ambos os materiais de parede obtiveram bons resultados em eficiência de encapsulamento (>80%), rendimento (> 50%) e capacidade de carga (<50%). O infravermelho por transformada de Fourier (FTIR) comprovou a interação eletrostática dos coacervados, confirmando a eficácia da encapsulação. As análises termogravimétricas (TGA) e calorimetria exploratória diferencial (DSC), além de Rancimat, mostraram a estabilidade da microcápsula. As microcápsulas apresentaram melhor resistência à desintegração na faixa de pH de 4 a 5 e em temperaturas abaixo de 80 °C, sendo assim foi escolhida a matriz alimentar de iogurte para aplicação das microcápsulas. A presença do óleo de pequi levou ao um aumento significativo de ácidos graxos insaturados no perfil de ácidos graxos do iogurte, e a etapa de resfriamento do iogurte a mais adequada para adição das microcápsulas. Posteriormente, foi avaliada a influência das microcápsulas de óleo de pequi nas análises de pH, sólidos totais, sinérese, cor, morfologia, textura e viscosidade, durante o tempo de armazenamento de 28 dias. Nos 28 dias de armazenamento, os valores de pH diminuíram de 4,5 para 4,32 para todas as formulações, mas os valores de sólidos totais aumentaram (>11%) e a sinérese diminuiu (<50%) devido à retenção de água causada pelos biopolímeros das microcápsulas. No perfil de liberação pela digestão *in vitro*, houve uma liberação gradativa do óleo, fato que aumentou a bioacessibilidade do beta-caroteno. Com isso, conclui-se que as microcápsulas de goma de cajueiro/quitosana proporcionaram uma matriz mais densa, protegendo melhor o óleo, e ao aplicar em iogurte, melhorou o perfil de ácidos graxos e promoveu a adição de um importante composto bioativo, o beta-caroteno, sendo que as formulações com as microcápsulas obtiveram melhor estabilidade e bioacessibilidade do beta-caroteno.

Palavras-chaves: Óleo de pequi; Goma de cajueiro; Quitosana; Gelatina; Microencapsulação; Iogurte; Beta-caroteno.

ABSTRACT

The addition of vegetable oil to yogurt, such as pequi oil (*Caryocar coriaceum* Wittm.), has stood out for the food industries because it is associated with an increase in unsaturated fatty acids and non-existent additions of bioactive, such as carotenoids. Microencapsulation can be used to mask the strong flavor of pequi oil, in addition to protecting bioactive compounds and promoting their controlled release. Therefore, the objective of this work is to characterize pequi oil microcapsules, obtained by complex coacervation, using cashew gum/chitosan and cashew gum/gelatin as wall materials, and to evaluate their application in yogurt. Both wall materials had good results in encapsulation efficiency (>80%), yield (>50%), and load capacity (<50%). Fourier transform infrared (FTIR) confirmed the electrostatic interaction of coacervates, confirming the efficacy of encapsulation. Thermogravimetric analysis (TGA) and differential scanning calorimetry (DSC), in addition to Rancimat, showed the stability of the microcapsule. The microcapsules showed better resistance to disintegration in the pH range from 4 to 5 and at temperatures below 80 °C, so the yogurt food matrix was chosen for application of the microcapsules. The presence of pequi oil led to a significant increase in unsaturated fatty acids in the fatty acid profile of yogurt, and the yogurt cooling step was the most suitable for the addition of microcapsules. Subsequently, the influence of pequi oil microcapsules in the analysis of pH, total solids, syneresis, color, morphology, texture, and viscosity, during a storage time of 28 days, was evaluated. At 28 days of storage, pH values decreased from 4.5 to 4.32 for all formulations, but total solids values increased (>11%) and syneresis decreased (<50%) due to water retention caused by the biopolymers of the microcapsules. In the release profile by in vitro digestion, there was a gradual release of oil, a fact that increased the bioaccessibility of beta-carotene. Thus, it is concluded that the microcapsules of cashew gum/chitosan provided a denser matrix, better protecting the oil, and when applied to yogurt, it improved the fatty acid profile and promoted the addition of an important bioactive compound, beta-carotene, and the formulations with microcapsules had better stability and bioaccessibility than beta-carotene.

Keywords: Pequi oil; Cashew gum; Chitosan; Gelatin; Microencapsulation; Yogurt, Beta-carotene.

LISTA DE ILUSTRAÇÕES

Figura 1 –	Pequizeiro (<i>Caryocar coriaceum</i> Wittm.).....	18
Figura 2 –	Constituição esquemática do pequi (fruto).....	19
Figura 3 –	(A) Óleo extraído da polpa do pequi e (B) estrutura química do beta-caroteno.....	22
Figura 4 –	(A) Esquema representativo, onde (A) é interação eletrostática para formação das microcápsulas pela técnica de coacervação complexa e (B) é a precipitação dos coacervados. (C) Imagem real dos coacervados formados e (D) micrografias das microcápsulas formadas.....	24
Figura 5 –	(A) Exsudato (goma bruta), (B) polissacarídeo isolado (goma de cajueiro) e (C) principais estruturas químicas constituintes.....	30
Figura 6 –	(A) Quitosana obtida pela desasetilação da quitina e (B) estrutura química da quitina e da quitosana.....	35
Capítulo I		
Figure 1 –	Representative scheme for the spray drying microencapsulation process, where: 1) feeder; 2) magnetic stirrer; 3) peristaltic pump; 4) hot air/gas inlet; 5) atomizer nozzle; 6) drying chamber; 7) gas extractor; 8) cyclone; and 9) particle collector.....	44
Figure 2 –	Representative scheme for the complex coacervation process, where: 1) oil dispersed in the emulsion; 2) first solubilized polymer; 3) second solubilized polymer; 4) pH adjustment; 5) refrigeration; and 6) precipitation of coacervates.....	47
Figure 3 –	Representative scheme for the ionic gelation process, where: 1) syringe; 2) emulsion (polymer + active material); 3) cross-linking solution; 4) microparticles; 5) magnetic stirrer; and 6) microparticle wall formation.....	49
Figure 4 –	Representative scheme for the electrostatic layer-by-layer process, where: 1) water; 2) oil; 3) agitation; 4) emulsifier; 5) primary emulsion; 6) polymer I; 7) secondary emulsion; 8) polymer II; and 9) tertiary emulsion.....	50

Figure 5 –	Representative scheme for microencapsulation by polymerization: I) interfacial, where: 1) aqueous solution (hydrophilic phase); 2) monomer B; 3) monomer A; 4) oil (lipophilic phase); 5) diffusion of monomers to the interface; and 6) polymerization reaction and matrix formation. II) <i>in situ</i> , where 1') monomer B; 2') monomer A; 3') aqueous solution (hydrophilic phase); 4') oil (lipophilic phase); 5') dissolving the monomers in the continuous phase; and 6) polymerization reaction and matrix formation.....	53
Capítulo II		
Figure 1 –	Flowchart representative of the preparation of yogurts enriched with microencapsulated pequi oil added in different stages.....	78
Figure 2 –	Transmission electron microscopy (TEM) micrographs of the microcapsules, where A and C correspond to CCP (cashew gum/chitosan-pequi oil) microcapsules, and B and D correspond to CGP (cashew gum/gelatin-pequi oil) microcapsules. Scanning electron microscopy (SEM) micrographs of the microcapsules are given in E and G corresponding to CCP microcapsules, and F and H corresponding to CGP microcapsules.....	81
Figure 3 –	FT-IR spectra for A) cashew gum (CG), chitosan (CT), pequi oil (PO), cashew gum/chitosan (CG/CT) and cashew gum/chitosan-pequi oil (CCP); B) CG, gelatin (GE), PO, cashew gum/gelatin (CG/GE) and cashew gum/gelatin-pequi oil (CGP).....	83
Figure 4 –	(A) Weight loss (%) over time (°C); B) derivative weight loss (mg/min) over time (°C), for microcapsules of cashew gum/chitosan (CG/CT) and cashew gum/gelatin (CG/GE), and pequi oil (PO); C) Thermograms of cashew gum/chitosan-pequi oil (CCP) and cashew gum/gelatin-pequi oil (CGP) microcapsules, and PO where degradation temperature ranges (ΔT_d), degradation temperature peaks (T_d), and degradation enthalpies (ΔH_d) were calculated; D) Oxidation curves (conductivity versus time) were obtained from Rancimat	

accelerated test. Arrows point out the mean induction period determined for each sample.....	84
Figure 5 – The pequi oil (PO) release profile of cashew gum/chitosan-pequi oil (CCP) and cashew gum/gelatin-pequi oil (CGP) microcapsules performed by: A) <i>in vitro</i> accelerated over time (min); B) as a function of pH (2 to 7); C) as a function of temperature (2 - 80 °C).....	86
Capítulo III	
Figure 1 – A) Y-C is the control yogurt without additions; B) Y-PO is yogurt added with 0.8% (w/w) pure oil; C) Y-CCP is yogurt added with 2.4% (w/w) of CCP microcapsules; D) Y-CGP is yogurt added with 1.7% CGP microcapsules.....	102
Figure 2 – Optical microscopy micrographs of yogurt formulations, where A is control yogurt (Y-C), B is yogurt added with pequi oil (Y-PO), C yogurt added with pequi oil microcapsules, using cashew gum/ chitosan (Y-CCP) and D is yogurt added to pequi oil microcapsules using cashew gum/gelatin (Y-CGP). Transmission electron microscopy micrographs (TEM) of yogurts, where E is Y-C, F is Y-PO, G is Y-CCP, and H is Y-CGP.....	109
Figure 3 – Texture profile analysis (TPA) of yogurt formulations, where Y-C is the control yogurt, Y-PO is the yogurt added with pequi oil, Y-CCP is the yogurt added with pequi oil microcapsules, using the gum cashew/chitosan and Y-CGP is yogurt added with pequi oil microcapsules, using cashew gum/gelatin. Different lowercase and capital letters show a significant difference ($p < 0.05$).....	110
Figure 4 – Shear rate x apparent viscosity ratio of yogurts made during storage time at 4 °C, where A is the control yogurt, B is the yogurt added with pequi oil, C is the yogurt added with pequi oil microcapsules, using cashew gum/chitosan and D is yogurt added with pequi oil microcapsules using cashew gum/gelatin. Where black, red, green, blue, and cyan lines represent the storage time of 1, 7, 14, 21 and 28 days, respectively.....	113

Figure 5 – Concentration of beta-carotene (%) of formulations Y-PO (yogurt added with pequi oil), Y-CCP (yogurt added with microcapsules of pequi oil, using cashew/chitosan gum) and Y-CGP (yogurt added of pequi oil microcapsules, using cashew gum/gelatin), where A is the stability of beta-carotene over the 28 days of storage, and B is the release profile of beta-carotene during *in vitro* digestion..... 114

LISTA DE TABELAS

Tabela 1 –	Perfil de ácidos graxos do óleo da polpa de pequi obtidos por diferentes métodos de extração.....	21
Tabela 2 –	Trabalhos recentes de microencapsulação de óleo vegetais por coacervação complexa.....	26
Tabela 3 –	Artigos científicos que utilizam a goma de cajueiro na tecnologia de microencapsulação.....	32
Capítulo I		
Table 1 –	Recent representative articles on the methods, core substances, encapsulating matrices, and (suggested) applications for microencapsulated vegetable oils.....	42
Capítulo II		
Table 1 –	Kinetic parameters for the release of microcapsules CCP (cashew gum/chitosan-pequi oil) and CGP (cashew gum/gelatin-pequi oil) using mathematical models of zero order, first order, Higuchi and Korsmeyer-Peppas. Where, K is the release constant, R² is the correlation coefficient and n is the diffusion exponent.....	87
Table 2 –	Fatty acid profile (%) of pequi oil (PO), cashew gum/chitosan-pequi oil (CCP) and cashew gum/gelatin-pequi oil (CGP) microcapsules and yogurt added from microcapsules in stages Y1 (the PO microcapsules were added along with the microorganism culture), Y2 (the PO microcapsules were added after being kept cooled overnight) and Y3 (the PO microcapsules was added after 2 hours of cooling and kept cooled overnight).....	89
Capítulo III		
Table 1 –	Effect of the incorporation of pequi oil and pequi oil microcapsules on the pH, total solids and syneresis of yogurts, where: Y-C is the control yogurt, Y-PO yogurt added with pequi oil; Y-CCP yogurt added with pequi oil microcapsules using cashew/chitosan gum and Y-CGP yogurt added with pequi oil microcapsules using cashew gum/gelatin.....	107

Table 2 –	Color parameters, where: Y-C is the control yogurt, Y-PO yogurt added with pequi oil; Y-CCP yogurt added with pequi oil microcapsules using cashew/chitosan gum and Y-CGP yogurt added with pequi oil microcapsules using cashew gum/gelatin.....	108
Table 3 –	Parameters of the Ostwald-de Waele model (K, n and R²) and apparent viscosity (η) calculated for a shear rate of 1 s⁻¹ during storage time at 4 °C, where Y-C is the control yogurt, Y-PO is pequi oil added yogurt, Y-CCP is pequi oil microcapsule added yogurt, using cashew gum/chitosan gum and Y-CGP is pequi oil microcapsule added yogurt, using cashew gum/gelatin.....	112

LISTA DE ABREVIATURAS

FT-IR	Fourier Transform Infrared Spectroscopy
TGA	Thermogravimetric Analysis
DSC	Differential Scanning Calorimetry
SEM	Scanning Electron Microscopy
TEM	Transmission Electron Microscopy
CG	Cashew Gum (goma de cajueiro)
CT	Chitosan (quitosana)
GE	Gelatin (gelatina)
PO	Pequi Oil (óleo de pequi)
CCP	Microcápsulas de óleo de pequi, utilizando a goma de cajueiro/quitosana
CGP	Microcápsulas de óleo de pequi, utilizando a goma de cajueiro/gelatina
Y-C	Iogurte controle
Y-PO	Iogurte adicionado com óleo de pequi puro
Y-CCP	Iogurte adicionado com microcápsulas CCP
Y-CGP	Iogurte adicionado com microcápsulas CGP
EE	Encapsulation Efficiency
TO	Total Oil
SO	Surface Oil
FAME	Fatty Acid Methyl Esters
CG-FID	Gas Chromatography apparatus with Flame Ionization Detector
HPLC	High Performance Liquid Chromatography
LC	Loading Capacity
TPA	Texture Profile Analysis
BC	Beta-carotene
SGF	Simulated Gastric Fluid
SIF	Simulated Intestinal Fluid

SUMÁRIO

1	INTRODUÇÃO	15
2	OBJETIVOS.....	17
2.1	Geral	17
2.2	Específicos	17
3	REVISÃO DE LITERATURA.....	18
3.1	Pequi (<i>Caryocar coariceum</i> Wittm.).....	18
3.1.2	Óleo da polpa de pequi.....	20
3.2	Microencapsulação.....	22
3.2.1	Coacervação complexa.....	23
3.2.2	Secagem por liofilização.....	27
3.2.3	Liberação controlada.....	28
3.3	Matriz encapsulante.....	29
3.3.1	Goma de cajueiro.....	30
3.3.2	Quitosana.....	34
3.3.3	Gelatina.....	36
3.4	Aplicação da microencapsulação na área de alimentos.....	37
4	ARTIGOS	40
4.1	CAPÍTULO I - Microencapsulation methods for vegetable oils: principles, stability and applications - a review.....	40
4.2	CAPÍTULO II - Characterization and controlled release of pequi oil microcapsules for yogurt application.....	69
	CAPÍTULO III - Yogurts supplemented with pequi oil microcapsules: Effects on physicochemical properties, stability, in vitro digestion and bioaccessibility.....	97
4.3	CONCLUSÃO	122
	REFERÊNCIAS.....	123
	ANEXO I.....	141
	ANEXO II.....	142

1 INTRODUÇÃO

Os iogurtes são produtos derivados do leite mais popular, sendo resultantes da acidificação química ou fermentação láctica lenta da lactose do leite por bactérias iniciadoras, *Streptococcus thermophilus* e *Lactobacillus delbrueckii* subsp. *bulgaricus* (GHARIBZAHEDI; CHRONAKIS, 2018; LADJEVARDI; GHARIBZAHEDI; MOUSAVI, 2015). Devido ao seu alto consumo, pode ser um bom veículo para garantir e melhorar a ingestão diária de nutrientes, o que pode prevenir doenças, e trazer impactos positivos na saúde dos consumidores (SILVA et al., 2019). Assim, a incorporação de ingredientes funcionais em matrizes alimentares, como iogurte, tem sido realizada com o objetivo de fortificar, e aumentar o valor agregado do produto.

Dentre os componentes bioativos que possuem baixa concentração no iogurte, pode-se destacar os ácidos graxos insaturados, porém existem poucos estudos que melhoraram o perfil de ácidos graxos do iogurte, sendo os óleos vegetais e de peixes os mais utilizados (BABA et al., 2018; BELLO et al., 2015; NIEUWENHOVE et al., 2019; RIBEIRO, B.; BONIF, 2021).

O óleo de pequi tem se destacado como matéria-prima para a indústria alimentícia e farmacêutica pela excelente qualidade associada a altos teores de ácidos graxos insaturados, predominantemente oleico (60,6%) (PESSOA et al., 2015), e carotenoides, como o beta-caroteno, um precursor da vitamina A (PINTO et al., 2018). O beta-caroteno, encontrado no óleo de pequi (cerca de 270 µL g⁻¹ de óleo), tem um papel crucial na saúde humana, como melhorar a imunidade, diminuir o risco de doenças cardíacas, e aumentar as funções gastrointestinais (GENG et al., 2022; XIE et al., 2021). No entanto, os carotenoides têm uma estrutura apolar e moléculas altamente insaturadas, tornando-os suscetíveis à oxidação e isomerização durante o processamento ou armazenamento (ŠEREHELJ et al., 2021). O óleo de pequi já é utilizado na indústria de alimentos na produção de margarinas (OLIVEIRA et al., 2011) e queijos (BENEVIDES et al. 2009), conferindo ao produto uma especificidade característica desejável pelos fabricantes. Porém algumas vezes, dependendo da aplicação, mascarar características naturais de sabor e aroma são tão importantes quanto sua estabilidade química. A utilização dos métodos de microencapsulação pode mascarar o forte sabor do óleo de pequi, além de proteger e promover sua liberação controlada.

Dos métodos de microencapsulação usados, a coacervação complexa tem sido particularmente bem-sucedida na estabilização de lipídios insaturados, e no fornecimento de um ingrediente com um prazo de validade sensorial prolongado (BARROW; NOLAN; JIN, 2007). Por ser um método bastante recomendado para a microencapsulação de substâncias lipofílicas, vários trabalhos o utilizam para encapsular óleos vegetais. O método consiste em

um fenômeno de separação de fase líquido-líquido que ocorre entre biopolímeros de cargas opostas por meio de interação eletrostática (EGHBAL; CHOUDHARY, 2018). A coacervação complexa funcionará impedindo que os compostos interajam fisicamente e/ou quimicamente com o ambiente externo, criando uma barreira ao redor do material ativo (SOUZA et al., 2020).

No presente estudo foram utilizadas duas combinações de diferentes materiais de parede: goma de cajueiro/quitosana e goma de cajueiro/gelatina. Estudos anteriores mostraram o potencial da goma de caju como substituto da goma arábica na microencapsulação do óleo de pequi (SILVA et al., 2018; NASCIMENTO et al., 2020). Uma seleção cuidadosa do material da parede é vital, pois impõe a eficiência de encapsulação e a estabilidade da microcápsula. O material de parede mais adequado para aplicações em alimentos deve ter as seguintes propriedades: não reativo com o núcleo, capaz de selar e reter o núcleo intacto dentro da cápsula, capaz de proteger eficazmente o núcleo contra condições ambientais adversas, isento de qualquer sabor desagradável, ser comestível e não tóxico, e economicamente viável (DHAKAL; HE, 2020; MCCLEMENTS; DECKER; WEISS, 2007; NAZZARO et al., 2012).

Com isso foi realizada aplicação dessas microcápsulas de óleo de pequi no iogurte com o objetivo de enriquecê-lo com os componentes bioativos do óleo. A adição do óleo de pequi no iogurte tem como principais funções aumentar o teor de ácidos graxos insaturados, como também a melhora nutricional proporcionada pelo beta-caroteno presente no óleo, que é precursor da pró-vitamina A. Testes de caracterização e liberação controlada das microcápsulas foram realizados previamente para a escolha da melhor matriz alimentar.

2 OBJETIVOS

2.1 Geral

Caracterizar as microcápsulas de óleo de pequi, obtidas por coacervação complexa, utilizando a goma de cajueiro/quitosana e goma de cajueiro/gelatina como materiais de parede, e avaliar sua aplicação em iogurte.

2.2 Específicos

- Produzir microcápsulas de óleo de pequi por coacervação complexa seguida da secagem por liofilização, caracterizar as microcápsulas pela eficiência de encapsulação, rendimento, capacidade de carga, morfologia e FT-IR, e estudar a estabilidade térmica (TGA e DSC) e oxidativa acelerada (Rancimat);
- Verificar o perfil de liberação sobre as condições *in vitro* ao longo do tempo, e em diferentes faixas de pH e temperatura, e calcular o perfil cinético de liberação a partir dos resultados obtidos na liberação *in vitro*;
- Realizar as análises de liberação e perfil de ácidos graxos do óleo de pequi e das microcápsulas aplicadas em matriz alimentar de iogurte.
- Analisar as propriedades do iogurte (pH, cor, sólidos totais, sinérese, textura viscosidade e morfologia) e estudar a estabilidade do óleo por meio da quantificação do beta-caroteno durante o tempo de armazenamento de 28 dias.
- Quantificar o beta-caroteno presente no óleo de pequi (encapsulado e não-encapsulado) adicionado em iogurte durante a digestão *in vitro* e analisar sua bioacessibilidade após completa digestão.

3 REVISÃO DE LITERATURA

3.1 Pequi (*Caryocar coriaceum* Wittm.)

O gênero *Caryocar* é amplamente difundido na América do Sul e compreende mais de vinte espécies. No Brasil, considerando uma área que inclui os Estados de Amazonas, Pará, Maranhão, Piauí, Goiás, Bahia, Ceará, São Paulo e Minas Gerais, as principais espécies são *Caryocar brasiliense* Cambess. e *Caryocar coriaceum* Wittm. (SENA et al., 2010).

O pequizeiro (*C. coriaceum*) (Figura 1) é uma espécie lenhosa perene nativa do nordeste do Brasil, ocorrendo em áreas de cerrado e cerradão (vegetação savana) na Chapada do Araripe no sul do Ceará. Segundo Sousa Júnior (2012), a Chapada do Araripe, em função de suas características edafoclimáticas, sendo mais úmida e chuvosa em relação a outras áreas do Nordeste, se apresenta como uma região favorável à produção do pequi. O pequizeiro pode ser classificado como frutífera ou oleaginosa, em razão das suas características e formas de utilização.

Figura 1: Pequizeiro (*Caryocar coriaceum* Wittm.).

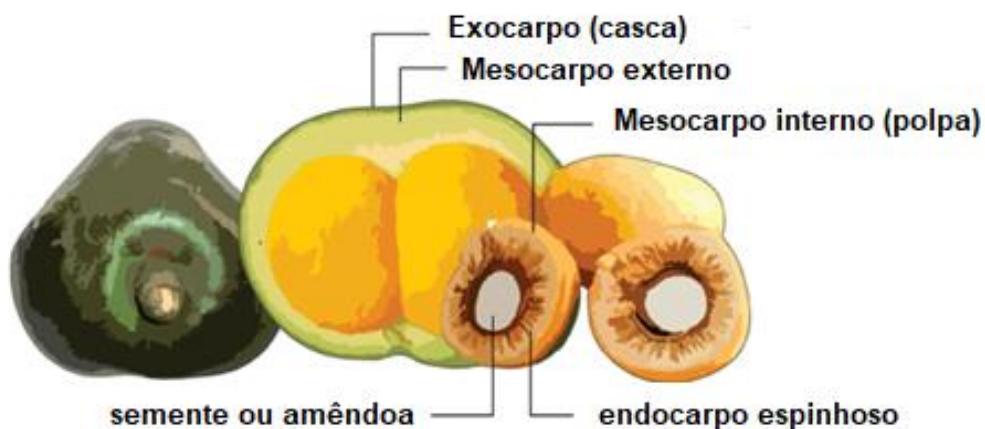


Fonte: próprio autor.

O pequi, também conhecido como pequi, piquiá, piqui-do-cerrado, piquiá bravo, pequerim, amendoâ-de-espinho, grão-de-cavalo e suari, tem como palavra de origem o tupi, e

significa casca espinhosa (SANTOS et al., 2013). O fruto (Figura 2) é constituído pelo exocarpo ou pericarpo, de coloração esverdeada ou marrom-esverdeada, mesocarpo externo, polpa branca com coloração pardo-acinzentada e mesocarpo interno, que constitui a porção comestível do fruto, possuindo coloração amarelada, e separa-se facilmente do mesocarpo externo quando maduro. O endocarpo, que é espinhoso, protege a semente ou amêndoas, que é revestida por um tegumento fino e marrom, sendo também uma porção comestível (NASCIMENTO-SILVA; NAVES, 2019).

Figura 2: Constituição esquemática do pequi (fruto).



Fonte: adaptado de Nascimento-Silva & Naves, 2019.

As cascas (exocarpo e mesocarpo) representam aproximadamente 80% da massa do fruto inteiro, e apresentam alto teor de fibras alimentares (45%). Além disso, a avaliação do perfil de monossacarídeos revelou a presença de uma grande quantidade de polissacarídeos pécticos (56%) (LEÃO et al., 2018). As cascas do pequi também possuem bioativos como polifenóis e carotenoides que proporcionam altos valores de atividade antioxidante (CANGUSSU et al., 2021; CALDEIRA et al., 2021).

A polpa do fruto de pequi é rica em lipídios (33,4%), é fonte importante de fibra alimentar (10,02%) e possui 3% de proteínas. Os quatro componentes majoritários da amêndoas de pequi são lipídios (51,51%), proteínas (25,27%), carboidratos (8,33%) e fibra alimentar (2,2%), apresentando baixo teor de umidade. (LIMA et al., 2007; PESSOA et al., 2015; TRAESEL et al., 2016). Tanto na polpa como na amêndoas do pequi, predominam os ácidos graxos insaturados com 61,35% e 52,17%, respectivamente, e teor elevado de minerais (cálcio,

ferro, zinco, fósforo, magnésio e potássio) (JOHNER et al., 2018). O ácido oleico está presente em maior concentração na polpa (55,87%), seguido pelo ácido palmítico (35,17%) (MIRANDA-VILELA et al., 2009).

O valor energético da amêndoia do pequi é considerado alto (aproximadamente 600 kcal/100 g), bem como o teor de lipídios (cerca de 50%), e de proteínas (acima de 25%) (TORRES et al., 2016). Os ácidos palmítico e oleico são predominantes, com em quantidades semelhantes, 43,76% e 43,59%, respectivamente. Também estão presentes o ácido linoleico (5,51%), esteárico (2,04%), e palmitoleico (1,23%), além de outros ácidos graxos em menores quantidades. Assim, tanto a polpa como a amêndoia do pequi possuem ácidos graxos importantes para compor uma dieta saudável (LIMA et al., 2007).

3.1.1 Óleo da polpa de pequi

A polpa do pequi apresenta aproximadamente 60% de óleo comestível, sendo que o processo tradicional de extração consiste no cozimento intensivo em água, e posterior retirada do sobrenadante. As principais desvantagens desse método de extração são o baixo rendimento, a necessidade de alta temperatura, e o fato de o óleo não ser filtrado. Para superar essas limitações, a busca de métodos que utilizem temperaturas amenas, e solventes não tóxicos, vem sendo estudados.

A extração do óleo por meio da separação física de fases por centrifugação, possibilita a obtenção de um produto de alta qualidade, já que não utiliza solventes orgânicos e altas temperaturas. Resumidamente, o processo para obtenção do óleo, partindo da polpa do pequi, baseia-se em aquecer a polpa entre 45 °C e 55 °C para facilitar a extração do óleo dos tecidos, centrifugar, e obter o óleo que fica sobrenadante (LIMA et al., 2019). Outro método de extração vantajoso, é a extração com CO₂ supercrítico, que utiliza temperaturas mais amenas (40–60 °C), e apresenta alto desempenho de extração, separação fácil de soluto do solvente, solvente não tóxico, e alta pureza (JOHNER et al., 2018).

O perfil de ácidos graxos presentes no óleo da polpa de pequi apresenta diferenças nas proporções de ácidos graxos saturados e insaturados em função das características do solo onde a árvore foi plantada e, também do processo de extração usado (Tabela 1). De maneira geral, o óleo de pequi apresenta altos teores de ácidos graxos palmítico (maior que 35%) e oleico (maior que 49%) e baixíssimos teores de ácido linolênico, perfil interessante para as indústrias de alimentos, devido a maior estabilidade oxidativa frente ao aquecimento. Segundo Sprecher (1981), o ácido oleico participa do metabolismo humano e desempenha papel

importante na síntese de hormônios, sendo essencial na nutrição humana, além de ajudar a diminuir os triglicerídeos, colesterol LDL, colesterol total e o índice glicêmico. A presença de ácido oleico também aumenta a estabilidade à oxidação do óleo vegetal (MEZZOMO et al., 2010).

Tabela 1: Perfil de ácidos graxos do óleo da polpa de pequi obtidos por diferentes métodos de extração.

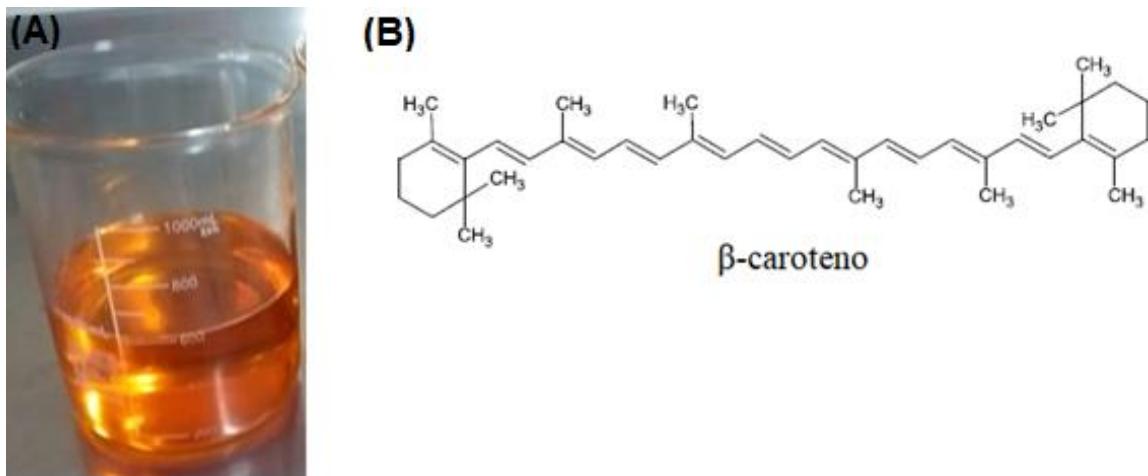
Ácidos graxos (FIGUEIREDO et al., 2016)	Extração por cozimento em água	Extração por solvente (SENA et al., 2010)	Extração fluido supercrítico (PESSOA et al., 2015)	Extração por separação física de fases (*)
Palmítico (C16:0)	34,1	34,18	35,34	32,81
Palmitoleico (C16:1)	0,3	0,27	0,55	0,41
Esteárico (C18:0)	1,7	1,73	1,83	1,58
Oleico (C18:1)	55,8	55,79	58,98	61,41
Linoleico (18:2)	1,8	1,80	2,38	2,32
Linolênico (18:3)	---	--	0,34	0,34

*Resultados obtidos pelo próprio autor.

Fonte: elaborada pela autora.

Precursor da pró-vitamina A, o beta-caroteno é o carotenoide responsável pela pigmentação característica do óleo de pequi (Figura 3) e age como um antioxidante natural presente no óleo, sendo o principal carotenoide encontrado (50% do conteúdo total). Ribeiro et al. (2012) explicaram que o maior teor de beta-caroteno é obtido com a exposição do óleo à temperaturas baixas durante o processo de extração, pois esta condição favorece a preservação dos carotenoides no óleo. As características benéficas dos carotenoides à saúde tornam essencial o consumo de alimentos considerados fontes desses compostos. Todavia, os carotenoides são compostos altamente insaturados e instáveis, o que os torna suscetíveis à degradação durante o processamento e armazenamento, diminuindo o valor nutricional dos alimentos (MATTA, 2013).

Figura 3: (A) Óleo extraído da polpa do pequi e (B) estrutura química do beta-caroteno.



Fonte: elaborada pela autora.

O óleo, tanto da polpa quanto da amêndoia, pelo seu sabor distinto, e por ser fonte de lipídios e vitaminas antioxidantes (A e E), é bastante utilizado na alimentação, e no preparo de molhos e temperos, acompanhando pratos regionais, e substituindo outras fontes de lipídios (FIGUEIREDO et al., 2016). Devido ao alto teor de ácidos graxos monoinsaturados (ácido oleico), a sua adição na dieta possui efeitos hipolipemiantes, reduzindo o risco de desenvolver doenças cardiovasculares.

O óleo de pequi vem sendo usado na medicina popular para o tratamento de resfriados e gripes, reumatismo, úlceras externas, dores musculares, e inflamação (SERRA et al., 2020). Suas propriedades terapêuticas se devem ao alto teor de fenóis totais, bem como aos seus ácidos graxos, importantes contribuintes para sua atividade antioxidante, e anti-inflamatória (FIGUEIREDO et al., 2016; SARAIVA et al., 2011; SENA et al., 2010). Acredita-se que os ácidos graxos essenciais tenham importante efeito anti-inflamatório no organismo, sendo usados como tratamentos nutricionais para doenças de pele, artrite e doenças respiratórias, como asma (HÄSSIG; LIANG; STAMPFLI, 2000).

3.2 Microencapsulação

A tecnologia de microencapsulação foi apresentada pela primeira vez por Green e Schleicher na década de 1950 com um registro de patente para a preparação de cápsulas contendo corantes, que foram desenvolvidas para serem incorporadas ao papel para fins de cópia (PAULO; SANTOS, 2017). É uma técnica na qual um ou mais compostos (núcleo, fase

interna ou material ativo) são circundados ou imobilizados por um ou mais materiais (casca, matriz encapsulante, material de suporte ou parede) para serem protegidos de fatores externos, como luz, alta concentração de oxigênio, calor, umidade, impedindo a evaporação de compostos voláteis, mascarando sabores e odores desagradáveis, e desenvolvendo valor agregado (COMUNIAN; FAVARO-TRINDADE, 2016). As microcápsulas são geralmente partículas de tamanho variando de 1 a 1000 µm (YE; GEORGES; SELOMULYA, 2018).

A técnica de microencapsulação pode facilitar o manuseio conveniente de materiais, permitindo a conversão de um material líquido/gasoso em sólido (HUANG; YU; RU, 2010). Um benefício adicional da microencapsulação é fornecer uma concentração adequada e dispersão consistente do material do núcleo. Essas funcionalidades têm sido amplamente exploradas na distribuição de medicamentos e vacinas nos setores farmacêuticos, e estão cada vez mais sendo utilizadas para agregar valor a novos produtos na indústria de alimentos (DHAKAL; HE, 2020).

A microencapsulação é um método multidisciplinar que envolve conhecimentos e de física, físico-química, química de polímeros, química de coloides, bioquímica, biotecnologia e ciência dos materiais (DHAKAL; HE, 2020). Existem diversos métodos de microencapsulação, e podem ser divididos em (OZKAN et al., 2019): métodos físicos (spray drying, spray chilling, liofilização e leito fluidizado) métodos físico-químicos (coacervação simples, coacervação complexa, gelificação iônica e deposição eletrostática camada-por-camada, evaporação de solvente, envolvimento lisossômico) e químicos (polimerização interfacial, polimerização *in situ*, e inclusão molecular).

Esta abordagem tecnológica tem sido explorada pelas indústrias farmacêutica (68%), alimentícia (13%), cosmética (8%), têxtil (5%), biomédica (3%), agrícola (2%) e eletrônica (PAULO; SANTOS, 2017). A microencapsulação visa aumentar a eficácia de substâncias selecionadas na indústria, e vários autores têm discutido as principais vantagens da sua aplicação em diferentes setores da indústria. No entanto, as indústrias farmacêutica e alimentícia são as principais forças motrizes nos avanços da microencapsulação.

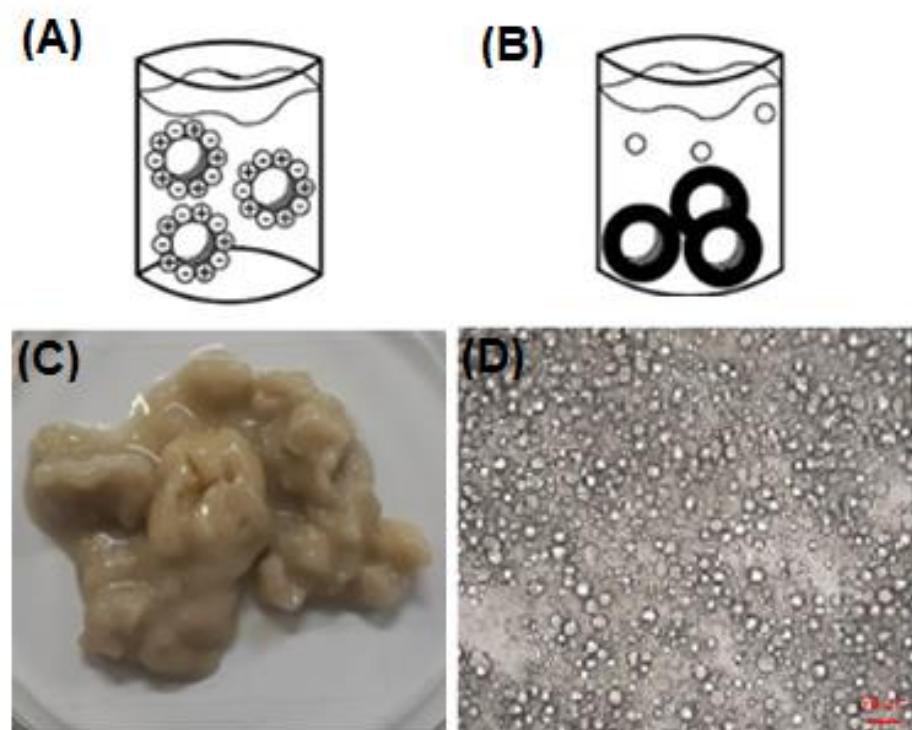
3.2.1 Coacervação complexa

Coacervação é um termo usado na química coloidal para denotar o processo de separação de fase associativo, induzido pela modificação do ambiente do meio (pH, força iônica, temperatura, solubilidade), sob condições controladas (TIMILSENA et al., 2017, 2019). A coacervação complexa é um fenômeno de separação de fase líquido-líquido que ocorre entre

biopolímeros de cargas opostas, por meio de interação eletrostática (EGHBAL; CHOUDHARY, 2018), impedindo que os compostos interajam fisicamente e/ou quimicamente com o ambiente externo, criando uma barreira ao redor do material ativo (SOUZA et al., 2020).

O processo de coacervação complexa (Figura 4) é um sistema trifásico que envolve o solvente, o material ativo, e o material de revestimento. Em geral, este processo envolve quatro etapas: (i) preparação de uma solução aquosa de dois ou mais polímeros e mistura da fase hidrofóbica com a solução aquosa de um polímero (geralmente solução proteica) e homogeneização da mistura resultante, de modo a produzir uma emulsão estável; (ii) mudança de pH, onde cada polímero irá assumir as respectivas cargas efetivas; (iii) mudança de temperatura para separação de fases; e (iv) endurecimento dos polímeros utilizando temperatura elevada, agente de dessolvatação ou reticulador (DESAI; PARK, 2005; TIMILSENA et al., 2019).

Figura 4: (A) Esquema representativo, onde (A) é interação eletrostática para formação das microcápsulas pelo método de coacervação complexa e (B) é a precipitação dos coacervados. (C) Imagem real dos cocervados formados e (D) micrografias das microcápsulas formadas.



Fonte: elaborada pela autora.

A coacervação complexa é conhecida por sua simplicidade, baixo custo, escalabilidade, e reprodutibilidade no encapsulamento de ingredientes alimentícios, o que resulta em alta eficiência de encapsulação, mesmo com capacidade de carga muito alta (até 99%). Timilsena et al. (2019) relataram que as características das matrizes encapsulantes usadas no processo de encapsulamento afetam significativamente a estabilidade do material ativo, a eficiência do processo, e o grau de proteção dos componentes ativos.

Vários parâmetros operacionais influenciam a complexação dos polímeros por meio de interações eletrostáticas (força iônica), pH, razão entre matrizes encapsulantes, concentração do material da parede, distribuição de carga, homogeneização, solubilidade das macromoléculas, peso molecular dos biopolímeros, e propriedades físicas e químicas das microcápsulas. Portanto, uma maior compreensão desses parâmetros é fundamental para uma melhor coacervação, e sua aplicação de forma mais eficiente (BEN AMARA et al., 2017; EGHBAL; CHOUDHARY, 2018; MA et al., 2019; RIOS-MERA et al., 2019; ZHANG, G. et al., 2009). Embora a força eletrostática entre macromoléculas com carga oposta seja a principal força motriz, outras forças como ligações intermoleculares de van der Walls, e interações hidrofóbicas nas proteínas, também afetam o complexo processo de coacervação (TIMILSENA et al., 2017; TURGEON; SCHMITT; SANCHEZ, 2007).

Essa técnica de microencapsulação tem sido particularmente bem-sucedida na estabilização de lipídios insaturados, e no fornecimento de um ingrediente com maior prazo de validade sensorial (BARROW; NOLAN; JIN, 2007). Por ser um método bastante recomendado para a microencapsulação de substâncias lipofílicas, vários trabalhos utilizam este método para encapsular óleos vegetais (tabela 2).

Tabela 2: Trabalhos recentes de microencapsulação de óleo vegetais por coacervação complexa.

Material encapsulante	Material ativo	Finalidade	Referência
Goma de cajueiro/gelatina	Óleo de pequi	Otimizar os parâmetros do processo de formação das microcápsulas	(NASCIMENTO et al., 2020)
Ovalbumina/alginato de sódio	Óleo de sacha inchi	Proteger os compostos bioativos e estudo térmico	(SOARES et al., 2019)
Goma arábica/gelatina	Óleo de pequi	Avaliar a influência da temperatura, velocidade de agitação com o objetivo de preservar os carotenoides presentes no óleo	(JUSTI; SANJINEZ-ARGANDOÑA; MACEDO, 2018)
Goma de cajueiro/quitosana	Óleo de pequi	Otimizar os parâmetros do processo de formação das microcápsulas	(SILVA et al., 2018)
Quitosana/xantana e quitosana/pectina	Óleo de palma	Aplicar as micropartículas ricas em carotenoides em alimento (pão e iogurte)	(RUTZ et al., 2017)
Gelatina/alginato	Óleo de buriti	Estudar influência da velocidade da agitação no tamanho das microcápsulas	(LEMOS; MARIANO MARFIL; NICOLETTI, 2017)
Isolado de proteína de linhaça/goma de linhaça	Óleo de linhaça	Comparar os métodos de secagem na estabilidade oxidativa	(KAUSHIK et al., 2016)
Proteína da semente de chia/Goma de semente de chia	Óleo de chia	Melhorar a estabilidade oxidativa do óleo	(TIMILSENA et al., 2016)

Fonte: elaborada pela autora.

3.2.2 Secagem por liofilização

A liofilização é uma das técnicas comumente utilizadas para secagem de microcápsulas termossensíveis produzidas por coacervação complexa, proporcionando para as micropartículas alta qualidade de estabilidade térmica e oxidativa, e estendendo seu tempo de estocagem (BALLESTEROS et al., 2017; GONZÁLEZ et al., 2016). Durante o processo de liofilização, a temperatura do material é reduzida abaixo do seu ponto de congelamento, e a água é removida por sublimação de gelo em vapor de água, a pressões inferiores às do ponto triplo da água (FENG et al., 2020).

O processo de liofilização pode ser dividido em três etapas: congelamento, secagem primária, e secagem secundária (ASSEGEHEGN et al., 2019). Durante a etapa de congelamento a maior parte da água é convertida em sólido, onde se formam redes de cristais de gelo. É nessa etapa que é determinada a morfologia do material, o tamanho, e a distribuição do tamanho dos cristais de gelo, que por sua vez influenciam vários parâmetros críticos, como resistência do produto seco, taxas de secagem primária e secundária, extensão da cristalinidade do produto, área de superfície, e reconstitutibilidade do produto seco (ASSEGEHEGN et al., 2019, 2020; SEARLES; CARPENTER; RANDOLPH, 2001).

Durante a secagem primária, a água livre congelada é removida pela conversão do gelo em vapor (sublimação). O processo de secagem é em função da temperatura da prateleira e da pressão da câmara, e a escolha apropriada desses dois parâmetros pode encurtar essa fase (BJELOŠEVIĆ et al., 2020). A última etapa do processo de liofilização é a secagem secundária, onde ocorre a remoção da água absorvida do produto. Durante a secagem secundária, a temperatura da prateleira aumenta ainda mais, enquanto a pressão é mantida constante ou, em alguns casos, é menor, e então a água sorvida na matriz do soluto é reduzida por dessorção (ISHWARYA; ANANDHARAMAKRISHNAN; STAPLEY, 2015; LIAPIS; BRUTTINI, 2009).

A principal vantagem do processo de liofilização é a obtenção de um produto de alta qualidade, devido à baixa indução de degradação térmica, à retenção de materiais voláteis responsáveis pelo aroma e sabor, e à estrutura rígida do material seco (LIAPIS; LITCHFIELD, 1979). O produto liofilizado possui uma textura porosa, sendo prontamente reconstituído quando imerso em água, ao seu respectivo tamanho e forma originais e possui estabilidade durante o armazenamento (MARQUES; SILVEIRA; FREIRE, 2006).

Dentre as desvantagens verificadas estão os custos elevados, devido ao processo de congelamento, a utilização de pressão reduzida, e o tempo maior que demanda em relação a outras técnicas, tornando o uso da liofilização na indústria de alimentos limitada aos produtos de alto valor agregado (RATTI, 2001).

3.2.3 Liberação controlada

O mecanismo de liberação do núcleo no local, e no momento adequado, é tão importante quanto a capacidade de proteção (DHAKAL; HE, 2020). As propriedades particulares da rede polimérica, tais como comprimento da cadeia, flexibilidade e mobilidade, absorção de água e comportamento de dilatação, extensão da plastificação, ou potenciais interações entre o polímero e o agente ativo, afetarão a taxa de difusão através da matriz polimérica e, portanto, a liberação do núcleo (MARTINS et al., 2014).

Os mecanismos de liberação variam com o tipo de matriz encapsulante usado para inserir ou encapsular o agente ativo, o método de preparação e o ambiente onde ocorre a liberação. Nos mecanismos de liberação, processos de difusão, biodegradação, dilatação (com formação de gel e inchaço) e osmose são os mais comumente estudados (ESTEVINHO et al., 2013). A classificação dos mecanismos de liberação é baseada nos fenômenos físico-químicos que promovem a liberação do agente ativo. Eles podem atuar individualmente ou combinados e incluem sistemas controlados por difusão, por barreira, ativados por pressão, por solvente, controlados osmoticamente, por pH, sensíveis à temperatura, ativados por fusão e combinados (GONÇALVES; ESTEVINHO; ROCHA, 2016).

Na área alimentícia os mecanismos de liberação mais relevantes são por ação do solvente ou por difusão, sendo este último considerado um dos mais relevantes (AZEREDO, 2005). A difusão consiste no deslocamento do agente ativo através da matriz, passando de uma região mais concentrada para uma de menor concentração (RODRÍGUEZ et al., 2016) e ocorre especialmente quando a micropartícula está intacta (SILVA; VIEIRA; HUBINGER, 2014), sendo controlada pelas limitações da transferência de massa na camada entre a matriz polimérica e o meio.

A ordem e o mecanismo de liberação das micropartículas podem ser descritos através da cinética de liberação, e avaliados na forma de diversos modelos matemáticos, sendo que as microcápsulas que tem como mecanismo de liberação a difusão, têm como modelos mais comumente utilizados, os de ordem zero, primeira ordem, Higuchi e Korsmeyer-Peppas (ANSARIFAR et al., 2017; CAMPELO-FELIX et al., 2017; ZANDI et al., 2017). Esses

modelos matemáticos se baseiam na lei de difusão de Fick e, dependendo do valor de n (coeficiente de difusão), podemos classificar o mecanismo de liberação nos seguintes casos: caso I, onde $n < 0,43$ ocorre liberação de acordo com a lei de difusão de Fick, seguindo um gradiente de potencial químico; caso II, onde $0,43 < n < 0,85$ o sistema de liberação é anômalo (não seguindo a lei de Fick); caso III, onde $n > 0,85$ ocorre uma liberação acelerada pela erosão ou intumescimento (molhabilidade) dos polímeros (CAMPELO et al., 2018).

3.3 Matriz encapsulante

Uma seleção cuidadosa do material da parede é vital, pois impõe a eficiência de encapsulação e a estabilidade da microcápsula. O material encapsulado mais adequado para aplicações em alimentos deve ter as seguintes propriedades: não reativo com o núcleo, capaz de selar e reter o núcleo intacto dentro da cápsula, capaz de proteger eficazmente o núcleo contra condições ambientais adversas, sem qualquer sabor desagradável, comestível e não tóxico e economicamente viável (DHAKAL; HE, 2020; MCCLEMENTS; DECKER; WEISS, 2007; NAZZARO et al., 2012). Dentre os materiais mais utilizados como matriz encapsulante estão os polissacarídeos e as proteínas:

- Polissacarídeos: compostos de fibra vegetal (inulina, pectina, β -glucana, polissacarídeo solúvel de soja), fibra animal (quitosana), gomas (guar, locusta, xantana, carragena, ágar, furcelanos, alginatos, gelana, curdlana, arábica, acácia e cajueiro), amido e derivados.
- Proteínas: proteína de soro de leite, gelatina, proteínas de sementes oleaginosas (de soja, canola, gergelim, girassol), zeína, proteína de ervilha, proteínas de arroz e glúten de trigo.
- Outros: fermento, ceras, lipídios.

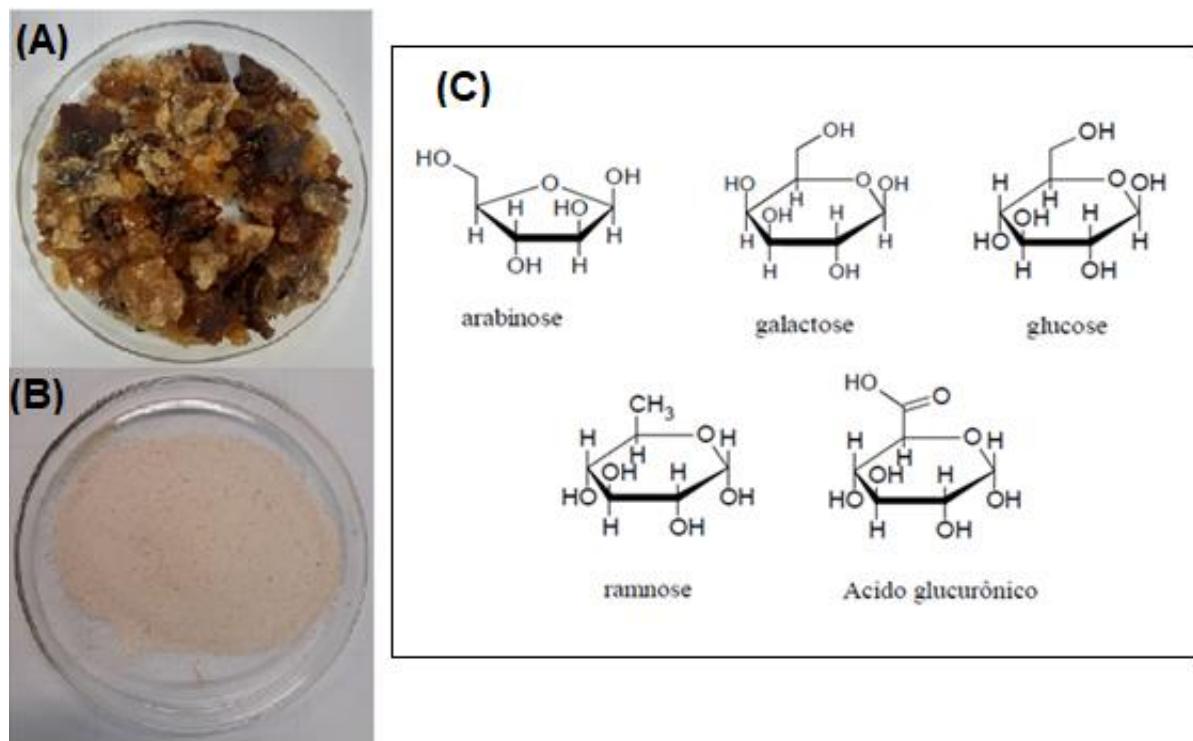
Nos últimos anos, o desejo dos pesquisadores de usar materiais alternativos em vez de materiais convencionais de parede, especialmente maltodextrina e goma arábica, levou ao uso de novos grupos de materiais de parede, que podem ser categorizados como materiais de parede “verdes”. Na verdade, o uso desses componentes oferece oportunidades para valorizar os subprodutos/resíduos alimentares de alto valor agregado. A utilização de subprodutos/resíduos para a produção desses compostos está de acordo com a tendência de produção sustentável. Além disso, alguns novos métodos de produção foram desenvolvidos para produzir componentes verdes a partir do subproduto/resíduo, levando em consideração as

questões ambientais e energéticas, que contribuem para a sustentabilidade de tais abordagens (SAMBORSKA et al., 2021).

3.3.1 Goma de cajueiro

A goma de cajueiro (figura 5) é produzida a partir do exsudato extraído da *Anarcardium occidentale* L., uma árvore popular conhecida como cajueiro. O cajueiro é uma árvore rústica que pode atingir 3,6 metros de altura e é facilmente encontrada em países tropicais como o Brasil, principalmente nas regiões Norte e Nordeste, em Estados como Piauí, Ceará e Rio Grande do Norte (RIBEIRO, A. J. et al., 2016).

Figura 5: (A) Exsudato (goma bruta), (B) polissacarídeo isolado (goma de cajueiro) e (C) principais estruturas químicas constituintes.



Fonte: elaborada pela autora.

O exsudato do cajueiro é obtido naturalmente pelas células epiteliais da casca após incisões ou em resposta a ataques de insetos e patógenos no tronco e nos ramos das árvores, produzindo assim a goma ou resina. Sua produção média é de 700 g por árvore/ano, com potencial de produção anual de até 38.000 t. A obtenção do exsudato pode ocorrer em todas as

partes da árvore e sua composição qualitativa e quantitativa depende da maturidade da árvore e das condições ambientais (KUMAR et al., 2012). A extração é realizada fisicamente por meio de incisões na casca ou quimicamente pela introdução na casca de substâncias como óxido de etileno, derivados do ácido benzóico e ácido 2-cloroetilfosfônico.

O exsudato, uma massa resinosa marrom, pode ser refinado por meio de solubilização, centrifugação, filtração e precipitação em etanol (TORQUATO et al., 2004). Em seguida, ele passa por uma etapa de secagem resultando em um pó amarelo rico em polissacarídeos. É um heteropolissacarídeo complexo constituído de uma cadeia principal de D-galactose (72%) com ramificação de D-glucose (14%), arabinose (4,6%), ramnose (3,2%) e ácido glucurônico (4,7%) (PAULA; RODRIGUES, 1995; PAULA; HEATLEY; BUDD, 1998).

As vantagens das gomas naturais incluem ser barato, biocompatível, processamento ecologicamente correto e alta biodisponibilidade (KUMAR et al., 2012). A goma de cajueiro tem sido estudada por suas propriedades funcionais, incluindo ser não tóxica, biodegradável e biocompatível (DIAS et al., 2016). Essa goma também exibe comportamento terapêutico, incluindo atividade anti-inflamatória (CARVALHO et al., 2015), efeitos antimicrobianos (CAMPOS et al., 2012; TORQUATO et al., 2004), cura natural (ARAGÃO-NETO et al., 2017; MONTEIRO et al., 2007), um aglutinante para comprimidos farmacêuticos (GOWTHAMARAJAN et al., 2011) e um imobilizador de enzima (SILVA et al., 2010). Além disso, a goma de cajueiro tem sido usada na indústria de alimentos e bebidas como um agente espessante e estabilizador coloidal (GOMEZ-ESTACA et al., 2016; KUMAR et al., 2012; PORTO; CRISTIANINI, 2014).

Nos últimos anos, a goma de cajueiro mostrou um potencial promissor nas indústrias farmacêutica e de biotecnologia (FORATO et al., 2015; PRAJAPATI et al., 2013). No campo biomédico e nanotecnologia, a goma de cajueiro tem sido usada para montar filmes (DIAS et al., 2016), sensores ultrafinos (BITTENCOURT et al., 2016; TEIXEIRA et al., 2015) e entrega de drogas sistemas (CORDEIRO et al., 2017; MONTEIRO et al., 2007). Em relação a este último, a goma de cajueiro tem sido utilizada como aglutinante para a produção de formulações farmacêuticas adesivas bucais, evitando o metabolismo hepático, melhorando a biodisponibilidade dos princípios ativos (GOWTHAMARAJAN et al., 2011).

A goma de cajueiro também já vem sendo estudada nas tecnologias de microencapsulação, principalmente como potencial substituto da goma arábica. A tabela 3, apresenta os principais trabalhos encontrados na literatura que utilizam a goma de cajueiro em diferentes técnicas de microencapsulação.

Tabela 3: Artigos científicos que utilizam a goma de cajueiro na tecnologia de microencapsulação.

Material encapsulante	Material ativo	Método de encapsulação	Objetivo	Referência
Goma de cajueiro	Beta-caroteno dissolvido no óleo de rícino	Eletropulverização	Producir e caracterizar com futuro potencial em aplicar nas áreas agrícolas, alimentícias e farmacêuticas	(VÁZQUEZ-GONZÁLEZ et al., 2021)
Goma de cajueiro/gelatina	Óleo de café verde	Coacervação complexa	Producir, caracterizar e aplicar em sucos	(DE OLIVEIRA, W. Q. et al., 2020)
Gelatina/ (goma arábica, pectina, goma de cajueiro, carboximetilcelulose e κ-carragenina)	Extrato de canela	Coacervação complexa	Caracterizar (estabilidade dos compostos fenólicos) e aplicar em sorvetes (mascarar sabor e adstringência)	(SOUZA et al., 2020)
Goma de cajueiro/gelatina	Óleo de pequi	Coacervação complexa	Otimizar os parâmetros do processo de formação das microcápsulas	(NASCIMENTO et al., 2020)
Goma de cajueiro e maltodextrina	Extrato de chá verde	Spray drying	Proteger os compostos bioativos e potencial como ingrediente alimentar	(SILVA, F. et al., 2018)

			Estudar o efeito do	
Goma de cajueiro	d- limoneno	Emulsão (produzidas por DHP)	DHP nas propriedades da emulsão e de encapsulação	(PORTO; CRISTIANI NI, 2018)
Goma de cajueiro/quitosa na	Óleo de pequi	Coacervação complexa	Otimizar os parâmetros do processo de formação das microcápsulas	(CARVALHO DA SILVA et al., 2018)
Goma de cajueiro, amido modificado e goma arábica	Óleo de peixe	Spray drying	Avaliar a goma de caju em comparação com os materiais convencionais em relação às propriedades e estabilidade oxidativa do óleo	(BOTREL et al., 2017)
Goma de cajueiro/gelatina	contendo astaxantina de resíduos de camarão	Coacervação complexa	Caracterizar e estudar a capacidade como corante em aplicações em iogurtes	(GOMEZ-ESTACA et al., 2016)
Goma de cajueiro e inulina	Óleo essencial de gengibre	Spray drying	Avaliar o efeito da substituição parcial da goma de caju pela inulina sobre as características do óleo essencial	(FERNANDES et al., 2016)

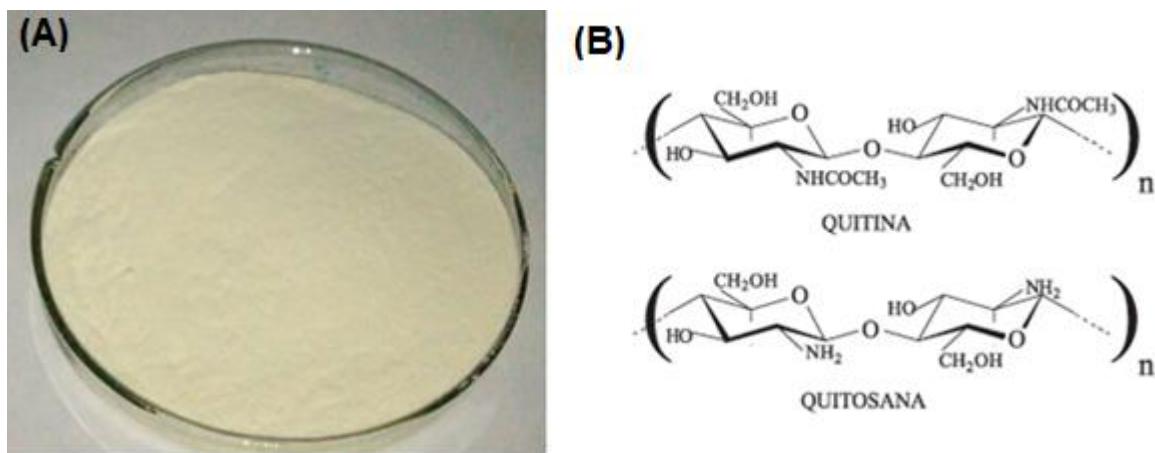
Alginato/goma de cajueiro	Óleo essencial de Lippia sidoides	Spray drying	Producir, caracterizar e estudar a cinética de liberação	(OLIVEIRA, E. F.; PAULA; PAULA, 2014)
Alginato/goma de cajueiro	Óleo essencial de Lippia sidoides	Gelificação ionotrópica	Producir, caracterizar e estudar a cinética de liberação in vitro e in vivo	(PAULA, H. C. B. et al., 2012)
Goma de cajueiro	Extrato de café	Spray drying	Proteger os compostos voláteis	(RODRIGUE S; GROSSO, 2008)

Fonte: elaborada pela autora.

3.3.2 Quitosana

Quitosana é segundo polímero natural mais obtido na natureza, depois da celulose, e é um polissacárido linear de amino de composto β -1,4 ligado a 2-(acetilamino)-2-desoxi-D-glucose (WANG et al., 2021). Obtido pela desacetilação da quitina extraída do exoesqueleto de crustáceos, insetos e parede celular de fungos, a quitosana (Figura 6) é um amino polissacarídeo natural de carga positiva (WANG et al., 2021). Esse polímero tem sido amplamente estudado como material de parede para microencapsulação de compostos que deveriam ter liberação controlada, como fármacos, óleos e compostos bioativos, com destaque para aqueles de caráter lipofílico. É usado sozinho ou em combinação com outros polímeros, como alginato, goma xantana, ciclodextrinas, oligossacarídeos e proteínas de soro de leite (CHANG et al., 2020; JANTARATHIN; BOROMPICHAI CHARTKUL; SANGUANDEEKUL, 2017; RIBEIRO, J. S.; VELOSO, 2021; RUDKE et al., 2019).

Figura 6: (A) Quitosana obtida pela desasetilação da quitina e (B) estrutura química da quitina e da quitosana.



Fonte: elaborada pela autora.

A quitosana consiste em resíduos de glucosamina e N-acetil glucosamina. Tem uma excelente capacidade de formação de complexos, que pode ser atribuída principalmente à disponibilidade de grupos -NH₂ livres distribuídos ao longo da cadeia principal da quitosana (YU et al., 2021). A abundância do grupo amina faz com que o polímero forme uma rede semicristalina emaranhada de ligações hidrofóbicas e de hidrogênio no estado sólido e contribui para uma boa solubilidade em condições ácidas (LIM; HWANG; LEE, 2021).

A molécula de quitosana não é anfifílica típica, mas os componentes da molécula são desacetilados (hidrofílicos) e resíduos de D-glucosamina acetilados (hidrofóbicos) que definem as propriedades ativas de superfície da quitosana. Dependendo do grau de desacetilação, a molécula fica mais ou menos hidrofóbica. A presença de porções hidrofóbicas e hidrofílicas na estrutura molecular favorece interações entre polímeros (MILKOVA, 2021).

A quitosana tem muitas aplicações potenciais na indústria por causa de propriedades físico-químicas e biológicas únicas. Dentre elas as mais estudadas são sua biodegradabilidade, biocompatibilidade, capacidade de quelação de íons de metais pesados, propriedades de formação de gel, baixa toxicidade e baixo custo (BUDINČIĆ et al., 2021), e bioatividades, como antioxidante, antimicrobiana, antifúngica, antitumoral, antialérgica, ativadora do sistema imunológico, anti-hipertensiva e redutora do colesterol. Essas propriedades funcionais podem depender de características estruturais, como peso molecular médio, grau de desacetilação, padrão de acetilação, polidispersidade e pureza. Além disso, a quitosana pode ser facilmente derivatizada para potencializar suas propriedades, como

aumentar a estabilidade em solução, atividades antimicrobianas e antioxidantes (ROCHA; COIMBRA; NUNES, 2017).

Em comparação com os polímeros sintéticos orgânicos na área têxtil e médica, a quitosana tem propriedades diferenciadas, como excelente aceitabilidade ambiental e não corrosividade. Além disso, a quitosana tem excelente desempenho de formação de filme e é atualmente aplicada na distribuição de drogas e nos campos alimentícios (HUO et al., 2018). A quitosana também tem sido amplamente utilizada na indústria farmacêutica e alimentícia como um transportador para a entrega de medicamentos. O uso de microesferas de quitosana como sistemas de liberação controlada de fármacos convencionais, fármacos protéicos e compostos bioativos, vem atraindo cada vez mais atenção desde o início dos anos 90 (ESTEVINHO et al., 2013).

A quitosana é considerada um polímero promissor como material de revestimento para encapsulamento com potencial aplicação (ROCHA; COIMBRA; NUNES, 2017). Tem sido frequentemente usada como um material de parede, bem como um emulsificante para microencapsulação de óleos insaturados (SHEN et al., 2010). Foi observado que, sendo um polissacarídeo poliacidônico, a quitosana envolve as gotículas da emulsão óleo-em-água (o/w) e repele metais pró-oxidantes no ambiente circundante (KLINKESORN et al., 2005). Curiosamente, a quitosana também é um polissacarídeo natural biofuncional, muitos pesquisadores relataram que a suplementação dietética de quitosana pode resultar em efeitos de promoção da saúde, como atividades hipolipidêmicas e cardioprotetoras (ANANDAN et al., 2015; VISHNU et al., 2017; ZHANG, W. et al., 2013).

3.3.3 Gelatina

A gelatina é uma mistura de vários polipeptídeos de alto peso molecular obtidos por meio da hidrólise controlada do colágeno fibroso insolúvel em ossos, couros, peles, tendões de animais (ARSYANTI et al., 2018; JANNAT et al., 2020). Devido às suas características tecnológicas e funcionais únicas, a gelatina é amplamente utilizada nas indústrias alimentícia, farmacêutica, médica, cosmética e fotográfica, como espessante, agente clarificante, emulsificante e formador de gel. A produção mundial anual de gelatina foi de aproximadamente 326.000 toneladas em 2008, e a demanda global por gelatina ainda está aumentando (JANNAT et al., 2020). Os recursos mais importantes da produção de gelatina são pele de porco (46%), pele de gado (29%), e ossos de porco e gado (23%) (AYKIN-DİNÇER; KOÇ; ERBAS, 2017).

Durante a extração da gelatina, os tecidos animais crus são submetidos a sucessivos tratamentos com ácido ou base diluída, resultando na clivagem parcial das ligações cruzadas das proteínas. A conversão do colágeno em gelatina gera moléculas de diferentes massas, devido à clivagem das ligações cruzadas covalentes inter-cadeias, e à quebra desfavorável de algumas ligações peptídicas intracadeia (ZHOU; MULVANEY; REGENSTEIN, 2006). O grau de conversão é dependente da intensidade do pré-tratamento ou da extração com água quente (SAMBORSKA et al., 2021).

O ponto isoelétrico da gelatina pode variar dependendo da fonte obtida, devido a pequenas variações dos grupos amida. A gelatina tipo A, que é fabricada a partir da hidrólise ácida, apresenta um valor do ponto isoelétrico próximo da condição alcalina (pH 7 a 9). Pelo contrário, a gelatina tipo B, fabricada a partir da hidrólise alcalina, mostra o valor do ponto isoelétrico próximo da condição ácida (pH 4 a 5) (ALI; KISHIMURA; BENJAKUL, 2018; COMUNIAN; FAVARO-TRINDADE, 2016).

As propriedades reológicas e funcionais da gelatina, como força do gel, viscosidade, gelificação e ponto de fusão, estão relacionadas às suas características químicas (ZHANG, G. et al., 2009). As propriedades físico-químicas mais importantes da gelatina são a força do gel e a viscosidade. A qualidade da gelatina é medida como a força do gel ou valor de Bloom, que pode ser classificado como baixo (<150), médio (150–220) e alto Bloom (220–300) (KAEWRUANG et al., 2014).

A gelatina tem sido amplamente utilizada como ingrediente em cápsulas moles e duras e como suplementos alimentares (YAP; GAM, 2019). Ainda é a principal escolha comercial como material de parede devido à sua excelente solubilidade em água, capacidade de emulsificação e espessamento, e alta atividade de reticulação devida à presença de grupos amino primários (PAULA, D. de A. et al., 2019).

3.4 Aplicação da microencapsulação na área de alimentos

Uma variedade de alimentos funcionais e suplementos dietéticos foram introduzidos no mercado nos últimos anos, oferecendo excelentes perspectivas para a melhoria da saúde pública. No entanto, a maior preocupação é que os compostos bioativos podem não ser totalmente absorvidos pelo corpo porque foram degradados antes de chegarem ao órgão-alvo. Por exemplo, a eficácia dos compostos bioativos pode ser reduzida devido à sua instabilidade causada por condições ácidas severas, reações enzimáticas, tempo de residência insuficiente e baixa permeabilidade no trato gastrointestinal (LEE et al., 2012). Por isso, para melhoria da

estabilidade do composto bioativo e controle da sua liberação, vem sendo empregada a tecnologia de encapsulação.

Para aplicações em alimentos, há muitos desafios no desenvolvimento de sistemas de microencapsulação eficientes e adequados. Por isso alguns critérios são utilizados para seleção da matriz encapsulante, assim como da técnica de microencapsulação, como por exemplo (DHAKAL; HE, 2020):

- Capacidade de proteger os núcleos de elementos ambientais no processamento de alimentos, incluindo alta temperatura, pressão, tensões mecânicas, oxigênio, acidez e alcalinidade, umidade e outros compostos reativos;
- Não utilização de calor e estresse mecânico;
- Digestível no sistema digestivo humano;
- Seguro para consumo humano, idealmente derivado de ingredientes comestíveis naturais;
- Facilidade na produção em escala industrial;
- Idealmente inodoro e incolor;
- Boa solubilidade em água;
- Viabilidade econômica.

Já foram relatados diversos usos da microencapsulação na aplicação em alimentos. Nesse sentido, pode-se citar uso de microcápsulas em bala de geleia (MOURA et al., 2019), sucos (OLIVEIRA, et al., 2020), biscoitos (GÓMEZ-MASCARAQUE et al., 2017), licores (JIANG; ZHU, 2019), chá (HERNÁNDEZ-BARRUETA et al., 2020) e iogurtes (COMUNIAN et al., 2016; RUTZ et al., 2017).

Os produtos lácteos são uma excelente fonte de proteínas de alta qualidade, cálcio, potássio, fósforo, magnésio, zinco e vitaminas B, como riboflavina, niacina, vitamina B6 e vitamina. As proteínas do iogurte são de excelente qualidade biológica, assim como as do leite, porque o valor nutritivo de suas proteínas é bem preservado durante o processo de fermentação (SENGUPTA et al., 2016). Os iogurtes são os produtos derivados do leite mais populares, produzidos por acidificação do leite ou por fermentação da lactose por bactérias iniciadoras, nomeadamente *Streptococcus thermophilus* e *Lactobacillus delbrueckii* subsp. *bulgaricus* (GHARIBZAHEDI; CHRONAKIS, 2018; LADJEVARDI; GHARIBZAHEDI; MOUSAVI, 2015).

O mercado global de iogurtes foi avaliado em 2019 em US \$ 99.553,38 milhões, e está estimado em US \$ 141.829,95 milhões até 2025, com taxa de crescimento anual composta

(CAGR) de 6,25%, de 2020 a 2025. O mercado de iogurtes tem visto um crescimento significativo devido ao aumento de consumidores preocupados com a saúde. Consequentemente, o mercado de iogurtes tem apresentado várias opções saudáveis, e sabores para satisfazer as preferências do consumidor (RIBEIRO, B.; BONIF, 2021). Um grande número de estudos mostrou que há muitos benefícios para a saúde com o consumo de iogurtes, incluindo melhora na tolerância à lactose e função imunológica, redução dos níveis de colesterol sérico e pressão arterial, controle de infecções gastrointestinais e sintomas do intestino irritável, aumento de nutrientes 'biodisponibilidade e indução de atividades anticarcinogênicas, antimicrobianas, antioxidantes e hipoalergênicas (YU et al., 2021).

Na última década, houve um interesse notável em fortificar leite e produtos lácteos com uma ampla variedade de ingredientes bioativos. O iogurte é um produto alimentar muito popular, destacando-se como um dos produtos lácteos fermentados mais consumidos no mundo. Devido ao seu alto consumo, pode ser um bom veículo para garantir e melhorar a ingestão diária de nutrientes, o que pode prevenir doenças e trazer impactos positivos na saúde dos consumidores (SILVA, et al., 2019). Assim, a incorporação de ingredientes funcionais em matrizes alimentares, como iogurte, tem sido realizada para fins selecionados, como a incorporação de curcumina (E100) (ALMEIDA et al., 2018), óleo de echium encapsulado, fitoesteróis e ácido sinápico (COMUNIAN et al., 2017), óleo de peixe encapsulado (GHORBANZADE et al., 2017), e aditivos naturais de camomila e erva-doce (CALEJA et al., 2016).

Dentre os componentes alimentares que menos estão presentes no iogurte, destacam-se a fibra alimentar, os compostos fenólicos, e os ácidos graxos insaturados. Dietas com alto teor desses componentes desempenham um papel significativo na prevenção de várias doenças (ROMÁN et al., 2019). Como resultado, fontes naturais como frutas e cereais têm sido usadas para fortificar iogurtes com fenólicos (HELAL; TAGLIAZUCCHI, 2018) e fibra alimentar (HASHEMI GAHRUIE et al., 2015). No entanto, foram relatadas pesquisas limitadas sobre a fortificação de iogurte com ácidos graxos insaturados (monoinsaturados e/ou poli-insaturados) para melhorar seu perfil lipídico (BABA et al., 2018; BELLO et al., 2015). Entre os poucos estudos relatados para melhorar o perfil de ácidos graxos de iogurtes foram geralmente usados óleos vegetais e óleos de peixe (BABA et al., 2018; BELLO et al., 2015; NIEUWENHOVE et al., 2019; RIBEIRO, B.; BONIF, 2021).

4 ARTIGOS**4.1 CAPÍTULO I - Microencapsulation methods for vegetable oils: principles, stability, and applications - a review**

Revista: Food Technology and Biotechnology ISSN: 1330-9862

Qualis: B1

Fator de impacto: 3.918

Microencapsulation methods for vegetable oils: principles, stability, and applications - a review

Running head: Microencapsulation methods for vegetable oils

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SUMMARY

In addition to being used in food, fuel, and lubricants, vegetable oils are promising in many additional applications such as food additives, nutritional supplements, cosmetics, and biomedicine; however, their low oxidative stability can limit their use. Microencapsulation is a well-established methodology for the preservation of oils against degradation, controlled release of active ingredients, protection against external factors during storage, and enhanced durability. In this article, microencapsulation methods for vegetable oils are reviewed, including physical methods (spray drying and freeze-drying), physical-chemical methods (complex coacervation, ionic gelation and electrostatic layer-by-layer deposition), and chemical methods (interfacial/*in situ* polymerization). This article also provides information on the principles, parameters, advantages, disadvantages, and applications of these methods.

Key words: Microparticles; vegetable oils; oxidative stability; fatty acids; controlled release.

INTRODUCTION

Vegetable oils are gaining a lot of attention in commercial development these days because of their availability, low price, biodegradability, and mild environmental impact. Vegetable oils contain, as their main components, triglycerides-esters of glycerol with three long-chain fatty acids (1, 2). The fatty acids can be the same or different in terms of hydrocarbon chain formed from 10 to 22 carbon

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atoms. In addition, the location and number of double bonds in the fatty acid chains cause these compounds to exhibit different physical and chemical properties (2). One of the most important parameters that influence lipid oxidation is the degree of unsaturation of the fatty acids (3). Oxidation caused by several external factors such as temperature, light, presence of oxygen and humidity can lead to the formation of unpleasant flavors and odors, reduction in the product shelf life, and generation of free radicals, which can have negative physiological effects on the body (4). The reason to use microencapsulation methods is to protect the oil against these external factors, along with the possibilities of masking its odors and flavors and providing release control.

Microencapsulation is a technique in which one or more substances (e.g., a core substance, an active material, a separate phase in a mixture) are surrounded or immobilized by one or more materials (e.g., a shell, a polymer matrix, a support, or wall material) and protected from biotic and abiotic factors (5). It is an effective technology to protect fatty acids and associated vitamins from the oxidative degradation process (6). The shell and core characteristics are important factors that play a critical role in determining the encapsulation efficiency, core stability, and other microencapsulation physicochemical characteristics (7).

The several methods of microencapsulation (8) can be divided into: physical methods (spray drying and freeze-drying) physical-chemical methods (complex coacervation, ionic gelation and electrostatic layer-by-layer deposition), and chemical methods (interfacial polymerization and *in situ* polymerization). The choice of a microencapsulation method will depend on the active material and encapsulating matrix, as well as the possible application area ([Table 1](#)).

Table 1: Recent representative articles on the methods, core substances, encapsulating matrices, and (suggested) applications for microencapsulated vegetable oils.

Methods	Vegetable Oil	Encapsulating Matrix	(Suggested) Applications	References
	Linseed oil	Different combinations of maltodextrin, gum arabic, whey protein and methyl cellulose	Food application: bread	Gallardo et al. (9)
Spray-drying	Linseed oil	Modified starch	Suggested application in food	Barroso et al. (10)
	Green coffee oil	Different combinations of modified starch, gum arabic and maltodextrin	Suggested application in food	Silva, Vieira and Hubinger (11)

	Green coffee oil	Gum arabic	Suggested application in cosmetics	Nosari et al. (12)
	Cress seed oil	Whey protein	Food application: biscuit	Umeshha et al. (13)
Freeze-drying	Olive oil	Different combinations of maltodextrin, carboxymethylcellulose and lecithin	Suggested application in food	Calvo et al. (14)
	Walnut oil	Different combinations of sodium caseinate, maltodextrin, lecithin and carboxymethylcellulose	Suggested application in food	Calvo et al. (15)
Complex coacervation	Corn oil	Xylitol and gelatin	Suggested application in food	Santos et al. (16)
	Palm oil	Chitosan/xanthan and chitosan/pectin	Food application: yogurt and bread	Rutz et al. (17)
Ionic gelation	Pequi oil	Cashew gum/chitosan	Suggested application in cosmetics	Silva et al. (18)
	Pomegranate seed oil	Whey protein/gum arabic	Suggested application in food	Costa et al. (19)
Electrostatic layer-by-layer deposition	Green coffee oil	Cashew gum/gelatin	Food application: juice	Oliveira et al. (20)
	Chia oil	Sodium alginate and calcium chloride	Food application: hamburger	Heck et al. (20, 21)
Polymerization <i>in situ</i>	Linseed oil	Bovine serum albumin (emulsifier), poly-L-arginine and dextran sulfate	Suggested application in food	Lomova, Sukhorukov and Antipina (23)
	Sunflower oil	Bovine serum albumin, poly (sodium 4-styrenesulfonate) and poly (allylamine hydrochloride)	Suggested application in food	Sadovoy et al. (24)
Polymerization <i>in situ</i>	Green coffee oil	Lecithin and chitosan	Suggested application in cosmetics	Carvalho, Silva and Hubinger (25)
	Chia oil	Modified sunflower lecithin, chitosan, and maltodextrin	Suggested application in food	Julio et al. (26)
Polymerization <i>in situ</i>	Neem oil	Phenol formaldehyde	Insecticide	Bagle et al. (27)

This review aims to present the methods commonly used in the microencapsulation of vegetable oils. The principles of each method, operating parameters, advantages, and disadvantages will first be

presented. Then, the representative studies will be discussed, highlighting their main objectives and possible applications.

MICROENCAPSULATION METHODS FOR VEGETABLE OIL

Physical methods

Spray drying

Spray drying is one of the most common methods used in microencapsulation of vegetable oil. The method consists of a process capable of transforming solutions, suspensions, or emulsions into a solid product. The spray drying process (Fig. 1) can be defined as an operation in which a liquid stream pumped into an atomizer is constantly divided into very fine droplets inside the drying chamber. A polymer, which serves as the encapsulant, is usually dissolved in the solution or in the continuous phase of a suspension or emulsion. In the drying chamber, the fine droplets come into contact with hot air, which by convection provides energy to heat and vaporize most of the solvent present in the droplets, forming dust particles. These are separated from the drying gas using a cyclone or a filter bag (28, 29).

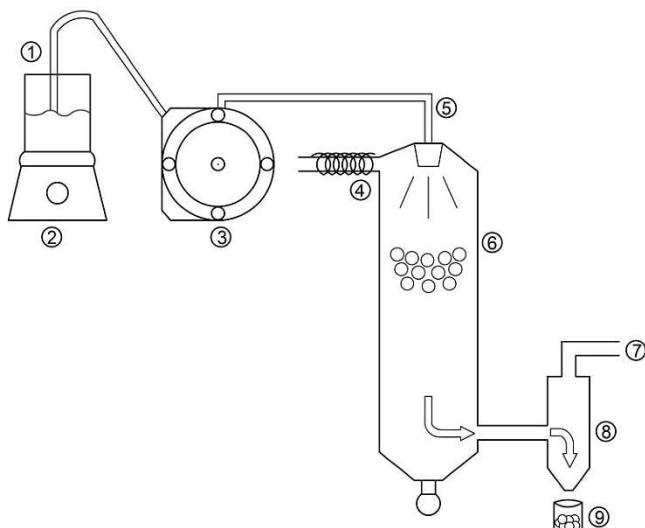


Fig. 1 Representative scheme for the spray drying microencapsulation process, where: 1) feeder; 2) magnetic stirrer; 3) peristaltic pump; 4) hot air/gas inlet; 5) atomizer nozzle; 6) drying chamber; 7) gas extractor; 8) cyclone; and 9) particle collector

Physical properties of emulsions and atomization parameters are important factors used to define the droplet formation and other parameters such as retention/encapsulation efficiency, physical-chemical properties, yield and storage stability (4, 11, 30-32).

Atomization parameters are related to the spray drying equipment: inlet/outlet temperature, feeding flow, atomizer gas flow, atomizer gas type, and nozzle size. (30, 31, 33, 34). Laboratory-scale spray-dryer usually has settings that allow the operator to vary the particles properties. The process can be modified in terms of its cycle mode, atomizer types, and airflow rate. However, this modularity becomes limited on an industrial scale due to financial and technological difficulties. For example, while

a variation in atomizer or airflow is viable on an industrial scale, the change of the cyclone or the drying chamber geometry can be very expensive (35).

This process has some advantages over other methods, such as the availability of large equipment, the possibility of using a wide variety of encapsulating materials, potentially large-scale production, simple equipment, high efficiency, and low process cost (36).

Many vegetable oils have been microencapsulated using the spray drying method. Bae and Lee (37) microencapsulated avocado oil in whey protein and maltodextrin matrix and obtained good results in improving the oil oxidative stability in different matrix concentrations. Other similar studies were reported emphasizing improvements in the oxidative stability of microencapsulated oil by spray drying (38-40).

Nosari et al. (12) observed the antioxidant activity of microencapsulated green coffee oil in gum arabic matrix under the effect of light, heat and oxygen and verified better stability results in comparison with non-encapsulated oil, even better than with the addition of alpha-tocopherol, an antioxidant widely used in the cosmetic and food industry. Gomes and Kurozawa (41) evaluated the potential antioxidant use of hydrolyzed rice protein in the microencapsulation of linseed oil and reported a reduction in the lipid oxidation of linseed oil during storage due to the greater antioxidant capacity of the protein hydrolysate. Oliveira et al. (42) evaluated the effect of a partial replacement of the whey protein isolate by maltodextrin and inulin on the pequi oil microcapsules and reported on the degradation of the bioactive compounds.

Freeze-drying

Freeze-drying or lyophilization is one of the microencapsulation methods most used in thermosensitive molecules, being a good alternative to the spray drying method (43). Microparticles with high resistance to thermal and oxidative degradation and good encapsulation efficiency are produced (38, 44, 45). During the freeze-drying process, the material temperature is reduced below its freezing point and the water is removed by sublimation at pressures below that of the triple point of water (46).

Freeze-drying process can be divided into three stages: freezing (solidification), primary drying (ice sublimation) and secondary drying (thawed water desorption) (47–50). During the freezing stage most of the water is converted into a solid, where ice crystal networks are formed. It is at this stage that the morphology of materials, the size and the size distribution of the ice crystals are determined, which in turn influence several critical parameters, such as dry product resistance, primary and secondary drying rates, extent of product crystallinity, surface area, and dry product reconstitutability (47, 50–52).

Primary drying is the second stage of the freeze-drying process, and this is closely related to the previous freezing stage (53). The sublimation of the ice starts from the top surface of the sample and continues to the bottom. For samples that were quickly frozen and formed small ice crystals that prevent

the mass transfer of sublimated water vapor through the dry layer, the primary drying can take a long time. On the other hand, slow freezing forms large ice crystals that facilitate the movement of water vapor (the mass transfer rate is high) and, as a result, the primary drying time is reduced (54). During primary drying, the free frozen water is removed by converting the ice to vapor (sublimation). The drying process depends on the shelf temperature and the chamber pressure, and the appropriate choice of these two parameters can shorten this phase (53).

The last stage of freeze-drying is secondary drying, where the water absorbed from the product is removed. This is the water that has not formed ice during freezing and not sublimated (47). During secondary drying, the shelf temperature increases even more, while the pressure is kept constant or, in some cases, is lower than that of primary drying (53). The sorbed water that remains in the solute matrix (the freeze-frozen phase) is then further reduced by desorption (55, 56).

Some recent studies have used freeze-drying as a microencapsulation method of vegetable oil. Özbek and Ergönül (57) evaluated the interaction effect of whey protein, maltodextrin, and gum arabic in microencapsulation of pumpkin seed oil in relation to emulsion stability, encapsulation efficiency, solubility, wetting time, total polyunsaturated fatty acid content, and total saturated fatty acid content. Calvo et al. (15) evaluated the influence of microencapsulation on the chemical composition of extra virgin olive oil and its oxidative stability, which prolonged the microencapsulated oils shelf life.

Comunian et al. (58) studied the co-encapsulation of pequi and buriti oils using whey protein to obtain better carotenoid retention and oxidative stability and compared the emulsion with and without the freeze-drying process. The freeze-dried samples showed the best carotenoid retention and oxidative stability, indicating that emulsification of the oils followed by freeze-drying can serve as effective carriers of bioactive compounds. Souza et al. (59) microencapsulated the chia oil, rich in polyunsaturated fatty acid (omega-3 and omega-6), to increase its stability during processing and storage.

Physical-chemical methods

Complex coacervation

Coacervation is a term used in colloidal chemistry to denote the process of formation of an associative phase induced by the environment modification (pH, ionic strength, temperature, solubility) under controlled conditions (6, 60). Complex coacervation is a phenomenon of liquid-liquid phase separation that occurs between oppositely charged polymers through electrostatic interactions (61). Complex coacervation functions in microencapsulation by creating a barrier around the active material and preventing active compounds from interacting physically and/or chemically with the external environment (62). It is a classic method of microencapsulation with great advantages, including more moderate reaction conditions during processing, lower equipment cost and greater loading capacity (5). This technique of microencapsulation has been particularly successful in stabilizing unsaturated lipids and providing a product with a consistent sensory shelf life (63).

Complex coacervation (Fig. 2) comprises a three-phase system that involves the solvent, the active material and the coating material. In general, this process for emulsions involves four steps: (i) preparing an aqueous solution of two or more polymers and mixing the hydrophobic phase with the aqueous solution of a polymer, often a protein solution, and homogenizing the resulting mixture, in order to produce a stable emulsion; (ii) pH change, where each polymer assumes its respective effective charges; (iii) change in temperature to a certain level necessary to induce coacervation and phase separation; and (iv) polymer hardening using high temperature, desolvation agent or crosslinker (60, 64).

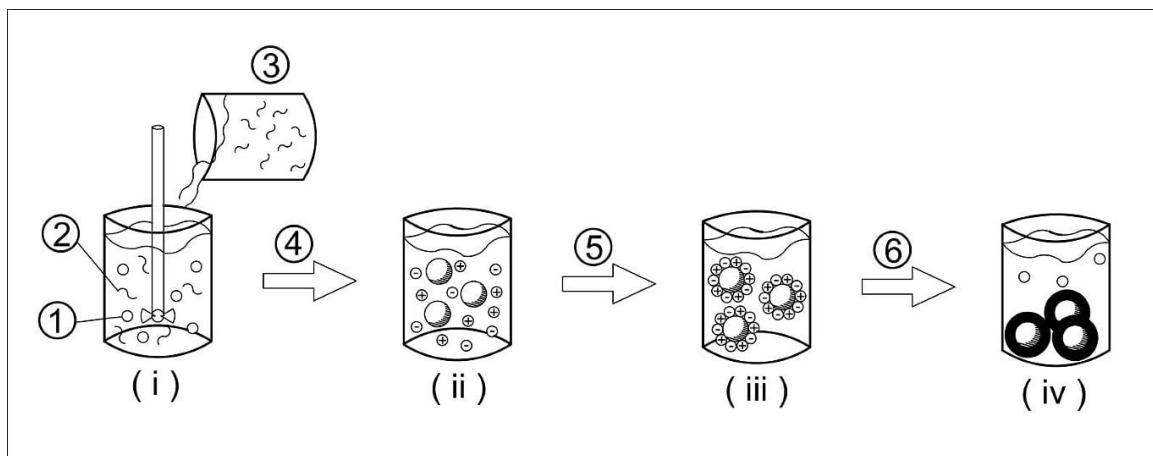


Fig. 2 Representative scheme for the complex coacervation process, where: 1) oil dispersed in the emulsion; 2) first solubilized polymer; 3) second solubilized polymer; 4) pH adjustment; 5) refrigeration; and 6) precipitation of coacervates.

Several operational parameters influence the complexation of the encapsulation procedure through electrostatic interactions (ionic strength), pH, composition of the encapsulating matrix, matrix concentration, charge distribution, homogenization, macromolecules solubility, and other molecular properties related to physical and chemical conditions of the solution. Therefore, a greater understanding of these parameters is fundamental for a better coacervation and its more efficient application (61, 65–68). Although the electrostatic force between oppositely charged macromolecules is the main driving force, van der Walls intermolecular forces and hydrophobic interactions in proteins also affect the complex coacervation process (6, 69).

After the coacervate formation process, the microcapsules can be dried, to improve storage and increase their shelf life. Among the drying methods, the most used are spray drying (70–72) and freeze-drying (62, 73–76). The choice of the drying method will depend on the nature of the encapsulating matrix and the active material.

Complex coacervation is a highly recommended method for the microencapsulation of lipophilic substances. Several studies use this method to encapsulate vegetable oils. Soares (76)

microencapsulated the sacha inchi oil (*Plukenetia volubilis* L.), rich in omega-3, in ovalbumin matrix and sodium alginate, obtaining microcapsules with good thermal behavior and protection for the bioactive compounds in the oil. Rutz et al. (17) studied the palm oil microencapsulation, rich in carotenoids, in chitosan/xanthan and chitosan/pectin matrices followed by spray drying and freeze-drying. Linseed oil, a rich source of omega-3 fatty acids was microencapsulated by Kaushik et al. (77) in a matrix formed by complex coacervation of linseed protein isolate and inseed gum. This matrix was cross-linked with glutaraldehyde and spray dried or freeze-dried; better results on oxidative stability was obtained than the non-encapsulated oil. Lemos, Marfil and Nicoletti (73) investigated the influence of hydrodynamic conditions in the buriti oil coacervation, rich in carotenoids, using gelatin/alginate as matrix and identified the agitation speed as having a strong influence on the microcapsules size. Justi, Sanjinez-Argandoña and Macedo (78) studied the pequi oil microencapsulation using gelatin/gum arabic as encapsulating matrices to improve the oil stability. In that study, the influence of temperature, agitation speed and core material on oil coacervation was evaluated in the preservation of carotenoids present in the oil. Timilsena et al. (7) obtained chia seed oil microcapsules in chia seed protein/chia seed gum matrix to improve the oil oxidative stability.

A few studies carried out the optimization of microcapsule formation parameters by complex coacervation. Devi et al. (79) microencapsulated the olive oil in gelatin/sodium alginate matrix and optimized the proportions of the biopolymers and pH. Silva et al. (18) studied cashew gum/chitosan for pequi oil microencapsulation and optimized the formation parameters for coacervates (viz., biopolymer charge, pH, and matrices ratios). A similar study was conducted by Nascimento et al. (80) with the cashew gum/gelatin matrix.

Ionic gelation

Ionic or ionotropic gelation is a microencapsulation process that starts from an aqueous polymeric solution, where ions with a low molecular weight interact with oppositely charged polyelectrolytes forming an insoluble gel as shown in Fig. 3 (81). It can be used to encapsulate hydrophilic or hydrophobic compounds (82–84). The active material to be encapsulated is dissolved/dispersed or emulsified in the polymeric solution. The drops of polymer solution that reach the ionic solution stimulate the formation of spherical gel structures, which contain the active material dispersed throughout the polymer matrix (85–88).

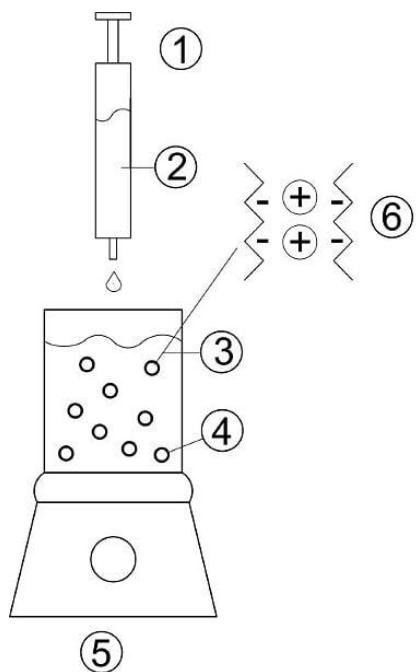


Fig. 3 Representative scheme for the ionic gelation process, where: 1) syringe; 2) emulsion (polymer + active material); 3) cross-linking solution; 4) microparticles; 5) magnetic stirrer; and 6) microparticle wall formation

This technique was adopted for natural polysaccharides to produce biocompatible and biodegradable products (89, 90). Sodium alginate is the most used biopolymer for ionic gelation due to its gelling property and chemical structure. Having carboxylic groups, alginates readily form gels in the presence of calcium ions or other divalent or trivalent cations, and a high guluronate content in alginate can produce stronger gels (91).

This technique is simple, easy to encapsulate substances, relatively low cost, and does not require specialized equipment, high temperature or an organic solvent (5, 84, 85). In addition, the ionic gelation technique has several more advantages, such as the use of aqueous solutions, small particle size, better control of particle size through variations in the precursor concentration, and the possibility of encapsulating a wide variety of substances (92–94).

Ionic gelation can be used in association with the nozzle vibration technique (NVT) that is featured in some equipment. NVT causes the formation of droplets of the same size by superimposing vibrations on a fluid jet through a precisely drilled nozzle. The vibration frequency selected determines the amount of droplets produced (95). This technology has gained significant interest for its ability to produce reproducible microspheres with defined sizes, thereby generating uniform and monodisperse particles (96). For the optimization of dispersed droplets, some parameters must be well defined, such as feed flow rate, vibration frequency, vibration amplitude and electrode voltage (97–99).

This technique is also applicable for microencapsulation of vegetable oil. Because it does not entail thermal stress, some recent studies used this technique to improve the oxidative stability of the encapsulated active ingredients. Menin et al. (90) employed ionic gelation associated with NVT and obtained particles with oxidative stability up to 13 times greater than the non-encapsulated oil. Sathasivam et al. (100) used ionic gelation/NVT in the microencapsulation of red palm oil with carboxymethylcellulose matrix and obtained capsules with good thermal stability.

Heck et al. (21) used ionic gelation to microencapsulate the chia oil enriched with rosemary that is targeted to replace 50% fat in hamburgers. The hamburgers produced with microparticles of chia oil enriched with rosemary showed greater oxidative stability, especially after cooking. In addition, the incorporation of rosemary antioxidants into chia oil reduced the sensory defects caused by lipid oxidation.

Electrostatic layer-by-layer deposition

In electrostatic layer-by-layer deposition (Fig. 4), an ionic emulsifier that quickly adsorbs on the surface of lipidic droplets during homogenization is used to produce a primary emulsion containing small droplets; then, an oppositely charged polyelectrolyte is added to the system which adsorbs on the droplet surfaces and produces a secondary emulsion containing droplets coated with a two-layer interface. This procedure can be repeated to form oil droplets coated by interfaces containing three or more layers (101–105). The deposited polymeric coatings allow substances to withstand various environmental stresses, such as pH, ionic strength, freezing and heating and show improved performance relative to uncoated ones (106, 107).

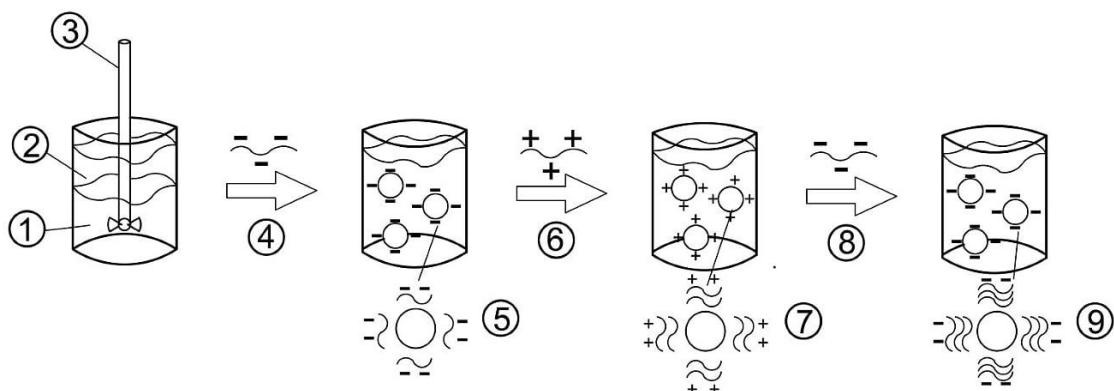


Fig. 4 Representative scheme for the electrostatic layer-by-layer process, where: 1) water; 2) oil; 3) agitation; 4) emulsifier; 5) primary emulsion; 6) polymer I; 7) secondary emulsion; 8) polymer II; and 9) tertiary emulsion

Layer-by-layer technology is simple, versatile and may be used to develop multilayer coatings when needed (108). The ionic characteristic (electric charge) must be evaluated as a function of the pH

between emulsifier and each biopolymer used in the system to determine the conditions for best electrostatic attraction between them (103, 109). The effectiveness can often be optimized by controlling the number, type and sequence of biopolymers layers used to coat the lipid droplets, as this allows the control of the thickness, composition, charge, permeability, and integrity of the interfaces (110).

Multilayer emulsions may have potential applications in the food or cosmetic industry, as this process offers advantages such as protecting emulsion droplets from oxidation or lipid aggregation, controlling or releasing active materials, and improving stability against environmental agents due to the thicker interfacial layers (25, 111). The electrostatic deposition method is, therefore, a versatile tool for modulating the functional performance of emulsion-based delivery systems by altering their interfacial properties (112).

Drying methods are recommended after the electrostatic layer-by-layer deposition process to transform the material into powder, with the objective of improving handling and storage. Freeze-drying (26, 113) and spray drying (25, 114–116) are the most used for drying of the particles. Carvalho, Silva and Hubinger (25) microencapsulated green coffee oil using emulsions stabilized by lecithin and chitosan through electrostatic layer-by-layer deposition followed by spray drying. Microparticles thus obtained exhibited better results for sun protection and oxidative stability than the free oil, with potential applications in cosmetics and personal care. Noello et al. (115) produced chia oil microparticles using both emulsions stabilized by whey protein concentrate and pectin through the electrostatic layer-by-layer deposition and emulsions prepared only with whey protein concentrate. The microparticles were dried by spray drying and showed higher oxidative stability than the pure oil. The emulsions obtained by electrostatic deposition had smaller droplet diameters and greater stability than emulsions produced only with whey. Julio et al. (26) did the physical-chemical characterization of chia oil microparticles produced from mono- and bi-layer emulsions using modified sunflower lecithin, chitosan and maltodextrin as matrix. The two-layer microparticles with modified sunflower lecithin were effective in protecting the chia oil against oxidative deterioration, being an adequate delivery system for the ω -3 fatty acids in this oil for the functional food application.

Fioramonti et al. (111) investigated the influence of acid pH and sodium alginate concentration on the flaxseed oil properties in water emulsions stabilized by whey protein isolate. Fioramonti et al. (113) also conducted another study about dehydration of microparticles. Freeze-drying was chosen due to the bioactive compounds present in linseed oil. However, the techniques applied to obtain microparticles by ultrasonic emulsification and freeze-drying processes contributed significantly to the oil oxidation, as high input energies during ultrasonic emulsification promoted an increase in lipid oxidation rates, with the consequent formation of highly reactive peroxides, whose concentration was beyond the limit allowed for food matrices. Fioramonti et al. (116) also evaluated the influence of homogenization pressure and spray drying. The experiments showed that it was possible to transform a

highly oxidizable ingredient of liquid phase into a solid, easy-to-handle powder with peroxide values within the permitted range for food.

Chemical methods

Interfacial/in situ polymerization

Microencapsulation of an active material by interfacial polymerization involves the oil-soluble phase dispersion in a continuous aqueous phase or an aqueous phase dispersion in an organic phase, depending on the solubility medium of the encapsulated core substance and the conditions for the precipitation of polymeric materials at the drop interface. Each phase contains a specific dissolved monomer suitable to react with the other monomer present in the other phase. The dispersed phase acts as a good solvent for the monomers, but it also serves as a non-solvent for the polymer produced in the reaction. Therefore, during polymerization, the system is composed of three mutually immiscible phases. Once the various monomers are added in drops to the system, reactions take place at the interface, resulting in the formation of insoluble oligomers in each drop with the tendency to precipitate at the interface to form a primary shell around the drop. The polymer formed is not soluble in the dispersed phase or in the continuous phase and precipitates (117, 118).

The interfacial polymerization technique has potential advantages, including possible control of microcapsule average size and shell thickness, high load of the active compound, versatile and stable mechanical and chemical properties of the shell, low cost, easy scale-up, simplicity and reliability of the process (119, 120). On the other hand, there are also some factors that limit the application of this technique, such as the production of a large oil-water interface, where proteins or enzymes are prone to inactivation, altering the biological activities of proteins during the polymerization reaction (8). Another negative point is that the resulting microcapsules usually have certain unreacted shell monomers, which can react with the core material and potentially cause its deactivation or other unwanted consequences (121).

In situ polymerization is similar to interfacial polymerization; however, the reagents involved in the synthesis of the active matrix are obtained from both dispersed and continuous phases. During in situ polymerization ([Fig. 5](#)), oil-in-water emulsions or water-in-oil emulsions are first produced under vigorous stirring or sonication of a biphasic liquid. The monomers and initiators used to build the capsule matrix are dissolved in the dispersed or continuous phase. As the polymer synthesized from the monomers is insoluble in the emulsion, polymerization usually occurs on the core material droplets surface, and the resulting polymer accumulates on the droplets surface, generating microcapsules with the desired core material (121–123). The controlled deposition and polymer precipitation occurs at the interface using precipitants, or a change in pH, temperature, or solvent quality (122).

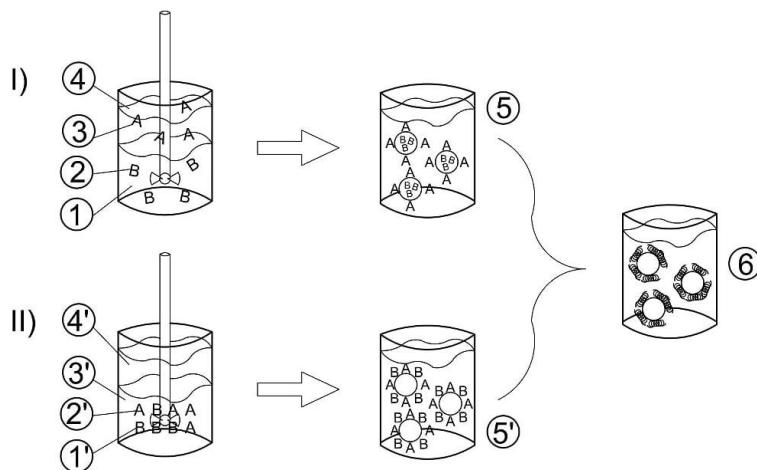


Fig. 5 Representative scheme for microencapsulation by polymerization: I) interfacial, where: 1) aqueous solution (hydrophilic phase); 2) monomer B; 3) monomer A; 4) oil (lipophilic phase); 5) diffusion of monomers to the interface; and 6) polymerization reaction and matrix formation. II) *in situ*, where 1') monomer B; 2') monomer A; 3') aqueous solution (hydrophilic phase); 4') oil (lipophilic phase); 5') dissolving the monomers in the continuous phase; and 6) polymerization reaction and matrix formation

In *situ* polymerization requires longer reaction times compared to other encapsulation techniques. However, this technique offers some advantages, such as low cost, ease of industrial manufacturing, and simplicity of the procedure (124). It should be noted that the microcapsules preparation by *in situ* polymerization depends not only on the core materials and the encapsulating matrix, but also on the reaction conditions, i.e., the type of emulsifier, agitation speed, core/matrix mass ratio, pH value, reaction temperature, and hydrophobic surface of the core (125, 126).

Moser et al. (127) studied the formation of microcapsules produced by the interfacial polymerization of chickpea protein and pectin in buriti oil emulsions and dried via spray drying. The microencapsulation and drying process did not influence the lipid oxidation, showing that the emulsions produced by interfacial polymerization protected the oil from the high temperatures of spray drying. Suryanarayana, Rao and Kumar (128) prepared linseed oil microcapsules coated by *in situ* polymerization of urea-formaldehyde resin. These microcapsules were incorporated into a paint formulation. The mechanical stability was studied and the microcapsules showed sufficient strength to withstand the shear generated during mixing and application of the paint.

CONCLUSIONS

In this review, several techniques commonly used in the microencapsulation of vegetable oil were presented. The advantages and disadvantages of each technique were discussed to assist in the choice of an appropriate approach for the encapsulation of the vegetable oil. Because the needs are

different for the food, cosmetic, personal care, and pharmaceutical industry, it is useful to have all these techniques available for use. From the publications in the literature, it is clear that this field is still growing and evolving, and we expect further developments and improvements in the future.

ACKNOWLEDGEMENTS

Thanks are due to Thomas Klasson for suggestions. The mention of trade names or commercial products in this publication is solely for the purpose of providing specific information and does not imply recommendation or endorsement by the U.S. Department of Agriculture (USDA). The USDA is an equal opportunity provider and employer.

FUNDING

This research received no external funding.

CONFLICT OF INTEREST

The authors declare no conflict of interest.

AUTHORS' CONTRIBUTION

All authors contributed to the study conception and design. The idea for the article were performed by [Luana Carvalho da Silva] and [Roselayne Ferro Furtado]. The literature search and data analysis were realized by [Luana Carvalho da Silva] and [Rachel Menezes Castelo]. The critically revised were performed by [Huai N. Cheng], [Atanu Biswas], [Roselayne Ferro Furtado] and [Carlucio Roberto Alves]. The first draft of the manuscript was written by [Luana Carvalho da Silva] and all authors commented on previous versions of the manuscript. All authors read and approved the final manuscript.

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**4.2 CAPÍTULO II - Characterization and controlled release of pequi oil microcapsules
for yogurt application**

Revista: LWT – Food Science and Technology INSS 0023-6438

Qualis: A1

Fator de impacto: 4.952

Characterization and controlled release of pequi oil microcapsules for yogurt application

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Abstract: Pequi oil is a valuable product for food industries due to its high levels of unsaturated fatty acids and carotenoids. This work used the complex coacervation technique with cashew gum/chitosan and cashew gum/gelatin matrices to encapsulate pequi oil in the production of enriched yogurt. Both wall materials achieved good results in encapsulation efficiency (>80%), yield (>50%), and loading capacity (<50%). The FTIR data demonstrated the presence of electrostatic interactions, thereby confirming encapsulation, and TGA, DSC and Rancimat data verified the microcapsule's stability. The acid release and temperature resistance results showed greater stability at pH's close to the optimum condition of the coacervation process and at temperatures below 80 °C. Finally, the potential for its application in yogurts was realized, showing that the preparation procedure of yogurt influenced the oil release rate and fatty acid profile, and that the addition of microcapsules should be optimally done during the cooling step.

Keywords: Polysaccharide; Protein; Complex coacervation; Pequi oil; Yogurt

1. INTRODUCTION

Pequi tree is native to Brazil and belongs to the *Caryocaraceae* family. Pequi oil has stood out as a useful raw material for the food and pharmaceutical industries due to its high levels of unsaturated fatty acids, predominantly oleic (60.6%), and carotenoids, such as beta-carotene, a precursor to vitamin A (Pinto et al., 2018). Oleic acid participates in human metabolism and plays an important role in hormone synthesis. In addition, it may improve heart conditions and reduce triglycerides, LDL cholesterol, total cholesterol, and the glycemic index (Mezzomo et al., 2010). Pequi oil is currently used in the food industry, despite its strong taste and smell, which give the product a distinctive characteristic noted by the manufacturers. In food formulations, sometimes masking the natural characteristics of taste and smell is as important as its chemical stability. The use of microencapsulation methods may mask the strong flavor and taste of the pequi oil, besides protecting against oxidation and facilitating its controlled release.

Oxidation can lead to unpleasant flavor and odor formation, reducing the product shelf life and promoting free radical generation, which can have negative physiological effects on the body (Alcântara et al., 2019). Complex coacervation is one of the most often used methods for lipid microencapsulation (Alexandre et al., 2019; Soares, Siqueira, Carvalho, Vicente, & Garcia-Rojas, 2019; Oliveira et al., 2020; Nascimento et al., 2020). This process entails moderate process conditions, low cost, and high encapsulation efficiency. It results from liquid-liquid phase separation that occurs between polymers of opposite charges through electrostatic interactions (Eghbal & Choudhary, 2018). This technique demands no sophisticated equipment, is effective, and can be easily adapted to protect essential fatty acids from the oxidative degradation process (Timilsena, Wang, Adhikari, & Adhikari, 2017).

Among the polysaccharides used as wall materials, gum arabic is one of the most often found in the food industry despite its high cost and problematic availability (Ghafarloo, Jouki, & Tabari, 2020). Recent studies have attempted to replace gum arabic by other types of plant-based gums (Jouki, Khazaei, Rezaei, & Taghavian-Saeid, 2021; Jouki & Khazaei, 2021; Khodashenas & Jouki, 2020; Shariati, Jouki, & Rafiei, 2020). A good substitute is cashew gum, due to its physical-chemical characteristics and also because it is a low-value coproduct of cashew production (Oliveira et al., 2018). Previous studies have already shown the potential of cashew gum as a substitute for gum arabic in the microencapsulation of pequi oil (Silva et al., 2018; Nascimento et al., 2020).

Nowadays, there has been much interest in fortifying milk and dairy products with a wide variety of bioactive ingredients. Because of its popularity, yogurt can be a good vehicle to ensure and improve the daily intake of nutrients, which can prevent diseases and maintain the health of consumers (Soares et al., 2019). Among the fatty acids that are present in yogurt can be mentioned the low quantity of unsaturated fatty acids. In this connection, enrichment with oils of vegetable or animal origin is desirable to improve the nutritional characteristic of yogurts. However, only a few studies have attempted to improve the unsaturated fatty acid profile of yogurts. Among the few reported studies, vegetables and fish oils were generally used (Bello, Torri, Piochi, & Zeppa, 2015; Nieuwenhove et al., 2019; Ribeiro & Bonif, 2021). The microencapsulation technology in the application of triglyceride oils in yogurt has been little explored in the literature (Baba et al., 2018; Hinnenkamp, Reineccius, & Ismail, 2021). Because of its economic potential, encapsulation of probiotics has been previously studied (Nyanzi, Jooste, & Buys, 2021).

In this work, two combinations of wall materials, cashew gum/chitosan (CCP) and cashew gum/gelatin (CGP) were compared for pequi oil microencapsulation to produce oil-enriched yogurts. The addition of microcapsules to yogurt was evaluated in two steps during the manufacturing process of the dairy products. The microencapsulation process was characterized, and aspects of the oil-controlled release were also evaluated in this study.

2. MATERIALS AND METHODS

2.1. Materials

Cashew gum (CG) polysaccharides were obtained from the *Anacardium occidentale* L. exudate collected from cashew trees at the Experimental Pacajus Field of Embrapa Agroindustry Tropical. Low molecular weight and 75-85% deacetylated chitosan (CT) was purchased from Sigma-Aldrich (St. Louis, MO, USA). Bovine gelatin (GE) 225H type B was provided by Rousselot® (The Netherlands). Methyl tricosanoate was purchased from Sigma-Aldrich. The microorganism culture was commercially acquired from Bio Rich® (*Lactobacillus acidophilus* LA-5 1x10⁶ UFC/g, *Bifidobacterium* BB-12 1x10⁶ UFC/g, and *Streptococcus thermophilus*).

2.2. Polysaccharides isolation from cashew gum

The isolation of polysaccharides was performed using the methodology previously described by Silva et al. (2018). Initially, the exudate collected was crushed in a knife mill.

Then, the sample was solubilized in water (300 g of the sample in one liter of water), filtered and centrifuged (15,303xg for 10 min at 25 °C). After removing the residues, the supernatant was precipitated in ethanol at a sample : ethanol ratio of 1:3 (v/v) for 24 h at 8 °C. The excess ethanol was removed, and the precipitate dried in an air circulation oven at 60 °C. Finally, the sample was ground, and the purified CG obtained.

2.3. Pequi pulp oil extraction

The pequi fruits (*Caryocar coriaceum* Wittm.) were washed, sanitized (chlorine at 200 g/L in water for 30 min), peeled and submitted to a hammer pulper (300 kg/h capacity). The pulp was stored in plastic containers and kept in a freezer. For pequi oil (PO) extraction, the pulp was heated to 45 °C and centrifuged at 4,500 rpm for 15 min to separate the oil (Lima et al., 2019).

2.4. Formation of microcapsules

The cashew gum/chitosan pequi oil-microcapsules (CCP) were prepared according to the methodology described by Silva et al. (2018). For the coacervation process, each emulsion was prepared from 100 mL CT (0.05 g/L) in deionized water (20 mL/L acetic acid) with 2 g PO; 100 mL of CG solution (0.11 g/L) in deionized water was added and homogenized using an ultra-turrax homogenizer for 3 min at 10,000 rpm. Then, 400 mL of water was added and homogenized in the ultra-turrax.

The cashew gum/gelatin pequi oil-microcapsules (CGP) were obtained using the methodology described by Nascimento et al. (2020). An emulsion was initially prepared to produce a solution containing 100 mL of GE (0.2 g/L) in deionized water and 2 g of PO; a solution of 100 mL of CG (0.4 g/L) in deionized water was then added and stirred in an ultra-turrax for 3 min at 10,000 rpm. Thereafter, 400 mL of water was added and homogenized again in the ultra-turrax.

Finally, after the emulsions of CCP and CGP were prepared, the pH was adjusted to 4.5, and cooled (5 °C) overnight. The solutions containing the microcapsules were centrifuged at 15,303xg for 10 min at 25 °C, the excess water was removed, and the rest was frozen in an ultra-freezer (-80 °C) for 24 hours. The frozen materials were taken to a freeze-dryer (Liotop LP 820) until completely dried and dispersed in an impact mill (IKA A11 basic).

2.5. Microcapsules characterization

2.5.1. Yield

The yield was calculated based on the weight ratio of freeze-dried microcapsules before the drying process, according to eq.1 (Jouki, Khazaei, Rashidi-alavijeh, & Ahmadi, 2021), where Y is the percentage yield, M_f is the value in grams of the final dry mass obtained after freeze-drying, and M_i is the initial mass used in preparing the solution for the coacervation process (biopolymers mass + oil mass) (Jouki, Khazaei, Rashidi-alavijeh, & Ahmadi, 2021; Huang, Sun, Xiao, & Yang, 2012).

$$Y(\%) = \frac{M_f}{M_i} \times 100 \quad (\text{eq.1})$$

2.5.2. Encapsulation efficiency

The amounts of total and superficial oil present were quantified by the oleic acid peak areas obtained by gas chromatography and standardized using an internal standard C23:0 (methyl tricosanoate). The encapsulation efficiency (EE) was determined by eq. 2, where A_{so} is the oleic acid area standardized from the superficial oil, and A_{to} is the oleic acid area standardized from the total oil.

$$EE(\%) = \frac{A_{to} - A_{so}}{A_{to}} \times 100 \quad (\text{eq.2})$$

2.5.2.1. Determination of total and superficial oil

For the determination of the total oil (TO), 25 mL of 4 mol/L HCl solution was added to 0.5 g and 0.25 g of CCP and CGP, respectively, and shaken at 100 rpm for 24 h. 50 mL of ethanol (for better separation of the oil from the polymers), and 5 mL of n-heptane were added and centrifuged (15,303xg for 10 min at 25 °C). The fraction containing heptane with the released oil was collected, transesterified with methanol, and taken to a gas chromatograph to obtain the oleic acid peak area.

For the determination of the superficial oil (SO), 0.5 g and 0.25 g of CCP and CGP, respectively, were weighed and 50 mL of ethanol and 5 mL of n-heptane were added and stirred for 1 min. The fraction containing heptane with oil-released microcapsules were collected, transesterified, and taken to a gas chromatograph to obtain the oleic acid peak area.

2.5.2.2. Gas chromatography analysis

The fatty acids were converted into fatty acid methyl esters (FAMEs). In a 5 mL fraction of n-heptane containing the released oil, 0.25 mL of the 2 mol/L NaOH solution in methanol was added and vortexed for 20 sec. After transesterification to obtain FAMEs, 1 mL of the supernatant was collected and evaporated for further analysis. The analysis of the FAMEs was carried out in a gas chromatography apparatus with flame ionization detector (CG-FID) (Shimadzu, model GC2010 Plus), equipped with an Automator, model AOC 5000. A capillary column (SP2560) with biscyanopropyl polydimethylsiloxane stationary phase (100 m × 0.25 mm, df 0.20 µm; Supelco Bellefonte, PA) was used to separate the compounds. The injection mode used was flow division (split 1:30), and the carrier gas was hydrogen with a constant flow of 1.5 mL/min. The injector and detector temperature were 220 °C. The programming of the chromatographic oven included an initial temperature of 80 °C, ascending with a heating ramp from 11 °C/min to 180 °C, increasing in a ramp from 5 °C/min to 220 °C, and maintaining for 23 minutes. The identification of the peaks in the chromatogram was performed by comparing their retention indexes with those of a standard solution of fatty acids (CRM47885, Supelco) previously injected, following the same methodology. An internal standard C23:0 (methyl tricosanoate), diluted in hexane, at the concentration of 2 µL/mL, was used, where 10 µL of the standard solution and 700 µL of n-hexane (HPLC grade) were added together with the sample for the calculation of the peak area for standardized oleic acid. For the milk and yogurt samples, the fat extraction was performed by the method of Bligh & Dyer (1959).

2.5.3. Loading capacity

The loading capacity (LC) of the microcapsules was calculated according to Eq. 3, where M_{po} is the encapsulated PO mass calculated by the mass used initially concerning EE, and M_f is the value in grams of the final dry mass obtained after freeze-drying. According to the equation, the values were adjusted by the encapsulation efficiency.

$$LC(\%) = \frac{M_{po}}{M_f} \times 100 \quad (\text{eq.3})$$

2.5.4. Microcapsules morphology

The micrographs of the coacervates before freeze-drying were obtained via transmission electron microscopy (TEM) (Model Vega 3, Tescan). An aliquot was collected from the precipitated microcapsules, water was added and dispersed by vortexing, and a small drop was deposited in a carbon-coated copper grid and left to stand for 3 min. The excess sample was

removed with a filter paper. Then, the sample was stained with phosphotungstic acid (0.04 g/L) for 3 min and the excess was again removed with filter paper. The TEM analysis was carried out at an acceleration voltage of 30 kV.

The micrographs of freeze-dried microcapsules were obtained using a scanning electron microscope (SEM; Quanta 450 FEG System: FEI Company, USA) with a scanning voltage of 5 kV. The samples were metalized with a thin layer of silver produced by an evaporator (Emitech, k550).

2.5.5. Fourier transform infrared spectroscopy (FT-IR)

The polymers and freeze-dried microcapsules were mixed with potassium bromide (KBr) (1% w/w) and analyzed by Fourier transform infrared spectroscopy on a Spectrum Two spectrometer (Perkin-Elmer, USA). The scan was performed in the frequency range 400-4000 cm⁻¹ with a resolution of 4 cm⁻¹. The oil samples were analyzed by transmission on KBr disks with 0.025 mm Teflon spacers (Castelo, Silva, Sousa, Magalhães, & Furtado, 2020).

2.6. Thermal analysis

The microcapsules were analyzed by thermogravimetric analysis (TGA) and differential scanning calorimetry (DSC). PerkinElmer STA 6000 equipment was used for TGA analysis. The samples were weighed and scanned in the temperature range from 25 to 750 °C at a heating rate of 10 °C/min and a nitrogen flow rate of 20 mL/min. For DSC analysis (Shimadzu), previously weighed samples were heated to a temperature range of 25 to 300 °C with a heating rate of 10 °C/min and a flow of nitrogen gas at 50 mL/min flow rate.

2.7. Accelerated oxidative stability (Rancimat)

The PO oxidative stability was analyzed by the oxidative stability index performed by accelerated oxidation using the Rancimat equipment (Metrohm Rancimat 743 model 873). 3 g of PO and 1.5 g of microcapsules (with and without oil) were used in a constant airflow of 10 L/h and a fixed temperature of 110 °C. The sample induction time, measured in hours, was used as an oxidative stability index.

2.8. Oil release

2.8.1. Calculation of release kinetics

For the calculation of release kinetics, microcapsules were released in vitro under accelerated conditions as described by Jain, Thakur, Ghoshal, Katare, & Shivhare (2016) with adaptations. 25 mL of 0.1 mol/L HCl solution was added to 0.5 g and 0.25 g of CCP and CGP, respectively, with constant shaking in a shaker (100 rpm). The released oil was evaluated at 0, 15, 30, 60, 120, 240, 360 min. After the specified analysis time, 50 mL of ethanol and 5 mL of n-heptane were added and slightly agitated. The fraction containing heptane with released oil was collected, transesterified, and taken to the gas chromatograph to obtain the oleic acid peak area according to section 2.5.2.2.

For the assessment of the release mechanism, the data were fitted to mathematical models that describe zero order, first order, Higuchi, and Korsmeyer-Peppas kinetics (Eqs. 4, 5, 6, and 7) as described by Budinčić et al. (2021) with adaptations:

$$\text{Zero order: } Q = Q_0 - K_0 t \quad (\text{eq.4})$$

$$\text{First order } \ln Q = \ln Q_0 - K_1 t \quad (\text{eq.5})$$

$$\text{Higuchi: } Q = K_H t^{1/2} \quad (\text{eq.6})$$

$$\text{Korsmeyer-Peppas: } Q = K_{KP} t^n \quad (\text{eq.7})$$

where Q is the amount of oil released at time t, Q₀ is the initial amount of oil in the solution, n is the diffusion exponent indicative of the active ingredient's transport mechanism, K₀, K₁, K_H, and K_{KP} are release rate constants for zero order, first order, and kinetic models of Higuchi and Korsmeyer-Peppas, respectively.

2.8.2. Oil release as functions of temperature and pH

For evaluation of the effect of temperature on oil release, 0.5 g and 0.25 g of CCP and CGP, respectively, were added to 25 mL preheated water at temperatures of 2, 20, 40, 60, and 80 °C and shaken at constant temperature in a shaker (100 rpm) for 5 minutes. The release was measured at different pH in the range of 2 - 7.

After the analysis time, 50 mL of ethanol and 5 mL of n-heptane were added to the sample and slightly agitated. The fraction containing heptane with the released oil was collected, transesterified and taken to the gas chromatograph to obtain the oleic acid peak area according to section 2.5.2.2.

2.9. Application of microcapsules in yogurt

2.9.1. Yogurt production

Yogurt was prepared according to Yu et al. (2021) with modifications. Initially, the milk was pasteurized at 70 °C for 30 min, followed by cooling to 43 °C, where the microorganism culture was added in the ratio of 400 mg for 1 L of milk. The milk was kept at 43 °C in an oven for 3-4 hours until clots were formed at pH 4.6. Finally, the yogurt was kept cooled overnight for further analysis of oil release and fatty acid profile. The PO microcapsules were added (1% w/v) under three different conditions: Y1: the PO microcapsules were added along with the microorganism culture, Y2: the PO microcapsules were added after kept cooled overnight, and Y3: the PO microcapsules were added after 2 hours of cooling and kept cooled overnight (Figure 1).

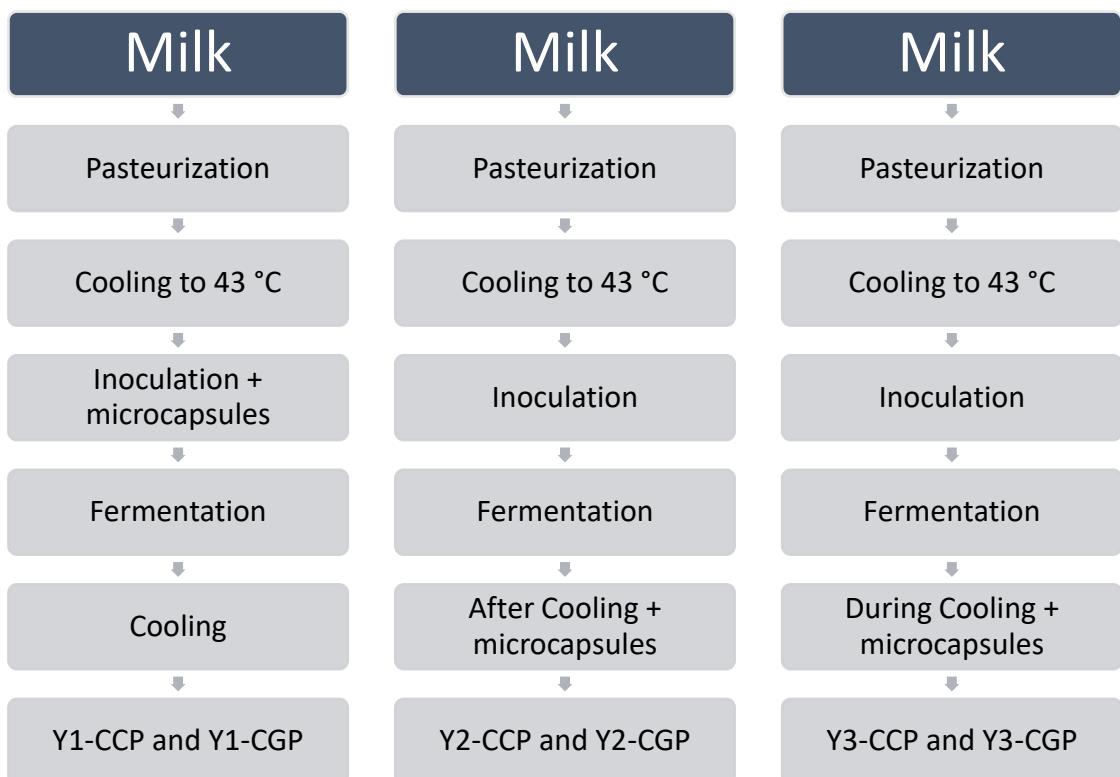


Figure 1: Flowchart representative of the preparation of yogurts enriched with microencapsulated pequi oil added in different stages.

2.10. Statistical analysis

The results for yogurt preparation were performed in triplicate and analyzed statistically using the Statistica 13.0 software. The values of efficiency, yield, and loading capacity were compared by Student's T-test.

3. RESULTS AND DISCUSSIONS

3.1. Microcapsules characterization

3.1.1. Encapsulation efficiency (EE), yield and loading capacity (LC)

Careful selection of wall material is vital, as it affects encapsulation efficiency as well as other characteristics of the microcapsules. Among the wall materials, the most used in complex coacervation are polysaccharides and proteins. The present work evaluates the combination of CCP and CGP, and the influence of these matrices on the EE, yield, and LC of PO microencapsulation.

The EE results differed significantly ($p>0.05$), with the CCP microcapsules (93.65 ± 0.37) exhibiting higher values than the CGP microcapsules (83.75 ± 2.88). A higher EE result indicates better trapping of the active material and a lower amount of surface oil that is more exposed to the external environment. Oliveira et al. (2020) encapsulated the green coffee oil by complex coacervation in a matrix of cashew gum and gelatin and obtained EE results above 85%. Other studies that used complex coacervation for vegetable oil microencapsulation also produced capsules with EE above 80% (Comunian et al., 2018; Lemos, Marfil, & Nicoletti, 2017; Timilsena, Adhikari, Barrow, & Adhikari, 2016).

The microcapsules indicated no significant difference ($p<0.05$) with respect to yield, being 53.29 ± 1.32 and 53.98 ± 1.15 for CCP and CGP microcapsules, respectively, showing that the change of wall material in this case had no detectable influence. Rutz et al. (2017) analyzed the yield results for different wall materials (chitosan/pectin and chitosan/xanthan), and also found no significant difference between the averages calculated. Alexandre et al. (2019) evaluated the yield of cashew gum and gelatin microcapsules crosslinked with tannic acid and obtained yield results ranging from 7.77% to 39.77% among the formulations attempted.

Regarding the LC, there was a significant difference between the results for CCP (25.71 ± 0.51) and CGP (39.30 ± 1.45) ($p>0.05$), with the better result for the CGP microcapsules. Other workers that used the complex coacervation as an encapsulation method also found LC about 30% (Oliveira et al., 2020; Timilsena et al., 2019). A higher LC decreases the thickness of the encapsulating matrix, which may cause a higher release rate (Devi, Hazarika, Deka, & Kakati, 2012) and influence the value of EE. This behavior was observed for CCP microcapsules that exhibited a higher EE and a lower LC, and for CGP that showed a lower EE and a higher LC.

3.1.2. Microcapsules morphology

Figures 2 A and B show the micrographs obtained by TEM of the CCP and CGP microcapsules, respectively. Both images revealed spherical micrometric shapes, with no signs of breaks and oil leaks. The particle size was heterogeneous as seen in Figures 2 C and D. In previous studies, the mean particle size of the CCP microcapsules was 4.8 μm (Silva et al., 2018) and 8.2 μm for the CGP microcapsules (Nascimento et al., 2020). The microcapsule density proved to be quite different, with the CCP having a darker tone, showing a denser matrix, which may rationalize the better result of EE. The CGP microcapsules, despite giving a better LC result, show a matrix with a lower quantity of biopolymers resulting in a less dense morphology, which makes the capsules more susceptible to ruptures caused by external factors.

Jeon, Yoo, & Park (2015) used TEM for the morphological characterization of particles obtained by multilayer electrostatic deposition with denser regions of 5 layers, with micrographs like those obtained with the CCP microcapsules. The studies carried out by Yu, Xue, & Zhang (2021), on the other hand, obtained micrographs in which the internal core and the external matrix can be viewed separately, typical of microcapsules obtained by complex coacervation, as can be observed in micrographs obtained from CGP microcapsules.

Micrographs of freeze-dried microcapsules were obtained by SEM. The agglomeration of microparticles (Figure 2 E and F) was also visualized by Cruz, Dagostin, Perussello, & Masson (2019) as a common feature of freeze-drying. The micrographs (Figure 2 G and H) revealed a homogeneous matrix without the presence of cracks and wrinkles, which indicates that the interactions between biopolymers occurred adequately without the need to add crosslinking materials as described by Soares et al. (2019).

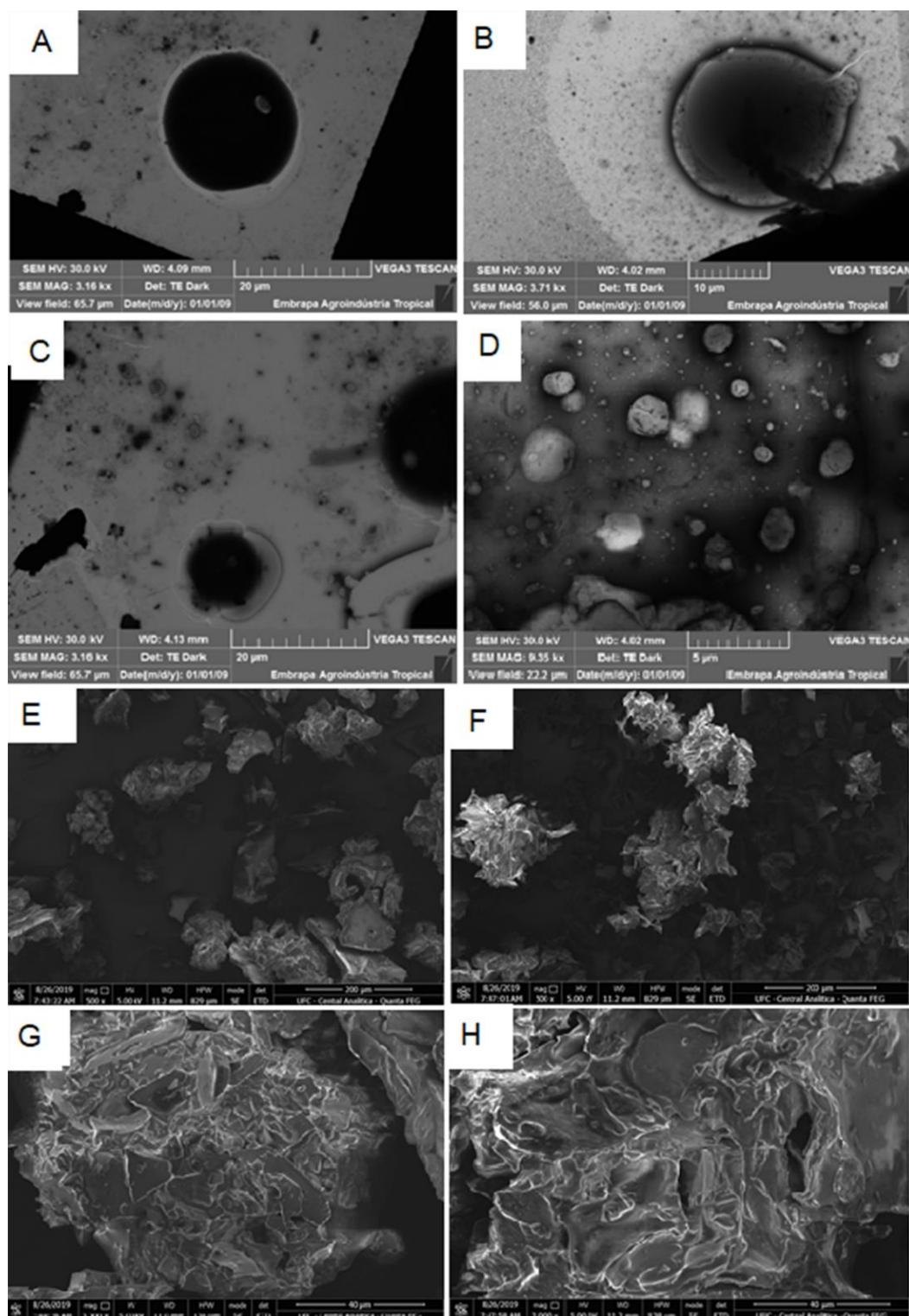


Figure 2: Transmission electron microscopy (TEM) micrographs of the microcapsules, where A and C correspond to CCP (cashew gum/chitosan-pequi oil) microcapsules, and B and D correspond to CGP (cashew gum/gelatin-pequi oil) microcapsules. Scanning electron microscopy (SEM) micrographs of the microcapsules are given in E and G corresponding to CCP microcapsules, and F and H corresponding to CGP microcapsules.

3.1.3. FT-IR

The FT-IR spectra for PO, CG, CT, and GE, as well as for CCP and CGP microcapsules, with and without the oil, are given in Figures 3 A and B. The PO showed strong characteristics of lipid bands in the 3050-2800 cm⁻¹ region, which are associated with the C-H stretch of the methyl (-CH₃) and methylene (-CH₂) structures in the oils. This region is also associated with cis-alkene (-HC=CH-) present in unsaturated fatty acid molecules. The peak position can be used to determine the degree of unsaturation in oils because more double bonds lead to greater peak intensity (Ombredane et al., 2020; Timilsena et al., 2019). The large peak in the 1753 cm⁻¹ region is attributed to the C=O bonds of in fatty acid esters. The peaks at 1467-1167 cm⁻¹ are mainly from combinations of deformations of the groups -CH₃ and -CH₂. The bands in the region of 1237 and 1167 cm⁻¹ are attributed to the symmetrical stretching (C-O-C) of triglycerides and phytosterol ester (Castelo et al., 2020).

The CG peaks that appear with low intensities at about 2925 cm⁻¹ are characteristic of O-H stretch in carboxyl groups. The CT spectrum (Figure 3 A) also showed the peaks of NH groups around 3300 cm⁻¹, and the amide bonds I, II and III are defined in angular deformation around 1656 and 1580 cm⁻¹, with greater intensity than GE. A low-intensity band around 1380 cm⁻¹ was found for acetyl CH₃ groups remaining after deacetylation (Castelo et al., 2020). GE is a biodegradable amphoteric polymer composed of polypeptides with different molecular weights (Devi et al., 2012). In the GE spectrum (Figure 3 B), the strong absorption band around 3300 cm⁻¹ was attributed to the amino groups, which have a positive charge in the acid medium (Cruz et al., 2019).

When comparing the spectra of the CCP (Figure 3 A) and CGP (Figure 3 B) microcapsules, each spectrum reveals distinct characteristics present in the biopolymers spectrum, as well as characteristic bands of PO. For both microcapsules, the cis-alkene band (-HC=CH-) at ca. 3000 cm⁻¹ and C=O peak at 1753 cm⁻¹ appear clearly and differently from the CCP and CGP microcapsules. The decreases in band intensity in the 1634 cm⁻¹ range for CCP microcapsules and the 1649 cm⁻¹ range for CGP microcapsules indicate that electrostatic interactions have occurred between the CT and GE amine groups (-NH₃⁺) and CG carboxyl groups (-COO⁻).

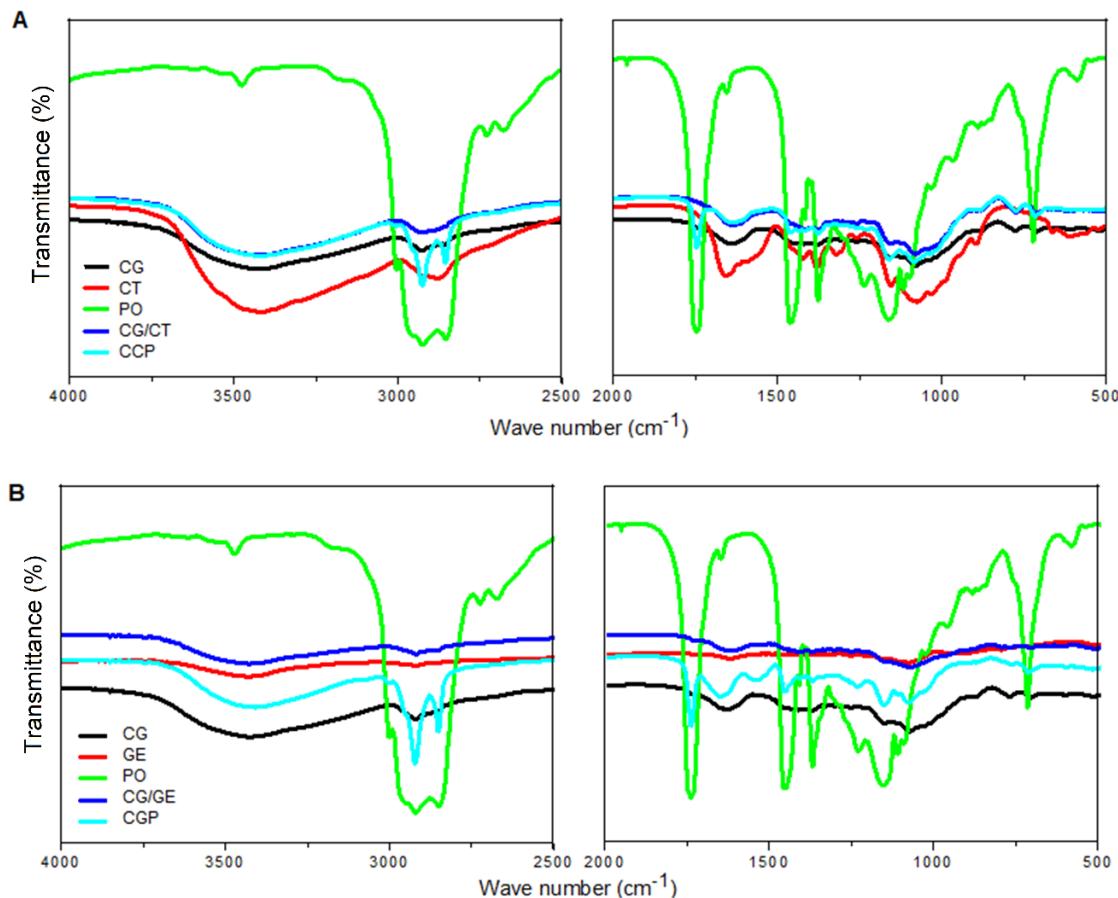


Figure 3: FT-IR spectra for A) cashew gum (CG), chitosan (CT), pequi oil (PO), cashew gum/chitosan (CG/CT) and cashew gum/chitosan-pequi oil (CCP); B) CG, gelatin (GE), PO, cashew gum/gelatin (CG/GE) and cashew gum/gelatin-pequi oil (CGP).

3.2. Thermal analysis and oxidative stability

TGA data (giving the percentage of weight loss) of the microcapsules during heating are illustrated in Figure 4 A and B. There was a slight weight loss from the CCP and CGP microcapsules up to about 150 °C, due to the loss of water. For the CCP microcapsules, three degradation peaks were presented: the first at 260 °C attributed to the degradation of chitosan (Chang, Varankovich, & Nickerson, 2016), the second at 319 °C referring to cashew gum, where polysaccharide degradation occurs (Silva, Feitosa, Paula, & Paula, 2009) and the third at 450 °C for PO degradation. For the CGP microcapsules, only the peaks for the degradation of the biopolymers were observed, indicating better stability, probably due to interpolymer affinity as a result of electrostatic interactions between them (Oliveira, Paula, & Paula, 2014).

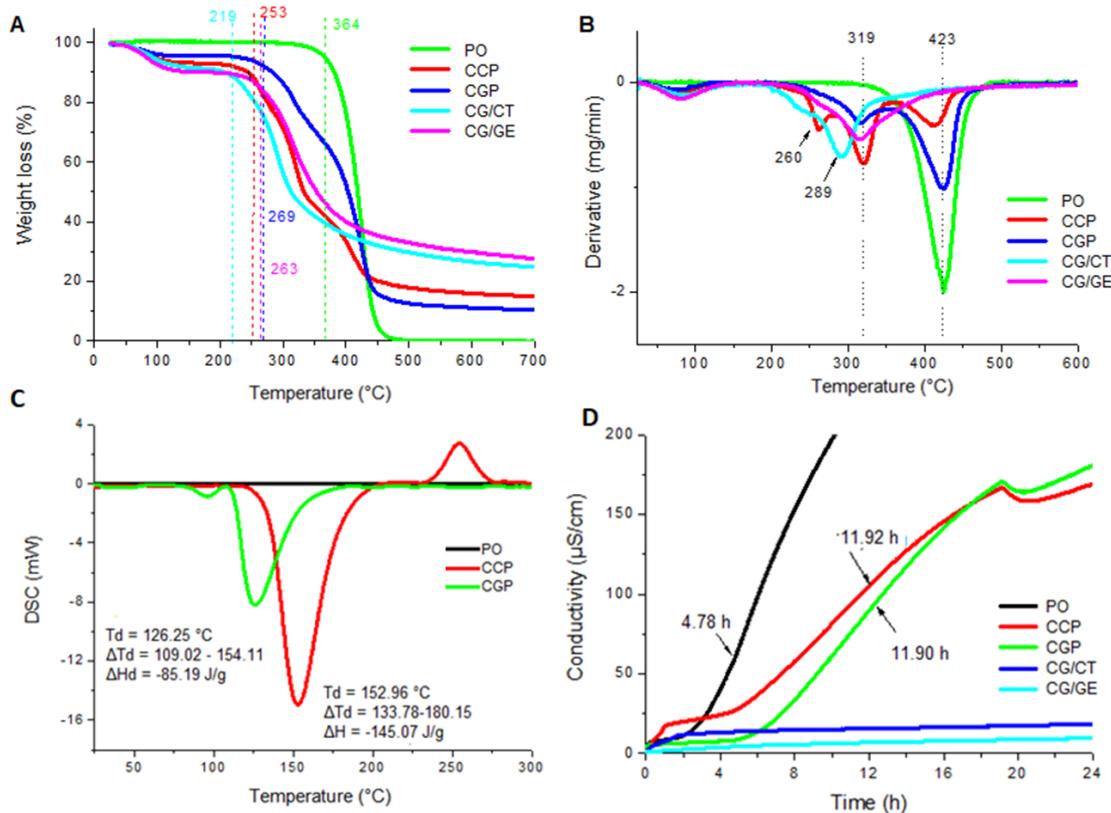


Figure 4: A) Weight loss (%) over time ($^{\circ}\text{C}$); B) derivative weight loss (mg/min) over time ($^{\circ}\text{C}$), for microcapsules of cashew gum/chitosan (CG/CT) and cashew gum/gelatin (CG/GE), and pequi oil (PO); C) Thermograms of cashew gum/chitosan-pequi oil (CCP) and cashew gum/gelatin-pequi oil (CGP) microcapsules, and PO where degradation temperature ranges (ΔT_d), degradation temperature peaks (T_d), and degradation enthalpies (ΔH_d) were calculated; D) Oxidation curves (conductivity versus time) were obtained from Rancimat accelerated test. Arrows point out the mean induction period determined for each sample.

Fig. 4 C shows the DSC thermograms of the CCP and CGP microcapsules and PO. The range of degradation temperature (ΔT_d), degradation temperature peak (T_d), and degradation enthalpy (ΔH_d) of the CCP and CGP microcapsules were determined from the thermograms. The peak degradation temperature and enthalpy of degradation of CGP ($T_d = 126.25 \text{ }^{\circ}\text{C}$ and $\Delta H_d = -85.10 \text{ J/g}$) were lower than the CCP microcapsules ($T_d = 152.96 \text{ }^{\circ}\text{C}$ and $\Delta H_d = -145.07 \text{ J/g}$). The higher peak degradation temperature and the degradation enthalpy of the CCP microcapsules indicated greater thermal stability than the CGP microcapsules. Both CCP and CGP microcapsules achieved better results than free biopolymers when compared with the data

in the literature, where T_d can vary from 80 to 110 °C, proving the increase in thermal stability due to the complexation of polymers (Soares et al., 2019; Huang et al., 2012).

One of the aims of microencapsulation is to delay the onset of oxidation. Under the condition of accelerated oxidation at high temperatures, the induction time of PO and microcapsules with and without oil can be seen in Figure 4 D. For the PO the mean induction time found was 4.78 h, for the CCP and CGP microcapsules (with oil) the mean induction time was 11.92 h and 11.90 h, respectively. The microencapsulation of PO by the CCP and CGP matrices delayed oxidation by approximately 2.5 times the heating time compared to the pure oil, whereas no difference in the mean induction time was found for the two encapsulating matrices. Encapsulation studies by complex coacervation have previously been shown to protect oils when subjected to the condition of accelerated oxidation. Thus, Oliveira et al. (2020) and Comunian et al. (2016a) verified protection against oxidation of up to 6 and 2 times, respectively, a longer time than pure oil, using cashew gum and gelatin to microencapsulate green coffee oil and echium oil, respectively.

3.3. Pequi oil-controlled release study

The release profile of active material encapsulated isolated is important for an understanding of its behavior and the mechanism by which the release occurs. Tests carried out under specific conditions can provide useful information, especially to determinate the type of product that can be incorporated. In the accelerated release simulated *in vitro* (Figure 5 A), it was observed that the “burst” effect occurred, where there is a rapid release of the oil up to 120 min, followed by a steady release between 120 to 360 min. Both microcapsules showed this behavior, differentiating only in the percentage of oil released.

CCP microcapsules reached the release point in the range of 30%, whereas the CGP microcapsules reached > 60% (Figure 5 A). The lower release results obtained by the CCP microcapsules may be related to the lower load capacity which provided a better packaging of the active material, making its release more difficult. Jain et al. (2016) carried out the accelerated *in vitro* release of beta-carotene microcapsules obtained by complex coacervation and reported an initial “burst” up to 30%, followed by a slower release. They attributed the initial explosive effect of release to the oil adsorbed on the surface and the slow release to the mixed mechanism of penetration, solubilization, and diffusion of oil into the matrix.

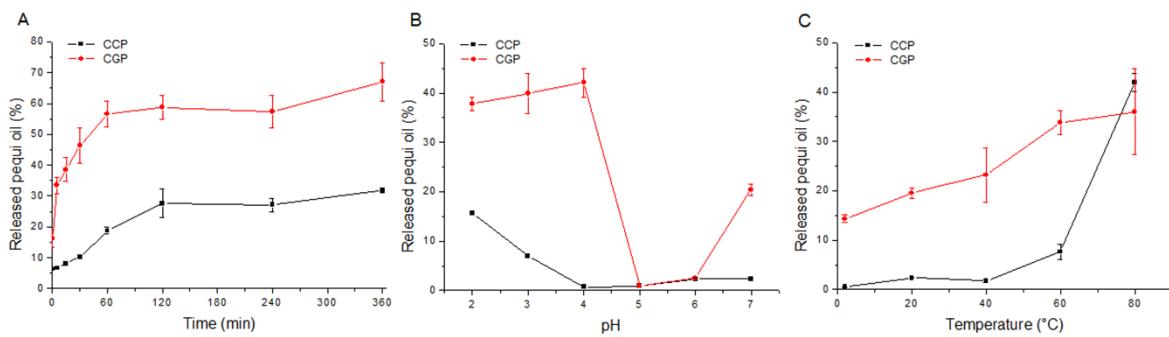


Figure 5: The pequi oil (PO) release profile of cashew gum/chitosan-pequi oil (CCP) and cashew gum/gelatin-pequi oil (CGP) microcapsules performed by: A) *in vitro* accelerated over time (min); B) as a function of pH (2 to 7); C) as a function of temperature (2 - 80 °C)

At the acidic pH range, both matrices had similar behaviors and showed the highest release values at the most extreme pH values (2 and 3). A decrease was observed at the pH near the isoelectric point of the formed complexes (3 to 5) and a slight increase close to neutrality (Figure 5 B). The release values of the CGP were higher than the CCP microcapsules. The low values found for the released oil in the pH used for the formation of the complexes was lower than the oil from particles; this can be explained by the greater agglomeration and precipitation of the microcapsules in the medium (increasing the oil retention), a behavior also noted by Comunian et al. (2016a) and Cruz et al. (2019).

The CCP microcapsules exhibited better resistance to the temperature increase up to 60 °C and then showed a “burst” increase in the transition up to 80 °C (Figure 5 C). The CGP microcapsules manifested a more gradual increase, ending in a result similar to that of CCP at 80 °C. Comunian et al. (2016a) evaluated the release at different temperatures of echium oil capsules obtained by complex coacervation, where, the microcapsules without crosslinking had the wall destroyed at 40 °C and the disruption of crosslinking started at 80 °C. Heating of the microcapsules may cause destabilization of the complex formed (Comunian et al., 2016b).

3.3.1. Release kinetics

For a better understanding of the kinetic profile of oil release from microcapsules, a study of accelerated *in vitro* release was performed. The results obtained up to 120 min were analyzed using mathematical models to simulate the release mechanism of the active material from the microcapsules. The values of the kinetic parameters used for the applied models are shown in Table 1.

Table 1: Kinetic parameters for the release of microcapsules CCP (cashew gum/chitosan-pequi oil) and CGP (cashew gum/gelatin-pequi oil) using mathematical models of zero order, first order, Higuchi and Korsmeyer-Peppas. Where, K is the release constant, R² is the correlation coefficient and n is the diffusion exponent.

Mathematical model	CCP	CGP
Zero order		
K ₀	0.1857	0.2907
R ²	0.9615	0.6923
First order		
K ₁	0.0128	0.0077
R ²	0.9494	0.5375
Higuchi		
K _H	2.0418	3.8702
R ²	0.8887	0.9160
Korsmeyer-Peppas		
K _{kp}	4.7512	18.5005
R ²	0.7896	0.9477
n	0.3039	0.2645

For the CCP microcapsules, the zero-order model gave the highest R², followed by the first-order model, indicating a linear trend during release; a similar result was also found by Cruz et al. (2019). The microcapsules that follow this type of profile do not disintegrate but release the active substance slowly and steadily (Fortunato et al., 2007). In the case of CGP microcapsules, a simple linear release was not the best model, and models such as Higuchi and Korsmeyer-Peppas were more preferred as shown in Table 2. The Korsmeyer-Peppas model had the highest value of R², followed by the Higuchi model; a similar result was also reported by Budinčić et al. (2021). This model is generally used to analyze the release of polymeric systems, when the release mechanism is not well known or when more than one type of release may be involved (Costa, 2002).

The diffusion exponent n varied from 0.3039 to 0.2645 for the CCP and CGP microcapsules, respectively. According to the literature, the value of n = 0.43 corresponds to the release of the active substance by diffusion according to Fick's law, while values less than 0.43 indicate pseudo-Fickian diffusion, where the diffusion shows similarities to a Fickian process. In this case, the release is quicker than Fickian (Ferreira, Pradela Filho, Santos, Takeuchi, & Assunção, 2019). Thus, it can be assumed that the release of pequi oil was based on a combination of removal of the superficial oil from the microcapsules and diffusion through the capsule wall; similar results were presented by Liu et al. (2016) and Budinčić et al. (2021)

3.4. Release of oil in yogurt and fatty acids profile

The oil release behavior of superficial oil from microcapsules introduced into different stages of yogurt production was evaluated in this study. As shown in the previous results of the release, the microcapsules showed better resistance to disintegration in an acid pH range from 4 to 5 and at a temperature below 80 °C. For this reason, the application in yogurt was chosen since the production conditions for yogurt are favorable to maintain the integrity of the microcapsule. The amount of superficial oil in the microcapsules introduced now of adding the microorganism was 20.78% and 31.29% for CCP and CGP respectively. The values of superficial oil were higher than those added after the cooling step at 0.37% and 0.36%, respectively. Under the third condition tested, a similar result for microcapsules added after 24 hours, the release was 0.34% and 0.54% for CCP and CGP respectively.

The fatty acids profiles of the PO, microcapsules, and the yogurt added with the microcapsules were also evaluated (Table 2). Among the results of the oil and the microcapsules, no differences were found for the percentages of saturated fatty acids (SFA), unsaturated (MUFA), and polyunsaturated (PUFA); thus, there is no interference from the microencapsulation process in the fatty acid profiles. On the other hand, for microcapsules introduced at the moment of adding the microorganism, variations were found with increased SFA and decreased MUFA, when compared with the PO values, showing that in the production process of the yogurt there is already oxidation of the oil resulting in differences in the percentage of SFA and MUFA.

The fatty acid profile of milk and yogurt, compared to formulations added with encapsulated and non-encapsulated oil, obtained higher values of SFA. This addition caused an increase in the percentage of oleic acid, between 25 and 33%. The yoghurt formulations that obtained better results in relation to amount of oleic acid were Y2-CCP and Y3-CCP.

Pereira et al. (2016) evaluated the variation of fatty acids exposed to radiation and observed some variations in the profile of SFA and MUFA due to material oxidation. Estrada, Boeneke, Bechtel, & Sathivel (2011) fortified the strawberry yogurt and analyzed the fatty acid profile, and no variation in the PUFA (predominant fatty acid) was observed during the production of the yogurt, but oxidation happened during storage.

Table 2: Fatty acid profile (%) of pequi oil (PO), cashew gum/chitosan-pequi oil (CCP) and cashew gum/gelatin-pequi oil (CGP) microcapsules and yogurt added from microcapsules in stages Y1 (the PO microcapsules were added along with the microorganism culture), Y2 (the PO microcapsules were added after being kept cooled overnight) and Y3 (the PO microcapsules was added after 2 hours of cooling and kept cooled overnight).

Fatty acid	PO	CCP	CGP	Milk	Yogurt	Y1-CCP	Y1-CGP	Y2-CCP	Y2-CGP	Y3-CCP	Y3-CGP
Decanoic (C10:0)	---*	---	---	0.78	1.38	---	---	---	---	---	---
Lauric (C12:0)	---	0.03	0.02	1.95	2.20	0.45	0.09	---	---	---	---
Myristic (C14:0)	0.06	0.06	0.05	9.56	10.03	2.08	0.29	---	---	---	1.61
Palmitic (C16:0)	32.40	32.55	32.62	29.71	29.26	32.63	33.69	32.49	32.35	34.67	34.30
Palmitoleic (C16:1)	0.41	0.44	0.44	2.35	2.16	0.62	0.43	0.42	---	---	---
Stearic (C18:0)	1.74	1.73	1.73	13.95	13.40	4.71	4.02	2.02	2.07	2.08	3.53
cis-9-Oleic (C18:1 w9)	61.25	61.22	61.06	30.38	30.06	55.20	57.14	61.64	60.28	63.24	58.56
Linolelaid (C18:2 trans-w6)	---	---	---	0.28	0.34	---	---	---	---	---	---
gamma-linoleic (C18:2 w6)	2.23	2.16	2.19	0.31	0.24	2.07	2.24	2.02	---	---	2.00
cis-11-eicosenoic (C20:1 w9)	0.73	0.71	0.72	0.41	0.25	0.66	0.72	0.94	---	---	---
Linolenic (C18:3 w3)	0.39	0.37	0.37	1.08	1.20	0.43	0.42	0.47	---	---	---
Saturated	34.20	34.37	34.42	54.95	56.27	39.87	38.09	34.51	34.42	36.75	39.44
Unsaturated	62.39	62.37	62.22	33.14	32.47	56.48	58.29	63.00	60.28	63.25	58.56
Polyunsaturated	2.62	2.53	2.56	1.67	1.78	2.50	3.00	2.49	---	---	2.00
Other/unidentified	0.79	0.73	0.80	10.24	9.48	1.15	0.62	0.00	5.30	0.00	0.00

* Fatty acid values not identified

4. CONCLUSIONS

The microcapsules of pequi oil produced by complex coacervation using CCP and CGP as wall materials showed a good potential for producing oil-enriched yogurts. The combined results of oil release from the particles under the different conditions studied were important to determine their application in the yogurt food matrix, given that other matrices can promote an immediate capsule release due to pH (very acidic or basic) for example, or during the manufacturing process due to high temperature. The microcapsules showed better resistance to disintegration at pH range from 4 to 5 and at temperature below 80 °C. The study of the best moment to add the microcapsules during the manufacture of the yogurt was equally important to ensure greater capsule integrity and yogurt quality. The result of our work is encouraging, and it is possible that the microencapsulation methodology used for CCP and CGP may be adapted to other pertinent food systems in the future. Efficiency, stability, and fatty acid profile analyzes indicated that the CCP microcapsules provided higher protection to pequi oil than CGP.

ACKNOWLEDGMENT

Mention of trade names or commercial products in this publication is solely for the purpose of providing specific information and does not imply recommendation or endorsement by the U.S. Department of Agriculture. USDA is an equal opportunity provider and employer.

Funding: This research received no external funding.

Conflicts of Interest: The authors declare no conflict of interest.

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4.3 CAPÍTULO III - Yogurts supplemented with pequi oil microcapsules: Effects on physicochemical properties, stability, in vitro digestion and bioaccessibility

Revista: International Dairy Journal INSS 0958-6946

Qualis: A2

Fator de impacto: 3.032

Yogurts supplemented with pequi oil microcapsules: Effects on physicochemical properties, stability, in vitro digestion and bioaccessibility

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Abstract: Microcapsules can improve the protection of bioactive compounds in pequi oil and mask the smell and taste inherent for application in yogurt. This work was evaluated the influence of pequi oil microcapsules on the physicochemical characteristic of yogurt and other aspects of stability, digestion, and bioaccessibility by analysis of beta-carotene present in the oil. In the 28 days of storage, pH values decreased from 4.5 to 4.32 for all formulations, but total solids values increased (>11%) and syneresis decreased (<50%) due to retention of water caused by the biopolymers of the microcapsules. The stability, in vitro digestion, and bioaccessibility of beta-carotene, obtained better results in the formulations containing the microencapsulated oil. The microcapsules influenced positively the physicochemical properties of the yogurt. Finally, the importance of microencapsulation technology in the protection of beta-carotene of the pequi oil was verified, as well as the controlled release, which contributes to increasing its bioaccessibility.

Keywords: Complex coacervation; Pequi oil; Beta-carotene; Biopolymers; Yogurt

1. Introduction

Yogurts are the most popular dairy products resulting from chemical acidification or slow lactic fermentation of milk lactose by starters cultures strains of *Streptococcus thermophilus* e *Lactobacillus delbrueckii* subsp. *bulgaricus* (Gharibzahedi & Chronakis, 2018; Ladjevardi, Gharibzahedi, & Mousavi, 2015). Due to its high consumption, it can be a good carrier to ensure and improve the daily intake of nutrients and consequently to cause positive impacts on the health of consumers (Silva et al., 2019). However, yogurt is not considered a rich source of bioactive compounds (Ozturkoglu-Budak, Akal, & Yetisemiyen, 2016), being the addition of these compounds very interesting. Yogurts that offer more health benefits due to the presence of bioactive compounds have gained market share, increasing the consumer acceptance (Mohammadi-gouraji, Soleimanian-zad, & Ghiaci, 2019).

Pequi oil has stood out as a natural material from plant for the food and pharmaceutical industry due to its excellent quality associated with high levels of unsaturated fatty acids, predominantly oleic (60.6%) (Pessoa et al., 2015), and carotenoids (Pinto et al., 2018). Due to the presence of these bioactive, it is widely used in popular medicine to treat various health disorders such as respiratory diseases, edema, eye problems related to low vitamin A , burns, wound healing, bruises, swelling and menstrual disorders (Ombredane et al., 2020). Pequi has great potential to be explored as a source of nutrients (Magalhães, Sá, Cardoso, & Reis, 2019), even with a strong aroma and smell. For this reason, the use of microencapsulation methods can mask the strong flavor of the pequi oil, in addition to protecting the bioactive compounds and promoting their controlled release.

Beta-carotene is found in pequi oil (about 270 $\mu\text{L g}^{-1}$ of oil) and is an important vitamin A source. It has a crucial role in human health, such as improving immunity, decreasing the risk of heart disease and increasing gastrointestinal functions (Geng et al., 2022; Xie et al., 2021). Several carotenoids, including beta-carotene, are produced on an industrial scale and are available in fortified foods or as supplements. However, carotenoids have a non-polar structure and highly unsaturated molecules making them susceptible to oxidation and isomerization during processing or storage (Šeregelj et al., 2021), therefore, several recent studies use microencapsulation technology to promote its stability and bioaccessibility (Girón-Hernández, Gentile, & Benlloch-Tinoco, 2021; Lin, Wu, Singh, & Ye, 2021; Niu, Shao, Feng, Qiu, & Sun, 2020).

Complex coacervation microencapsulation is used to encapsulate bioactive compounds and sustain their release under various conditions. Animal proteins, plant proteins and

polysaccharides are widely used during complex coacervation process (Muhoza et al., 2021). As it is a highly recommended technique for the microencapsulation of lipophilic substances, several studies use it to encapsulate vegetable oils (Silva et al., 2018; Nascimento et al., 2020; Timilsena, Akanbi, Khalid, Adhikari, & Barrow, 2019). In complex coacervation, the associative electrostatic interactions of two oppositely charged polyelectrolytes, initially soluble in water, undergo reciprocal and reversible complexation upon changes in temperature and/or pH, producing a complex of insoluble hydrophilic macromolecules (González-Monje, García, Ruiz-Molina, & Roscini, 2021).

The composition of microcapsules wall material make a crucial role in the physicochemical, rheological, morphological, microbial and sensory properties of the final product (Gumus & Gharibzahedi, 2021), as well as the chosen food matrix influences the stability and bioaccessibility of the bioactive compound of interest (Donhowe, Flores, Kerr, Wicker, & Kong, 2014). Therefore, this work evaluated the influence of the addition of pequi oil microcapsules on the physicochemical and morphological properties of yogurt. Subsequently, the stability of the encapsulated and non-encapsulated bioactive compounds in the yogurt was verified during the storage time. Finally, the release profile during *in vitro* gastrointestinal digestion and the bioaccessibility of beta-carotene was determinate of the microcapsules into the product. Microencapsulated pequi oil was obtained by complex coacervation using two polysaccharides' combinations of wall materials, cashew gum/chitosan and cashew gum/gelatin.

2. Materials and methods

2.1. Materials

Cashew gum (CG) polysaccharides were obtained from the exudate of *Anacardium occidentale* L., collected from cashew trees in the Pacajus experimental field of Embrapa Agroindústria Tropical. Polysaccharide isolation was performed using the methodology previously described by Silva et al. (2018). Chitosan (CT), of low molecular weight and 75-85% deacetylated was purchased from Sigma-Aldrich and bovine gelatine 225H type B was provided by Rousselot® (The Netherlands). The culture of the microorganism was purchased commercially by Bio Rich ® (*Lactobacillus acidophilus* LA-5 1x10⁶ UFC/g, *Bifidobacterium* BB-12 1x10⁶ UFC/g e *Streptococcus thermophilus*). The beta-carotene (beta-carotene; ≥93%, UV), Porcine gastric mucosa pepsin (P7000), porcine bile extracts (B8631) and porcine pancreatin (P7545, 8 × USP specifications) were purchased from Sigma-Aldrich.

2.2. Extraction of oil from pequi pulp

The pequi fruits (*Caryocar coriaceum* Wittm.) were washed, sanitized (Chlorine 200 ppm for 30 min), peeled and submitted to a hammer pulper (capacity 300 kg h⁻¹). The pulp was stored in plastic containers and kept in a freezer until oil extraction. For the extraction of pequi oil (PO), the pulps were heated to 45 °C and centrifuged at 4,500 rpm for 15 min to separate the oil (Lima et al., 2019).

2.3. Microcapsules formation

The microcapsules were obtained by complex coacervation, using CG/CT and CG/GE as wall materials.

The CG/CT microcapsules with the PO (CCP) were prepared according to the methodology described by Silva et al. (2018). For each homogenization step an ultra turrax (IKA T-25 digital) was used for 3 min at 10,000 rpm. Initially, the emulsions were prepared from 100 mL of CT (0.5% w/v) in deionized water (acetic acid 2% w/v) with 2 g of PO and homogenization. Then was added 100 mL of solution of CG (11% w/v) in water and homogenization. Finally, 400 mL of water were added and homogenized.

For the preparation of CG/GE microcapsules with the PO (CGP), initially a solution of 100 mL of GE (2% w/v) and a solution of 100 mL of CG (4% w/v) in deionized water were prepared according to methodology described by Nascimento et al. (2020). In the GE solution, 2 g of PO was added and homogenized, then it was added to the CG solution and homogenized again, and finally, 400 mL of deionized water was added and homogenized.

After preparing the CCP and CGP emulsions, the pH was adjusted to 4.5 and cooled (5 °C) overnight. The solutions containing the microcapsules were centrifuged (Heraeus Multifuge X3R) at 15,303xg for 10 min at 25 °C, removing excess water, and frozen in an ultra-freezer (-80 °C) for 24 hours. The frozen materials were taken to the freezer-drying (Lioto LP 820) until complete drying and was realized dispersion in an impact mill (IKA A11 basic).

2.4. Yogurt preparation

Ultra-high temperature (UHT) liquid whole milk was used according to the methodology applied by Yu et al. (2021) with modification. The milk was heated to 43 °C and added to the microorganism culture at a concentration of 0.4 g L⁻¹ (w/v). The milk was kept in an oven (43 °C) until clot formation at pH 4.5 (approximately 4h). After the coagulation time, the yogurt

was cooled ($4\text{ }^{\circ}\text{C}$) overnight for later addition of pequi oil microcapsules and pure oil. Four yogurt formulations were obtained, where Y-C is the control yogurt without additions; Y-PO is yogurt added with 0.8% (w/w) pure oil; Y-CCP is yogurt added with 2.4% (w/w) of CCP microcapsules; Y-CGP is yogurt added with 1.7% CGP microcapsules (Figure 1). The calculations for additions of microcapsules and pure oil to yogurt were in accordance with the roles of the National Health Surveillance Agency (ANVISA) that recommends daily intake of vitamin A of 600 μg for adults and 375–500 μg for children (Brazil, 2005), where 1 μg of beta-carotene is equivalent to 0.167 μg of retinol (vitamin A). Yogurt samples were stored in refrigeration ($4\text{ }^{\circ}\text{C}$) and analyzed at storage times of 1, 7, 14, 21, 28 days.

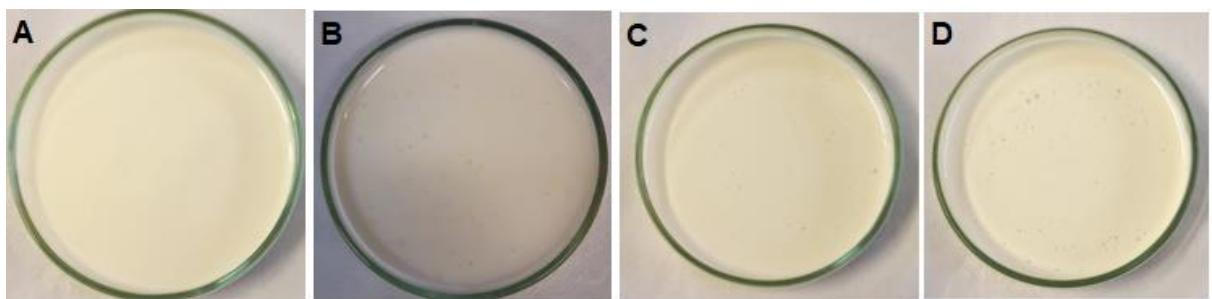


Figure 1: A) Y-C is the control yogurt without additions; B) Y-PO is yogurt added with 0.8% (w/w) pure oil; C) Y-CCP is yogurt added with 2.4% (w/w) of CCP microcapsules; D) Y-CGP is yogurt added with 1.7% CGP microcapsules.

2.5. Characterization of yogurt

2.5.1. pH

The pH of the samples was analyzed using a pH meter (mPA210, MS Tecnopon®) and a viscous liquid electrode (Analyser® 2A09E). In a beaker, 50 g of yogurt samples were weighed and analyzed during the storage period.

2.5.2. Total solids

The total solids amount of all yogurts was measured according to the AOAC 990.20 method (AOAC, 2000). Yogurt samples (2 g) were dried in a hot air oven at $105\text{ }^{\circ}\text{C}$ for 24 h, and the residues were weighed. The total solid (%) was calculated as the percentage weight of residual dry matter over the initial weight of the yogurt sample.

2.5.3. Syneresis

The amount of syneresis was realized according to method described by Akgün et al. (2019), with modification. 20 g yogurt was centrifuged for 10 min at 4000 rpm at 20 °C. The supernatant was removed and weighed. Syneresis (%) was expressed as the percentage weight of the supernatant over the initial weight of the yogurt sample.

2.5.4. Colorimetry

For colorimetric analysis, all yogurts during storage were monitored. For color measurement, yogurt samples (20 g) were placed in a petri dish, and the values of L* (light), a* (red/green) and b* (yellow/blue) were obtained using a colorimeter ChromaMeter CR-400 (Konica Minolta, Sensing, INC, Japan). The total color difference (ΔE), at 28 days of storage, was obtained by equation 1.

$$\Delta E = [(\Delta L^*)^2 + (\Delta a^*)^2 + (\Delta b^*)^2]^{1/2} \quad (\text{Eq. 1})$$

2.5.5. Morphology

A drop of yogurt was placed on the slides and covered with coverslips. Optical micrographs were performed using a Zeiss optical microscope coupled to a digital image acquisition system using a CCD camera. Yogurt micrographs were also obtained by transmission electron microscopy (TEM) (Model Vega 3, Tescan). An aliquot of yogurt was placed on a carbon-coated copper grid and allowed to stand for 3 min. Then, the sample was stained with phosphotungstic acid (0.4% w/v) for 3 min and the excess removed with filter paper. The TEM analysis was performed at an accelerating voltage of 30 kV.

2.5.6. Texture profile analysis

Texture profile analysis (TPA) was performed using a TA-TX2i texturometer (Stable Micro Systems Ltd., Surrey, England), equipped with a 30 kg load cell. 20 g of each yogurt sample was placed in three different bottles, forming an analytical triplicate. These samples were analyzed at a temperature of 7 ± 2 °C, using a P0.5 probe in two cycles of 40% penetration. The test speed was 1 mm s⁻¹, with a 2 g trigger. The parameters of hardness, springiness, cohesiveness, gumminess, and chewiness were calculated.

2.5.7. Rheology

The viscosity of yogurts was analyzed using a HAAKE MARS III rheometer (Thermo Scientific). The yogurt sample was loaded onto the cone plate geometry (C35/2° Ti L) and 0.105 mm gap with the temperature maintained at 4 °C. The viscosity flow curve was determined logarithmically increasing the frequency from 0.1 s⁻¹ to 100 s⁻¹ and descents from 100 s⁻¹ to 0.1 s⁻¹ controlled by the Haake Rheowin Job Manager software. The samples were conditioned for 5 min at 4 °C to recover the yogurt structure and the readings were carried out in a time of 5 min each. Apparent viscosity was measured at a shear rate of 1 s⁻¹. The pseudoplasticity of the yogurt samples was determined using the following power law model (Ostwald-de Waele) (Eq. 2):

$$\tau = k(\gamma)^n \quad (\text{Eq. 2})$$

2.6 Beta-carotene stability

The beta-carotene (BC) stability present in the Y-PO, Y-CCP and Y-CGP formulations was analyzed during the 28-day storage period. In 50 g of each yogurt formulation, 100 mL of 4M HCl was added to extract the oil (during 4h). After, 10 mL of hexane was added and centrifuged (15,303xg for 10 min at 25 °C) to capture the supernatant oil. The collected organic phase was dried under a stream of nitrogen, where 50 mg of the oil was redissolved in 5 mL of hexane to quantify BC. The stability of BC was expressed as a percentage (%), by the ratio of the BC amount calculated over the storage time over the initial BC amount.

2.6.1 Beta-carotene quantification

BC quantification was evaluated in a spectrophotometer (Varian Carry 50) at 450 nm. A standard curve was obtained $y = 0.1536x - 0.0351$ with R^2 of 0.99 from 1 mg of BC in 100 mL of hexane (10 µg mL⁻¹). Results were expressed as µg BC g⁻¹ oil sample.

2.7 Beta-carotene release profile in simulated *in vitro* gastrointestinal digestion

The digestion behavior of BC present in pequi oil (encapsulated and non-encapsulated) applied in yogurt were evaluated using a two-stage *in vitro* static digestion model (Chen et al. (2020), Rutz et al. (2017) with modification). In 10 g of yogurt were added 10 mL (1:1 w/v) of simulated gastric fluid (SGF) (pH 2.0, NaCl 0.15 M) containing 3.2 mg mL⁻¹ of pepsin and kept in a shaker incubator (Sola SL222) at 150 rpm, 37 °C for 1 h. After SGF incubation, the mixture was immediately adjusted to pH 7.0 using 2.5 M NaOH and 20 mL (1:1 v/v) of

simulated intestinal fluid (SIF) (pH 7.0, CaCl₂ 5 mM), containing 8 mg mL⁻¹ bile salts and 1 mg mL⁻¹ pancreatin. The mixture was incubated and shaken at 150 rpm for 2 h at 37 °C.

In the SIF step, beta-carotene release was analyzed at 5 different time intervals (0, 30, 60, 90 and 120 min). Hexane was added and the mixture was vortexed for 1 min to extract from BC. Subsequently, the samples were centrifuged at 1057 g for 3 min. The hexane-containing phase was collected and dried (the volume of hexane was adjusted to 5 mL) under a stream of nitrogen. BC release during SIF digestion was expressed as a percentage (%), by the ratio of the BC amount calculated over time to the initial BC amount.

2.8 Bioaccessibility of beta-carotene after digestion

Bioaccessibility, also known as micellization rate of BC after digestion was calculated according to the method described by Chen et al. (2020), with modifications. The material submitted to complete digestion in two stages was collected and centrifuged at 15,303xg, 4 °C, for 30 min. It was separated into three phases after centrifugation, the oil phase, the aqueous phase (micellar phase) and the sediment phase. The aqueous phase was collected and filtered. The BC in the micellar phase was extracted with methanol and hexane in a 2:3 (v/v) ratio, vortexed for 30 sec and centrifuged (15,303xg for 4 min). The upper yellow organic phase was then removed and transferred to a glass tube. The extraction process was repeated 3 times to ensure complete extraction of BC from the aqueous phase. The collected organic phase was dried under a stream of nitrogen and redissolved in 5 mL of hexane. Bioaccessibility was calculated according to the following equation 3:

$$\text{Bioaccessibility (BC)\%} = \frac{\text{BC concentration in micelles}}{\text{BC concentration in digesta}} \times 100 \quad (\text{Eq. 3})$$

2.9. Statistical analysis

Yogurt analyzes were performed in triplicate and the results are expressed as mean ± standard deviation (SD). The analyzed samples were submitted to a two-way ANOVA with a significance level of p = 0.05, using Tukey test for comparison of means. Statistical analyzes were performed using STATISTICA software version 13.0

3. Results and discussion

The supplementation of yogurts with vegetable oil microcapsules, which have a bioactive composition of interest, has been widely implemented, offering greater health benefits and

7better acceptance by consumers. In this work, the production of yoghurt supplemented with pequi oil microcapsules was carried out, using two different combinations of wall materials (CCP and CGP). The influence of microcapsules on the yoghurt matrix was verified by pH, total solid, syneresis, color, texture, and rheology analyses. Subsequently, the stability, in vitro digestion and bioaccessibility of beta-carotene present in pequi oil was evaluated.

3.1. pH, total solids and syneresis

The effect of the incorporation of CCP and CGP microcapsules into yogurt during the storage period was evaluated by pH, total solids, and syneresis analysis (Table 1).

The pH values ranged from 4.5 to 4.32 during the 28-day storage period. In all yogurt formulations studied, the pH values decreased significantly ($p>0.05$) in the first 14 days of storage, maintaining these values until 28 days. According to Estrada, Boeneke, Bechtel, & Sathivel (2011) the decrease in pH may be related to the persistent metabolic activity of microorganisms, also called post-acidification. Post-acidification or post-fermentation acidification is an unwanted process in fermented dairy products that refers to continuous acidification beyond its ideal range due to the persistent metabolic activity of the microflora into product during its shelf life (Deshwal, Tiwari, Kumar, Raman, & Kadyan, 2021).

The addition of encapsulated and non-encapsulated pequi oil not changed the pH in relation to the control, but the greater initial decrease can be considered by the presence of elements that made the metabolic activity of microorganisms more favorable (Ladjevardi et al., 2015). Fat content in yogurt formulation facilitates substrate inhibition for microorganism growth and activity and therefore lowers the pH value. Baba et al. (2018) also observed a decrease in pH, especially during the first 15 days of storage, of yogurts fortified with walnut oil emulsions and linseed with guar gum.

Comparing the syneresis values of the yogurt formulations, the yogurts added with microcapsules obtained lower values than the Y-C and Y-PO, showing the interference of the addition of biopolymers in the yogurt matrix. Syneresis values noted changed during the storage time considering each treatment of yogurt. The presence of biopolymers causes a stabilization of the yogurt's three-dimensional network, reducing the diffusion or separation rate of whey in yogurts (Gharibzahedi & Chronakis, 2018). Akgün et al. (2019) and Yu et al. (2021) obtained similar results and reported that the lower syneresis results are due to water retention caused by the biopolymers used.

Table 1: Effect of the incorporation of pequi oil and pequi oil microcapsules on the pH, total solids and syneresis of yogurts, where: Y-C is the control yogurt, Y-PO yogurt added with pequi oil; Y-CCP yogurt added with pequi oil microcapsules using cashew/chitosan gum and Y-CGP yogurt added with pequi oil microcapsules using cashew gum/gelatin.

	Properties	Yogurts	Day 1	Day 7	Day 14	Day 21	Day 28
pH	Y-C	4.50 ± 0.01 ^{aA}	4.40 ± 0.01 ^{aB}	4.34 ± 0.01 ^{abC}	4.34 ± 0.01 ^{aC}	4.34 ± 0.01 ^{aC}	
	Y-PO	4.44 ± 0.02 ^{bA}	4.36 ± 0.01 ^{bB}	4.36 ± 0.01 ^{bB}	4.31 ± 0.03 ^{aC}	4.33 ± 0.01 ^{aBC}	
	Y-CCP	4.47 ± 0.01 ^{abA}	4.39 ± 0.01 ^{aB}	4.34 ± 0.01 ^{abCD}	4.31 ± 0.02 ^{aC}	4.36 ± 0.01 ^{bD}	
	Y-CGP	4.46 ± 0.01 ^{bA}	4.36 ± 0.01 ^{bB}	4.32 ± 0.01 ^{aC}	4.30 ± 0.01 ^{aC}	4.32 ± 0.01 ^{aC}	
	Total solids (%)	Y-C	11.82 ± 0.02 ^{aA}	10.71 ± 0.11 ^{aA}	9.66 ± 0.09 ^{aB}	8.63 ± 0.09 ^{aB}	10.55 ± 0.05 ^{abAB}
		Y-PO	10.20 ± 0.26 ^{bA}	9.80 ± 0.13 ^{bA}	11.28 ± 0.15 ^{bB}	10.81 ± 0.15 ^{bC}	10.53 ± 0.25 ^{abc}
		Y-CCP	10.36 ± 0.41 ^b	10.85 ± 0.18 ^a	11.87 ± 0.19 ^b	11.67 ± 0.37 ^c	11.61 ± 0.31 ^a
		Y-CGP	11.41 ± 0.21 ^{aA}	10.64 ± 0.10 ^{aAB}	11.62 ± 0.30 ^{bA}	11.44 ± 0.01 ^{cA}	9.39 ± 0.14 ^{bb}
	Syneresis (%)	Y-C	59.33 ± 0.08 ^{aA}	55.93 ± 0.23 ^{aB}	56.25 ± 0.41 ^{aB}	56.52 ± 1.20 ^{aB}	57.53 ± 1.91 ^{aAB}
		Y-PO	57.63 ± 0.06 ^{bA}	56.22 ± 0.03 ^{aA}	57.38 ± 0.12 ^{aA}	57.63 ± 0.12 ^{aA}	57.83 ± 1.49 ^{aA}
		Y-CCP	44.28 ± 0.43 ^{cA}	44.67 ± 0.48 ^{bA}	46.90 ± 0.61 ^{bB}	47.63 ± 1.44 ^{bB}	47.73 ± 0.76 ^{bB}
		Y-CGP	45.30 ± 0.43 ^{dA}	44.47 ± 1.85 ^{bA}	44.35 ± 1.73 ^{cA}	44.33 ± 0.66 ^{cA}	45.30 ± 2.08 ^{ba}

Different lowercase letters show a significant difference ($p < 0.05$) between the columns of each property. Different capital letters show a significant difference ($p < 0.05$) between lines for each property.

3.2. Colorimetry

The color parameters L*, a* and b* obtained can vary from white (100) to black (0), from green (-) to red (+) and from blue (-) to yellow (+), respectively, according to presented in Table 2. Comparing the results of L* of the Y-C and Y-PO formulations, it was observed a significant decrease ($p > 0.05$) during the storage time, different from the formulations with microcapsules, which obtained better stability of the L* values. No relationship apparent between the presence and/or absence of microcapsules and non-encapsulated bioactive compounds and brightness values was found in this work, a similar result obtained by Comunian et al. (2017).

Table 2: Color parameters, where: Y-C is the control yogurt, Y-PO yogurt added with pequi oil; Y-CCP yogurt added with pequi oil microcapsules using cashew/chitosan gum and Y-CGP yogurt added with pequi oil microcapsules using cashew gum/gelatin.

Color	Yogurts	Day 1	Day 7	Day 14	Day 21	Day 28
L*	Y-C	92.19 ± 0.77 ^{aA}	89.5 ± 0.94 ^{aB}	96.8 ± 0.60 ^{aC}	88.63 ± 0.66 ^{abB}	88.66 ± 0.36 ^{aB}
	Y-PO	91.37 ± 0.59 ^{abA}	100.34 ± 0.25 ^{bB}	95.96 ± 0.66 ^{aC}	91.96 ± 0.81 ^{cA}	88.57 ± 0.44 ^{aD}
	Y-CCP	90.47 ± 0.23 ^{bA}	98.86 ± 0.59 ^{cB}	93.99 ± 0.96 ^{bC}	89.4 ± 0.50 ^{bA}	90.33 ± 0.43 ^{bA}
	Y-CGP	90.42 ± 0.31 ^{bA}	96.75 ± 0.62 ^{dB}	95.25 ± 0.98 ^{abB}	87.85 ± 0.82 ^{aC}	90.32 ± 0.79 ^{bA}
a*	Y-C	-1.24 ± 0.05 ^{aA}	-1.39 ± 0.17 ^{aA}	-1.36 ± 0.43 ^{abA}	-1.12 ± 0.08 ^{aA}	-1.03 ± 0.32 ^{aA}
	Y-PO	-2.2 ± 0.14 ^{bA}	-1.96 ± 0.25 ^{bA}	-1.71 ± 0.36 ^{aAB}	-1.45 ± 0.17 ^{aB}	-1.22 ± 0.14 ^{abB}
	Y-CCP	-0.95 ± 0.15 ^{acAB}	-0.71 ± 0.13 ^{cA}	-0.81 ± 0.18 ^{bAB}	-1.17 ± 0.3 ^{aB}	-1.68 ± 0.1 ^{bC}
	Y-CGP	-0.95 ± 0.18 ^{cAB}	-0.59 ± 0.3 ^{cA}	-0.94 ± 0.27 ^{bAB}	-1.24 ± 0.34 ^{aB}	-1.48 ± 0.25 ^{abB}
b*	Y-C	13.3 ± 0.52 ^{aA}	14.61 ± 0.2 ^{aB}	12.47 ± 0.40 ^{aA}	15.12 ± 0.07 ^{aB}	15.45 ± 0.52 ^{abB}
	Y-PO	15.8 ± 0.94 ^{bAB}	15.59 ± 0.99 ^{aAB}	14.55 ± 0.69 ^{bA}	15.27 ± 0.36 ^{aAB}	16.7 ± 0.67 ^{aB}
	Y-CCP	14.34 ± 0.47 ^{acA}	15.29 ± 0.33 ^{aA}	15.04 ± 0.28 ^{bA}	14.45 ± 0.75 ^{aA}	12.08 ± 0.63 ^{cB}
	Y-CGP	14.73 ± 0.29 ^{bcA}	15.56 ± 0.85 ^{aA}	14.39 ± 0.94 ^{bA}	12.46 ± 0.66 ^{bB}	14.23 ± 0.98 ^{bA}

Different lowercase letters show a significant difference ($p < 0.05$) between the columns of each property. Different capital letters show a significant difference ($p < 0.05$) between lines for each property.

The a* parameter had negative results, showing a slight tendency to greenish color and the b* had positive results, showing the yellowish hue, with greater results for the formulation with the non-encapsulated oil. Thus suggesting that the addition of microcapsules offers improves, in terms of maintaining the original color appearance of the yogurt, as also was shown by Tan et al. (2017).

Regarding the total color difference (ΔE), values of 4.14, 3.10, 2.38 and 0.74 were obtained for the formulations Y-C, Y-PO, Y-CCP and Y-CGP, respectively. The highest values obtained may be related to higher whey separation in the formulations without microcapsules (Y-C and Y-PO).

3.3. Morphological characterization

Micrographs of samples yogurt were obtained by optical microscopy (Figure 2 A, B and C) and transmission electronics microscopy (TEM) (Figure 2 D, E and F).

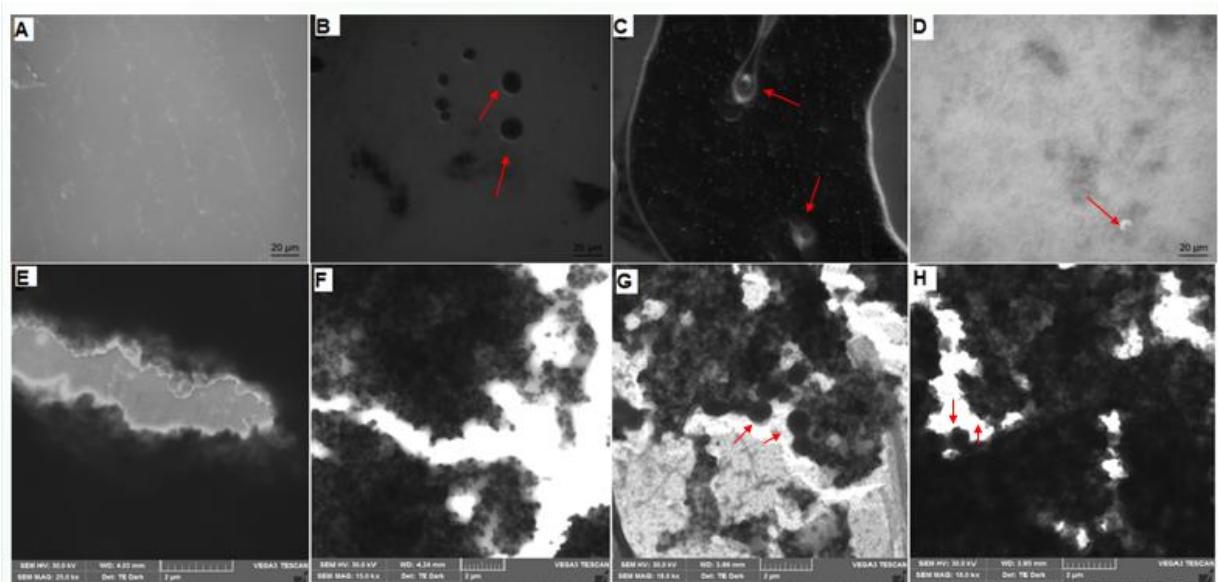


Figure 2: Optical microscopy micrographs of yogurt formulations, where A is control yogurt (Y-C), B is yogurt added with pequi oil (Y-PO), C yogurt added with pequi oil microcapsules, using cashew gum/ chitosan (Y-CCP) and D is yogurt added to pequi oil microcapsules using cashew gum/gelatin (Y-CGP). Transmission electron microscopy micrographs (TEM) of yogurts, where E is Y-C, F is Y-PO, G is Y-CCP, and H is Y-CGP.

Observing Figures 2 A and D (control yogurt formulation Y-C) a dense structure was visualized, since that these formulations were not submitted to mechanical stress for homogenization of the added materials. The dark areas observed correspond to the protein structure of the yogurt and the small size structures observed in the yogurt samples are related to the fat globules, which are characteristic of dairy products such as yogurt (Campo et al., 2019)

In figure 2 B, it is possible to observe the presence of microparticles of non-encapsulated oil from the Y-PO formulation. The denser and more compact microstructures in the yogurt formulations added with microcapsules prove that there was a dispersion and not agglomeration of the microcapsules, as also was observed in the works of Comunian et al. (2017) and Yu et al. (2021).

3.4 Texture profile analysis

Texture profile analysis (TPA) of yogurt formulations during storage time are showed in Figure 3. Elasticity and cohesiveness were the characteristics that had not significant difference ($p < 0.05$) between the formulations and the storage time.

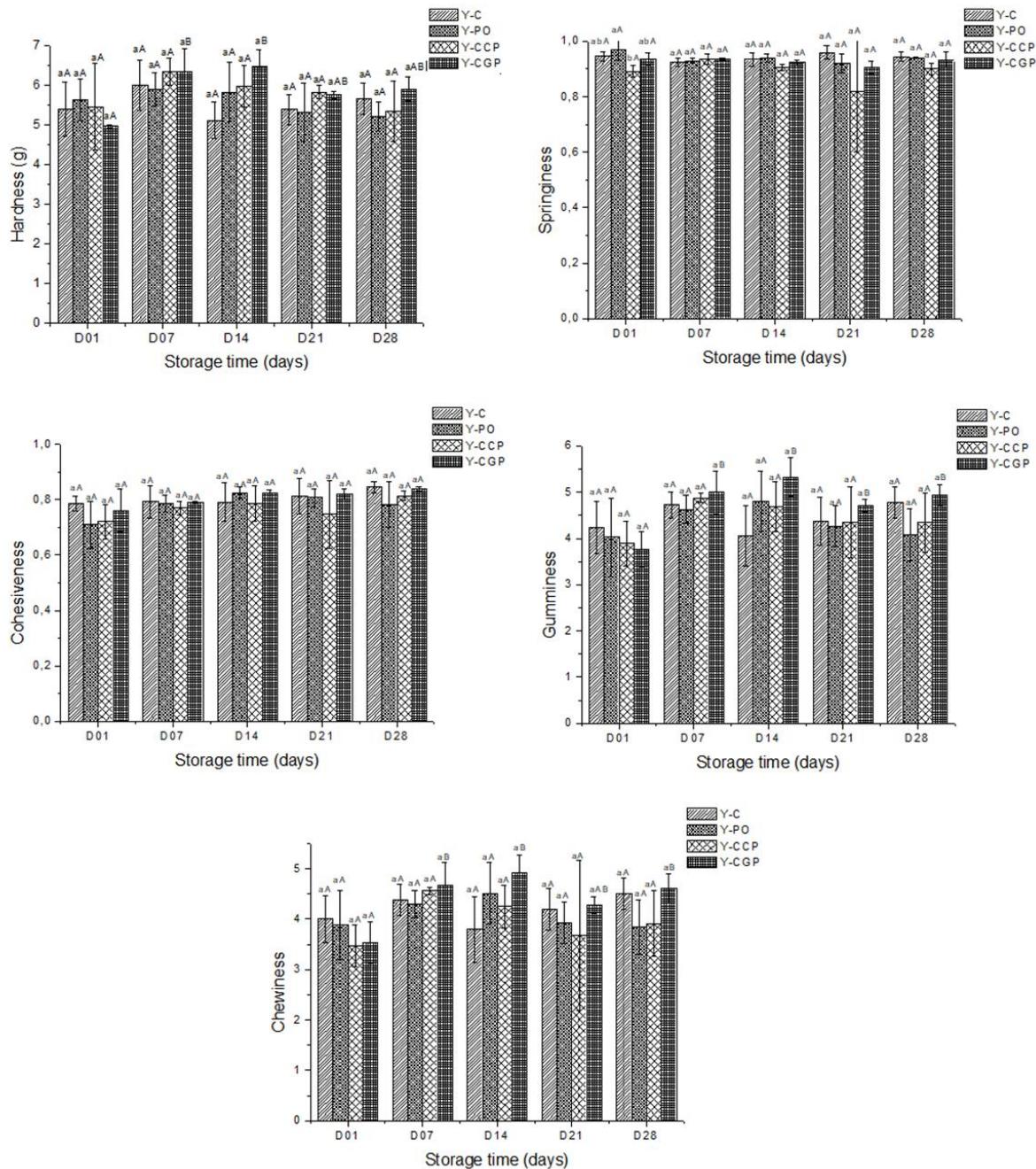


Figure 3: Texture profile analysis (TPA) of yogurt formulations, where Y-C is the control yogurt, Y-PO is the yogurt added with pequi oil, Y-CCP is the yogurt added with pequi oil microcapsules, using the gum cashew/chitosan and Y-CGP is yogurt added with pequi oil microcapsules, using cashew gum/gelatin. Different lowercase and capital letters show a significant difference ($p < 0.05$).

The parameters of hardness, gumminess and chewability had a significant increase on days 7 and 14 of storage, followed by a decrease, which is related to the decrease of the pH. Lower pH influence the increase in whey production, both are decisive factors to the product quality during storage time. Ladjevardi et al. (2015) reported that an increase in the total amount of yogurt solids can improve texture properties and therefore decrease the rate of syneresis. Studies carried out by Comunian et al. (2017), Ghorbanzade, Jafari, Akhavan, & Hadavi (2017) and Tan et al, (2017) obtained similar results to this study, where the encapsulates allowed more yogurt proteins to interact with each other, forming a three-dimensional structure with greater resistance to deformation. Thus, the texture profile results were maintained over the time of storage.

3.5 Reology aspects

Yogurts are commonly classified as pseudo-plastic liquids ($n<1$), so one of the mathematical models that describe this type of liquid (non-Newtonian) is the Ostwald-de Waele. As can be seen in table 3, the R^2 values were above 0.9, thus obtaining a correlation coefficient value within the standards for applying this model. All yogurt formulations, regardless of the storage day, had fluid behavior index values (n) lower than 1, and could therefore be classified as non-Newtonian pseudo-plastic liquids.

The rheological analyzes allow to evaluate the deformations and fluxes of matter, when subjected to a certain shear rate. The apparent viscosity of yogurts decreased with increasing rate of deformation during shear. They results are agree with works realized by (Comunian et al., 2017; Tan et al., 2017) (Figure 4). In the case of the Y-C, the apparent viscosity remained stable throughout storage, it was measured at a shear rate of 1 s^{-1} . However, there was a greater difference between the Y-PO formulation on the first day of storage, compared to the rest of the days, for samples stored for 28 days, showing a negative influence of the formulation containing the non-encapsulated pequi oil. The Y-CCP and Y-CGP formulations showed higher values, comparing the 1st and 28th day of storage, due to the addition of microcapsules, which increases the solids content of the final product. In contrast to the microcapsule added to yogurt, the gel structure of the pequi oil added yogurt was weak and this eventually reduced the viscosity, increasing the yogurt's tendency to flow, shrink and expel the whey (Dai, Corke, & Shah, 2016).

Table 3: Parameters of the Ostwald-de Waele model (K , n and R^2) and apparent viscosity (η) calculated for a shear rate of 1 s^{-1} during storage time at 4°C , where Y-C is the control yogurt, Y-PO is pequi oil added yogurt, Y-CCP is pequi oil microcapsule added yogurt, using cashew gum/chitosan gum and Y-CGP is pequi oil microcapsule added yogurt, using cashew gum/gelatin.

Parameters	Yogurts	Day 1	Day 7	Day 14	Day 21	Day 28
K	Y-C	2.84	2.86	4.87	3.91	3.24
	Y-PO	2.45	1.19	1.16	1.47	1.26
	Y-CCP	1.26	1.74	1.51	2.21	1.80
	Y-CGP	43.97	1.27	5.09	6.14	5.22
n	Y-C	0.12	0.23	0.22	0.20	0.15
	Y-PO	0.37	0.37	0.31	0.37	0.30
	Y-CCP	0.30	0.40	0.34	0.36	0.42
	Y-CGP	0.52	0.53	0.26	0.28	0.20
R^2	Y-C	0.98	0.99	0.99	0.97	0.99
	Y-PO	0.85	0.96	0.95	0.95	0.99
	Y-CCP	0.99	0.96	0.95	0.98	0.92
	Y-CGP	0.96	0.83	0.98	0.77	0.98
η (mPa.s)	Y-C	3268	2710	5237	3820	3355
	Y-PO	7512	881,8	1240	1559	1252
	Y-CCP	1252	1970	1620	2336	2051
	Y-CGP	4380	1834	5387	7166	9613

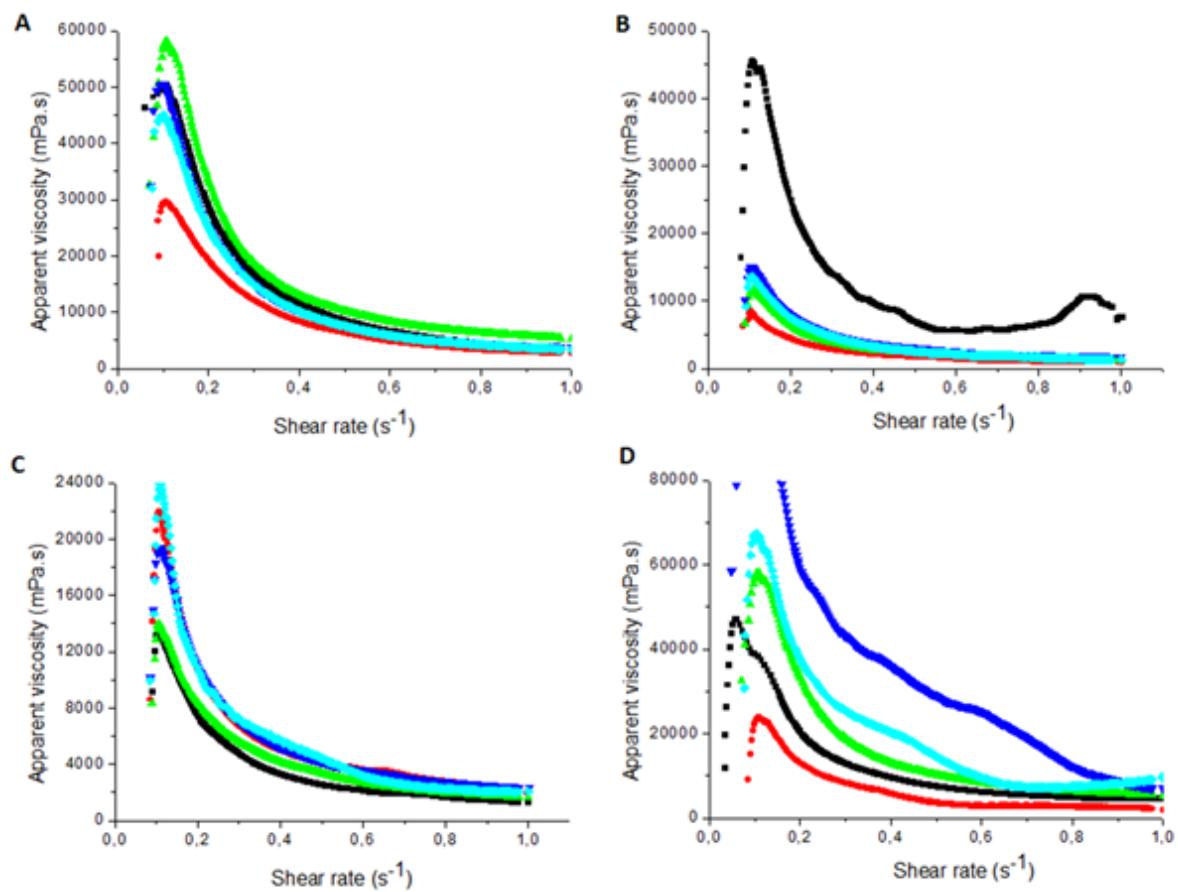


Figure 4: Shear rate x apparent viscosity ratio of yogurts made during storage time at 4 °C, where A is the control yogurt, B is the yogurt added with pequi oil, C is the yogurt added with pequi oil microcapsules, using cashew gum/chitosan and D is yogurt added with pequi oil microcapsules using cashew gum/gelatin. Where black, red, green, blue, and cyan lines represent the storage time of 1, 7, 14, 21 and 28 days, respectively.

3.6 Beta-carotene stability

The stability analysis of beta-carotene (BC) of pequi oil incorporated to yogurt formulations with encapsulated and non-encapsulated oil was performed to verify the oil protection during the 28 days of storage, as shown in Figure 5 A. In all formulations, the decrease in BC concentration was more accentuated in the first 7 days of storage, followed by a more gradual decrease up to 28 days. This BC degradation in the first days of storage occurred during the decrease in pH in the yogurt matrix, where there was a environment more favorable to for BC oxidation. Šeregelj et al. (2021) attributed that the apolar structure and highly unsaturated molecules become the carotenoids susceptible to oxidation and isomerization

during processing or storage. In this sense, the use of encapsulation technology to improve their stability is especially attractive for application in food.

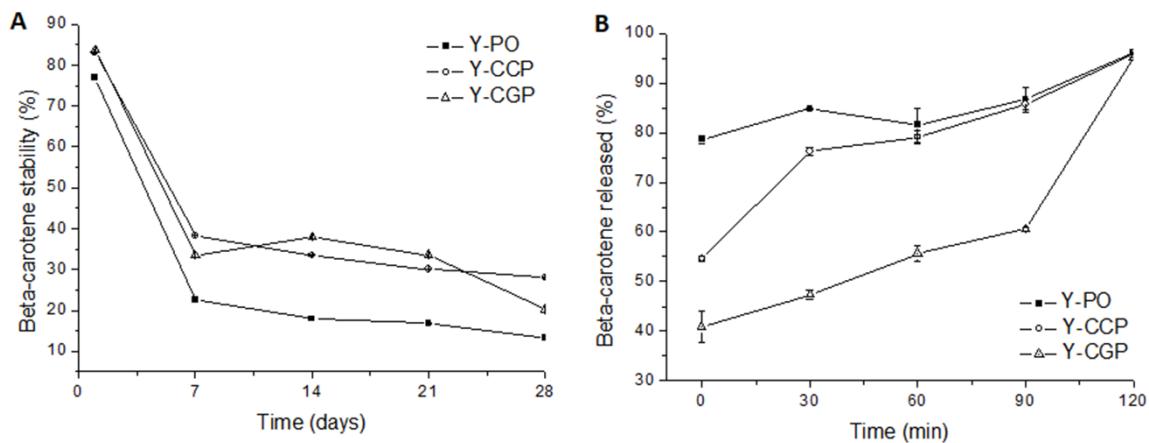


Figure 5: Concentration of beta-carotene (%) of formulations Y-PO (yogurt added with pequi oil), Y-CCP (yogurt added with microcapsules of pequi oil, using cashew/chitosan gum) and Y-CGP (yogurt added of pequi oil microcapsules, using cashew gum/gelatin), where A is the stability of beta-carotene over the 28 days of storage, and B is the release profile of beta-carotene during *in vitro* digestion.

The influence of microencapsulation on the BC protection can be proven by the higher BC concentrations at all storage times, when compared to Y-CCP and Y-CGP formulations with Y-PO formulation. At 28-day storage, beta-carotene retention was 13.26 ± 0.02 , 28.03 ± 0.08 and 20.16 ± 0.12 for the Y-PO, Y-CCP and Y-CGP formulations, respectively. Studies carried out by Campo et al. (2019) evaluated the stability of zeaxanthin nanoparticles applied in yogurts and also observed a decrease in retention during storage time, in the range of 16 to 22%, corroborating the results obtained. Šeregelj et al. (2021) observed that beta-carotene content in fortified yogurt was slightly changed during the storage period, observing decreasing trends for the tested yogurts.

3.7 Beta-carotene release profile by *in vitro* digestion

The BC release profile in a fluid that simulates gastrointestinal conditions can be seen in Figure 4 B. As expected, the formulations with microcapsules had a more gradual release, different of the formulation with only pequi oil. The formulation with CGP microcapsules had lower levels of release during up to 90 min in contact with SIF but was like Y-CCP during a

time of 120 min, when was released 96.11 ± 0.02 , 95.99 ± 0.04 and 95.16 ± 0.01 , for the Y-PO, Y-CCP and Y-CGP formulations, respectively. The non-full release is due to the fraction of beta-carotene that may have been absorbed in the digesta, which will be considered in the bioaccessibility step. Kersiené et al. (2020) verified the release kinetics of bioactive molecules during the *in vitro* digestion of the product and compared as the incorporation of the bioactive (loaded in double emulsion or added directly to the product). At the end time of the simulated intestinal condition, a complete release (approximately 100%) of the vitamins was recorded independent of the incorporation method. The fact that the Y-PO formulation not showed maximum release since the first contact with SIF can be explained by the influence of the yogurt matrix, which makes digestion difficult. During the digestion time, the matrix is destabilized and there was an increase in oil release. Rutz et al. (2017) observed that after application in food, the release of microencapsulated carotenoids from palm oil was lower and the released compounds were not degraded, indicating that food matrices can interact with bioactive compounds in different forms and protect them, even after the release of the microcapsules.

3.8. Beta-carotene bioaccessibility

Bioaccessibility was based on BC concentrations solubilized in the micellar fraction. The values obtained were 4.05 ± 0.03 , 4.18 ± 0.04 and 5.08 ± 0.01 for the Y-PO, Y-CCP and Y-CGP yogurt formulations, respectively. The low bioaccessibility values can be explained by the fact that the oil could barely be digested in the intestinal phase, due to the large droplet size and also by the highly acidic environment, which can cause BC isomerization and/or oxidation (Guo et al., 2022). The gradual released of the oil favors the formation of lower droplet and facilitates the digestion in the intestinal phase as it was verified in the Y-CGP formulation.

Several factors can influence the effectiveness of micellarization of carotenoids in the intestinal phase, including physicochemical properties, composition and interaction with other compounds in the food matrix, such as proteins, lipids and fibers (Xavier, Carvajal-Lérida, Garrido-Fernández, & Pérez-Gálvez 2018), which can affect digestive behavior and reduce the release of carotenoids, consequently, their bioaccessibility (Campo et al., 2019). Donhowe et al. (2014) evaluated the bioaccessibility of microencapsulated and free beta-carotene in yogurt and pudding. The authors reported that the incorporation of microencapsulated and free beta-carotene in micelles was lower in yogurt (0.8 and 5.5%) than in pudding (13.1 and 17%), which implies that the food matrix influenced significantly in the decrease of the carotenoids content of in the micellar phase.

5. Conclusion

The CCP and CGP microcapsules influenced the physicochemical properties (pH, total solid, syneresis, color, texture, and rheology) of the yogurt. In this work was possible to verify that wall material and oil interact with the other ingredients of the product. Sometimes, this interaction was positive bringing desirable characteristics to the product such as less syneresis. The stability of BC was considerably higher in all formulations with microcapsules during the yogurt storage, proving the importance of using microencapsulation technology in the protection of bioactive compounds. In the release profile by *in vitro* digestion, there was a gradual release of the oil, fact that increased the beta-carotene bioaccessibility, mainly observed in the Y-CGP formulation.

Funding: This research received no external funding.

Conflicts of Interest: The authors declare no conflict of interest.

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5 CONCLUSÃO

As microcápsulas de óleo de pequi produzidas por coacervação complexa usando CCP e CGP como materiais de parede mostraram um bom potencial para a produção de iogurtes enriquecidos com óleo. Ambos os materiais de parede apresentaram bons resultados de eficiência de encapsulação ($>80\%$), rendimento ($>50\%$) e capacidade de carga ($<50\%$). O FT-IR comprovou a interação eletrostática dos coacervados, confirmando a formação das microcápsulas, e o TGA, DSC e Rancimat mostraram a boa estabilidade térmica devido a interação dos materiais de parede.

As microcápsulas apresentaram melhor resistência à desintegração na faixa de pH de 4 a 5 e em temperaturas abaixo de 80 °C, resultados importantes para determinar sua aplicação na matriz alimentar de iogurte. O estudo do melhor momento para adicionar as microcápsulas durante a fabricação do iogurte foi igualmente importante para garantir maior integridade da cápsula e qualidade do iogurte. As análises de eficiência, estabilidade e perfil de ácidos graxos indicaram que as microcápsulas CCP proporcionaram maior proteção ao óleo de pequi do que o CGP.

As microcápsulas CCP e CGP influenciaram as propriedades físico-químicas (pH, sólido total, sinérese, cor, textura e reologia) do iogurte. Neste trabalho foi possível verificar que o material da parede e o óleo interagem com os demais ingredientes do produto. Às vezes, essa interação era positiva trazendo características desejáveis ao produto, como menos sinérese. A estabilidade do BC foi consideravelmente maior em todas as formulações com microcápsulas durante o armazenamento do iogurte, comprovando a importância do uso da tecnologia de microencapsulação na proteção de compostos bioativos. No perfil de liberação pela digestão *in vitro*, houve uma liberação gradativa do óleo, fato que aumentou a bioacessibilidade do beta-caroteno, observada principalmente na formulação Y-CGP.

Com isso, conclui-se que as microcápsulas de goma de cajueiro/quitosana proporcionaram uma matriz mais densa, protegendo melhor o óleo, e ao aplicar em iogurte, melhorou o perfil de ácidos graxos e promoveu a adição de um importante composto bioativo, o beta-caroteno, sendo que as formulações com as microcápsulas obtiveram melhor estabilidade e bioacessibilidade do beta-caroteno. O resultado do nosso trabalho é encorajador e é possível que a metodologia de microencapsulação usada para CCP e CGP possa ser adaptada a outros sistemas alimentares pertinentes no futuro.

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ANEXO I – ARTIGO PUBLICADO

Título do artigo: Optimization of cashew gum and chitosan for microencapsulation of pequi oil by complex coacervation.

Revista: Journal of Food Processing and Preservation **Publicação:** 42(3) e13538; 2018.

Qualis: A4

Doi: <https://doi.org/10.1111/jfpp.13538>

Received: 6 September 2017 | Revised: 29 September 2017 | Accepted: 20 October 2017
DOI: 10.1111/jfpp.13538

ORIGINAL ARTICLE

WILEY **Journal of**
Food Processing and Preservation

Institute of
Food Science
Technology **ifst**

Optimization of cashew gum and chitosan for microencapsulation of pequi oil by complex coacervation

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Funding information

CAPES

Abstract

Optimized conditions of cashew gum (CG)/and chitosan (CT) were evaluated for the encapsulation of pequi oil by complex coacervation. A comparison was established with gum Arabic (GA)/CT. At first, the coacervation process without pequi oil was performed for determining the most appropriate proportion and pH for microparticle formation. The best conditions were of 22:1 at pH 4.5 for the CG/CT, and 6:1 at pH 3.5 for the GA/CT. Pequi oil release in a pH range was higher in pH 4.5 and 5 for GA/CT and CG/CT, respectively. Microparticle yield was about 60% for both complexes. The microparticle size was 4.8 and 2.7 µm for CG/CT and GA/CT, respectively. The encapsulation efficiency was 86 and 89% for CG/CT and GA/CT, respectively. CG forms an interesting complex with CT, 22:1 ratio at pH 4.5, for a suitable encapsulation of pequi oil.

Practical applications

Pequi oil has attractive anti-inflammatory and antioxidant properties that could be used in the formulation of new cosmetics and nutraceuticals. The microencapsulation of pequi oil assists in the conservation of these properties because it avoids the direct exposure of the actives molecules to environmental factors and to the reagents and procedures involved in the preparation of a product. Complex coacervation method is recommended for the encapsulation of lipophilic substances and has the great advantage of not using high temperatures and being carried out in aqueous medium.

ANEXO II – ARTIGO PUBLICADO

Título do artigo: Pequi oil microencapsulation by complex coacervation using gelatin-cashew gum.

Revista: International Journal of Food Studies Publicação: 9; S197-S1109: 2020.

Qualis: A3

Doi: <https://doi.org/10.7455/ijfs/9.SI.2020.a8>

International Journal of Food Studies | IJFS January 2020 | Volume 9 | pages SI97–SI109

Pequi Oil Microencapsulation by Complex Coacervation using Gelatin-Cashew Gum

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Received: 23 January 2019; Published online: 18 January 2020

Abstract

New functional foods and beverages can be developed using bioactive compounds present in pequi oil. Complex coacervation is an encapsulation method used for preserving bioactive molecules, especially those that are hydrophobic or sensitive to high temperatures. The objective of this work was to produce and characterize pequi oil microparticles using cashew gum/gelatin matrix (CG/GE) through complex coacervation. Gum Arabic (GA) was also studied in comparison with CG. The coacervation process was performed without pequi oil to determine the ideal proportions of the matrix components, followed by the embedding of the oil in the microparticles for evaluation. Satisfactory microparticles were produced at pH 4.5 in the weight ratios of CG/GE = 2:1 and GA/GE = 1:3. Pequi oil release was greater in acidic pH, especially at pH 2 for the CG/GE matrix. The encapsulation efficiency for CG/GE and GA/GE was 72.53% (± 4.80) and 82.77% (± 6.09), respectively. The results showed that the CG/GE combination seemed very promising as an encapsulation matrix, especially for food applications involving pH values higher than 3.

Keywords: *Anacardium occidentale*; Coacervate; Encapsulation; Gelatin; *Caryocar coriaceum*; Polysaccharides