



## Expression, purification and use of the soluble domain of *Lactobacillus paracasei* $\beta$ -fructosidase to optimise production of bioethanol from grass fructans

C.M. Martel<sup>a</sup>, A.G.S. Warrilow<sup>a</sup>, C.J. Jackson<sup>a</sup>, J.G.L. Mullins<sup>a</sup>, R.C. Togawa<sup>c</sup>, J.E. Parker<sup>a</sup>, M.S. Morris<sup>b</sup>, I.S. Donnison<sup>b</sup>, D.E. Kelly<sup>a</sup>, S.L. Kelly<sup>a,\*</sup>

<sup>a</sup>Institute of Life Science and School of Medicine, Swansea University, Swansea SA2 8PP, Wales, UK

<sup>b</sup>Institute of Biological, Environmental & Rural Sciences, Aberystwyth University, Gogerddan, Aberystwyth SY23 3EB, Wales, UK

<sup>c</sup>Embrapa Recursos Genéticos e Biotecnologia, Laboratório de Bioinformática, Parque Estação Biológica – Final W5 norte, Caixa Postal 02372, Brasília, DF 70770-900, Brazil

### ARTICLE INFO

#### Article history:

Received 15 October 2009

Received in revised form 13 January 2010

Accepted 19 January 2010

Available online 12 February 2010

#### Keywords:

Bioethanol

Fructan

Fructanase

*Lactobacillus paracasei*

Perennial ryegrass

### ABSTRACT

Microbial inulinases find application in food, pharmaceutical and biofuel industries. Here, a novel *Lactobacillus paracasei*  $\beta$ -fructosidase was overexpressed as truncated cytosolic protein ( $\rho$ fosEp) in *Escherichia coli*. Purified  $\rho$ fosEp was thermostable (10–50 °C) with a pH optimum of 5; it showed highest affinity for bacterial levan ( $\beta$ [2-6] linked fructose) followed by nystose, chicory inulin, 1-kestose ( $\beta$ [2-1] linkages) and sucrose ( $K_m$  values of 0.5, 15, 15.6, 49 and 398 mM, respectively). Hydrolysis of polyfructose moieties in agriculturally-sourced grass juice (GJ) with  $\rho$ fosEp resulted in the release of >13 mg/ml more bioavailable fructose than was measured in untreated GJ. Bioethanol yields from fermentation experiments with Brewer's yeast and GJ +  $\rho$ fosEp were >25% higher than those achieved using untreated GJ feedstock (36.5[±4.3] and 28.2[±2.7] mg ethanol/ml, respectively). This constitutes the first specific study of the potential to ferment ethanol from grass juice and the utility of a novel core domain of  $\beta$ -fructosidase from *L. paracasei*.

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### 1. Introduction

The use of plant biomass for the production of carbon-neutral biofuels continues to attract investment from research and commercial sectors (Larsen et al., 2008; Schmer et al., 2008). Industrially viable strategies to optimise the release of energy from cellulosic and lignocellulosic fractions of plant material (Hendriks and Zeeman, 2009 for recent review) continue to constitute a focal point for biofuel research (e.g. bioethanol from lignocellulosic biomass; Larsen et al., 2008). However, consideration of the complete spectrum of plant biomass that could be used for the production of bioethanol highlights additional reservoirs of carbon-energy; plant fructans comprise one of these sources.

In addition to sucrose and starch, fructans contribute to the pool of storage carbohydrates in plants (Ritsema and Smeekens, 2003). The simplest plant fructan is inulin which consists of a linear chain of  $\beta$ (2-1)-linked fructose monomers that extends from the fructosyl residue of a sucrose ( $\alpha$ - $\beta$ -1-2 linked glucose and fructose) starter molecule common to all plant fructans anabolised *in vivo*. Levan-type fructans also comprise a linear chain of fructose monomers; however these are linked via  $\beta$ (2-6) bonds. Finally, mixed-type fructans (gramminans) contain both  $\beta$ (2-1) and  $\beta$ (2-6)-linked

fructose chains which can branch from the fructosyl and/or glucosyl residues of the sucrose starter molecule. Several fructan-containing plant crops including white clover (*Trifolium repens*), dandelion leaves (*Taraxacum* spp.), perennial ryegrass (*Lolium perenne* L.) and Jerusalem artichoke (*Helianthus tuberosus*) have been identified (see Kyazze et al., 2008). However, to date, few reports have been published on the production of bioethanol from plant fructans; those that are available tend to concentrate on the utilisation of *H. tuberosus* biomass (Nakamura et al., 1996; Szambelan et al., 2004). For example, it has been shown that inulin-type fructans derived from Jerusalem artichoke can be converted to ethanol by acidic hydrolysis followed by fermentation with *Saccharomyces cerevisiae* or via direct fermentation using *Kluyveromyces marxianus* strains (Negro et al., 2006). Similar research with a wider range of fructan-containing plant substrates is now required.

Given the total area (some 14 million hectares) of agricultural grassland in the UK (DEFRA, 2006), it is not surprising that perennial ryegrass has recently been identified as a possible substrate for the production of biofuels (Martinez-Perez et al., 2007). Unlike more specialist crops (e.g. wheat, sugar-beet) currently used for bioethanol production in Europe (Balat, 2007), ryegrass requires relatively few energy inputs (Donnison et al., 2009). Moreover, because of its fast establishment and robustness, ryegrass can be cultivated in marginal areas – an important consideration given the concerns surrounding use of arable land for non-food crops. The

\* Corresponding author. Tel.: +44 1792 292207; fax: +44 1792 503430.

E-mail address: [s.l.kelly@swansea.ac.uk](mailto:s.l.kelly@swansea.ac.uk) (S.L. Kelly).



ryegrass was harvested in mid-June using a Haldrop plot harvester and juiced using a Green-Star™ GS1000 twin screw juicer (Savant Distribution Ltd., UK). *L. perenne* biomass was processed at 4 °C within 2 h of harvest; all GJ extracts were stored and transported in a frozen state. Residual fibrous grass material was also frozen for use in alternative crop research trials. The typical sugar, fructan and protein composition of *L. perenne* (cv. Aberdart) has been documented elsewhere (Udén, 2006; Conaghan et al., 2008).

In our laboratory, aliquots of GJ were screened to remove large particulates, filter-sterilised (Ministart, Sartorius, 0.2 µm) and frozen (−80 °C) prior to use as a growth and fermentation substrate. When required, particle-free GJ was thawed and used to prepare six feedstock media: media 1 = untreated GJ; media 2 = GJ +  $\epsilon$ -fosEp; media 3 = GJ + heat-denatured  $\epsilon$ -fosEp (GJ +  $^{hd}$  $\epsilon$ -fosEp); media 4 = GJ + commercial exo-inulinase (GJ + Exo-I); media 5 = GJ + commercial endo-inulinase (GJ + Endo-I); media 6 = GJ + commercial exo- and endo-inulinase mixture (GJ + Exo/Endo-I). When added, commercial exo- and endo-inulinases from *Aspergillus niger* (Megazyme International Ireland Ltd.) or the  $\epsilon$ -fosEp (our laboratory) were used at a final concentration of 15 µg protein/ml (N.B. media 6 = 7.5 µg/ml of each inulinase). Following the addition of active enzymes (or the  $^{hd}$  $\epsilon$ -fosEp) to GJ feedstock, 10 ml volumes were filter-sterilised and incubated (18 h, 37 °C, 180 rpm) to catalyse hydrolytic activity. To standardise all treatments, media 1 (untreated GJ) was supplemented with filter-sterilised water in place of enzyme/s. The concentrations of glucose in all media at  $t_0$ h (prior to the start of growth and fermentation experiments) were quantified using a glucose assay kit (GAGO-20, Sigma); fructose concentrations were estimated using the triphenyl tetrazolium chloride assay (Avigad et al., 1961).

### 2.2.2. Brewing strain and growth and fermentation experiments

Growth and fermentation studies were undertaken using Turbo yeast (Gert Strand AB, Sweden), a commercial brewing strain of *S. cerevisiae*. Turbo cultures were routinely cultured and maintained on YEPD medium containing (w/v): 2% glucose, 2% bacto-peptone and 1% yeast extract – including 2% agar when required (all media components supplied by Difco). Automated growth and fermentation experiments were performed in 100-well honeycomb microplates using a Bioscreen C (Oy Growth Curves Ab Ltd., Finland) to record changes in optical density (OD<sub>600</sub>) over time. Uniform starting ( $t_0$ ) population densities ( $5 \times 10^5$  cells/ml) were achieved by adding yeast from overnight cultures (washed and diluted to  $1 \times 10^7$  cells/ml) to the media of interest (50 µl cells + 950 µl media); the resulting 1 ml volumes were vortexed and aliquoted into 200 µl volume wells (four replicate wells per treatment). Semi-anaerobic fermentation conditions were achieved by sealing the microplates with lids and incubating them (without a shaking regime) at 20 °C in the Bioscreen. At  $t_{75}$ h estimations of the ethanol concentration (mg/ml) in each well were made using an ethanol assay kit (DIET-500) used in conjunction with a saccharide removal kit (DSRK-500, Bioassay Systems Ltd.). In addition to manual (Neubauer haemocytometer) cell counts at  $t_{75}$ h, optical density (OD) data were exported from the Bioscreen C in ASCII format and processed using Excel2003 (Microsoft Inc.). OD<sub>600</sub> values were first corrected (by subtracting background OD<sub>600</sub> for GJ); Excel2003 was then used to determine  $\Delta$ OD values (maximum OD<sub>600</sub> – minimum OD<sub>600</sub>) between  $t_0$ h and  $t_{75}$ h. Student's *t*-tests were used to determine any levels of ethanol production and/or population growth that were significantly higher ( $P < 0.05$ ) than those seen when Turbo yeast was grown on untreated GJ. All statistical analyses were performed using SPSS (Version 13.0).

### 2.3. Molecular modelling of *L. paracasei* $\beta$ -fructosidase

Structural modelling was carried out using a homology modelling pipeline built with the Biskit structural bioinformatics plat-

form (Grunberg et al., 2007) that peruses the entire Protein Databank of protein structures for putative structural homologues. The pipeline workflow incorporates the NCBI tools platform (Wheeler et al., 2008), including the BLAST program (Altschul et al., 1990) for similarity searching of sequence databases, T-COFFEE (Notredame et al., 2000) for alignment of the test sequence with the template, the MODELLER program (Eswar et al., 2003) for homology modelling, and the DSSP algorithm (Kabsch and Sander, 1983) for secondary structure validation. Homology models were generated with 10 iterations of the MODELLER program.

Alignment searching with the *L. paracasei*  $\beta$ -fructosidase sequence yielded 11 homologue structures (1ST8, 1UYP, 1W2T, 1Y4W, 1Y9G, 1Y9M, 2AC1, 2ADD, 2ADE, 2AEY, 2AEZ), filtered to the two with the best homology. A homology model was generated based on 31.7% sequence identity with the crystal structure of exo-inulinase from *Aspergillus awamori* (PDB: 1Y4W, chain A) (Nagem et al., 2004), and 29.4% identity with  $\beta$ -fructosidase from *Thermotoga maritima* (PDB: 1W2T, chain F) (Alberto et al., 2006). No homologue could be found for the sequence preceding residue 150. Structural models were visualized using the molecular graphics program Chimera (Pettersen et al., 2004).

## 3. Results

### 3.1. Expression and purification of the recombinant $\epsilon$ -fosEp

Expression of *fosE* (Fig. 1) in *E. coli* yielded 22.5 nmoles/l of  $\epsilon$ -fosEp. SDS-PAGE indicated an apparent molecular weight of 100 kDa for recombinant  $\epsilon$ -fosEp (Fig. 2, lane 3). Although this is 20 kDa greater than the anticipated molecular weight of 81 kDa, altered gel mobility can be caused by a poly-histidine tail (Fig. 1). Trypsin digestion and nano-LC/MS/MS analysis of a 100 kDa  $\epsilon$ -fosEp protein band identified 21 peptides that matched the deposited *fosE* protein sequence (Accession No. Q27J21). These accounted for 26% and 51% of the peptide composition of full-length and truncated *fosE* proteins; a Mascot score of 3609 (scores >1000 being largely unequivocal) confirmed the identity of  $\epsilon$ -fosEp.

### 3.2. Biochemical characterisation of the $\epsilon$ -fosEp

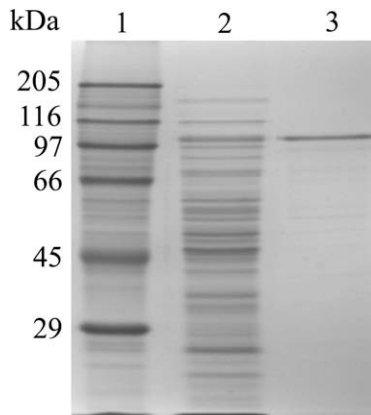
Thermostability studies (Fig. 3A) indicated that the  $\epsilon$ -fosEp was stable up to 46 °C for 10 min. At temperatures higher than this pro-

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MASATSASSTQISQNTTGSQPNNETTGETAQSSVNSTATA 40
SSSSVADLPSSSDSKSSIGSTISQPTVDKKEKTSKSDTADN 80
DLTKSVTTSDSDKALPTSKTTLPTSNEQVQSSVGGQSDTDQ 120
PASSATIATNAVTSQVSDVQNDQYNEPYRNQYHYSSSQNWIN 160
DPNGLFYDSKTLGLYNLYYQYQYNEPQVQWGNMSWGHAVSKDL 200
INWTQEDVAI PMLQNGQWEDFTYTNTTGSGLKDKGEVRYVG 240
VPTTNWGDADGKKAIFSGSIVVDTNNVSGLGKDAILAFYT 280
ADYQIATRKNDAEDGWGTWIGLTEIQEQLHAYSLDGGKT 320
FIQYSKDGNAANPQAI IPTSMNQGGAANFRDPSVYDAV 360
NKQYLLTVVSGQALIIYKSSNLLDWTYASKIERENDVNGG 400
VWECPSLVPK VAGTNETKWFVFCISVQQAHAHATGSGMQYY 440
VGNMTADGTWVPESSKTLQNPMTMSGDEFYAGI PFSNMP 480
DGRVMLAWQSNWSYVDEAKTSPWSGNMTLPREL S LK KNA 520
DTTDGYLLTNTVVKEIANNEEANVINKAESNFTVSRSDQ 560
VQYEGKQYKISATFSWDEADPKPSVGFKLRVSDDDQKYDMI 600
VGYDLTTGLLYVQRLNTGEPNMGAPRDKMKNATVNADGSIT 640
ITVYVDETSIEAFANDGEKSI TQNFMRPENIGDQATTGV 680
YVYSNDGTTKISDLTINPITSIWNSTGQLTEKHHHHHHH* 718

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**Fig. 1.** Amino acid sequence for the truncated *Lactobacillus paracasei* protein ( $\epsilon$ -fosEp). Peptide matches identified by nano-LC/MS/MS analysis of the purified  $\epsilon$ -fosEp are bolded; double underlining highlights poly-histidine tag of the recombinant  $\epsilon$ -fosEp.



**Fig. 2.** SDS polyacrylamide gel electrophoresis of the purified  $\alpha$ fosEp. Lane 1 = molecular weight markers; lane 2 = all cytosolic proteins expressed in *E. coli*; lane 3 = the Ni<sup>2+</sup>-NTA agarose purified  $\alpha$ fosEp.

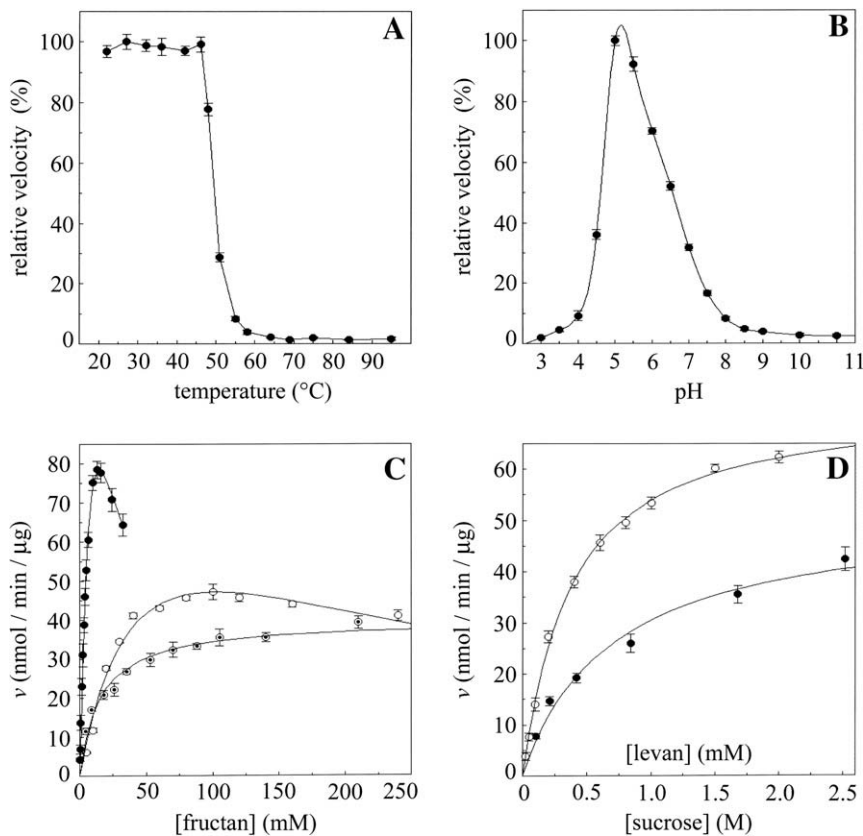
tein activity was lost, with complete denaturation occurring >55 °C. The  $T_{0.5}$  value for the  $\alpha$ fosEp was 49 °C under stated conditions. The pH profile of the  $\alpha$ fosEp (Fig. 3B) indicated an optimal pH of 5–5.5; protein activity declined sharply at pH values <5.0. The decrease in exo-inulinase activity at pH values >5.0 was more gradual; complete inactivation of the  $\alpha$ fosEp was not observed until pH 8 was exceeded.

Enzymatic hydrolysis of chicory inulin (glc:fru<sub>n</sub>,  $\beta$ [2-1] linked fructose), levan (glc:fru<sub>n</sub>,  $\beta$ [2-6] linkages), nystose (glc:fru<sub>3</sub>,  $\beta$ [2-1] linkages), 1-kestose (glc:fru<sub>2</sub>,  $\beta$ [2-1] linkages) and sucrose (glc:fru,  $\alpha$ - $\beta$ -1-2 bond) by the  $\alpha$ fosEp was observed (Table 1 and

Fig. 3). Conversely the  $\alpha$ fosEp displayed negligible activity on raffinose and did not cleave fructose monomers from stachyose or melizitose (Table 1). Truncated fosEp had the greatest affinity for bacterial levan with a  $K_m$  value 30-fold less than that for inulin or nystose, 100-fold less than the  $K_m$  for 1-kestose and 800-fold less than the  $K_m$  for sucrose. The nystose results indicate a preference for a fructan chain length of two or more fructose residues. Levan concentrations above 3 mM were not used because of the viscosity of the solutions produced. Substrate inhibition was observed with both 1-kestose and inulin at concentrations above 100 and 12 mM, respectively, with calculated inhibition constants ( $K_i$ ) of 210 and 13 mM for 1-kestose and inulin. In the case of inulin, part of the substrate inhibition observed may have been due to the increasing viscosity of the inulin solutions above 12 mM.  $V_{max}$  values obtained with inulin and 1-kestose were 3.45 and 1.55 nkat/ $\mu$ g  $\alpha$ fosEp whereas significantly lower  $V_{max}$  values of 0.66, 0.86 and 1.26 nkat/ $\mu$ g  $\alpha$ fosEp were obtained for nystose, levan and sucrose, respectively (Table 1). The low  $V_{max}$  value of just 0.07 nkat/ $\mu$ g  $\alpha$ fosEp obtained with raffinose indicated raffinose to be a particularly poor substrate. The maximum fructose turnover numbers observed using chicory inulin, nystose, levan, sucrose and 1-kestose were 106, 95, 89, 84 and 64 per second, respectively (Table 1). These results indicate that the  $\alpha$ fosEp has wide ranging substrate specificity and possesses exo-inulinase, exo-levanase and invertase activity.

### 3.3. Molecular modelling of $\alpha$ fosEp

Structural molecular modelling (Fig. 5) indicated that the  $\alpha$ fosEp is composed almost entirely of beta strands and turns, and is predicted to possess only four very short helical regions. The beta



**Fig. 3.** Biochemical characterisation of the  $\alpha$ fosEp. Chicory inulin (10% w/v) was used to determine thermostability (A) and pH profiles (B). Substrate saturation curves for inulin (filled circles), 1-kestose (hollow circles) and nystose (bullets) were determined (C) along with levan (filled circles) and sucrose (hollow circles) (D). A velocity of 60 nmol/min/ $\mu$ g protein is equivalent to 1 nkat/ $\mu$ g protein; derived kinetic parameters are listed in Table 1.

**Table 1**Substrate specificity of the  $\epsilon$ fosEp. Mean values from at least three separate determinations are shown with standard deviations in brackets.

Substrate	Monosaccharide (glc:fru:gal)	Linkage (fru:fru)	MW (Da)	$K_m$ (mM)	$V_{max}$ (nkat/ $\mu$ g $\epsilon$ fosEp)	Turnover (fru/s)
Inulin	glc:fru <sub>n</sub>	$\beta$ (2-1)	6200	15.6[ $\pm$ 3.1]	3.45[ $\pm$ 0.52]	106[ $\pm$ 15]
Levan	glc:fru <sub>n</sub>	$\beta$ (2-6)	12,000	0.5[ $\pm$ 0.1]	0.86[ $\pm$ 0.07]	89[ $\pm$ 8]
Sucrose	glc:fru	None	342	398[ $\pm$ 20]	1.26[ $\pm$ 0.02]	84[ $\pm$ 2]
1-Ketose	glc:fru <sub>2</sub>	$\beta$ (2-1)	504	49[ $\pm$ 9.7]	1.55[ $\pm$ 0.18]	64[ $\pm$ 11]
Raffinose	glc:fru:gal	None	504	392[ $\pm$ 130]	0.07[ $\pm$ 0.02]	16[ $\pm$ 2]
Nystose	glc:fru <sub>3</sub>	$\beta$ (2-1)	667	15[ $\pm$ 2.1]	0.66[ $\pm$ 0.02]	95[ $\pm$ 3]
Stachyose	glc:fru:gal <sub>2</sub>	None	667	–	0	0
Melezitose	glc <sub>2</sub> :fru	None	504	–	0	0

structure forms two distinct domains. The first domain, corresponding to residues 151–580, possesses a characteristic central cavity and is separated from the smaller domain (residues 581–700) by a notable cleft that appears to be a conserved feature of all currently characterised fructanase structures (Nagem et al., 2004). By analysis of conservation of residues in other inulinases, levanases and invertases, the cleft region and the central cavity of the major domain are clearly implicated in the catalytic activity of the enzyme. Comparison of the sequences of enzymes with only  $\beta$ (2-6) activity and those with combined  $\beta$ (2-1) and  $\beta$ (2-6) activity suggests that the cleft region is particularly important for  $\beta$ (2-6) degradative activity; the central cavity appears to be more involved with  $\beta$ (2-1) degradative activity. A number of residues associated with determining substrate specificity are located in a

region between the cavity and the cleft, in particular between residues 471–479.

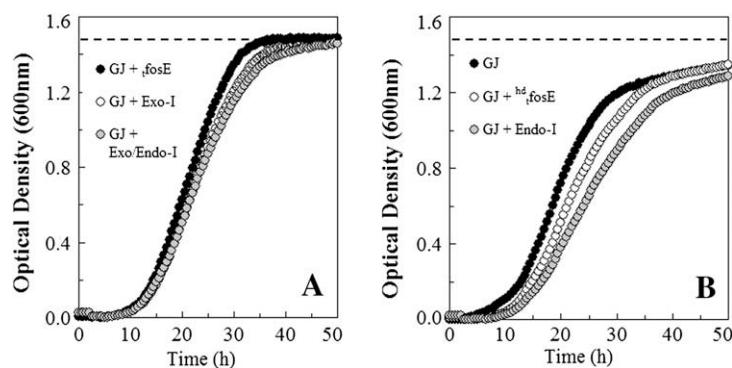
### 3.4. Enzymatic pre-treatment of grass juice feedstock

Enzymatic pre-treatment of GJ feedstock (media 1–6, Table 2) prior to fermentation experiments with Turbo yeast (Fig. 4) resulted in differences in  $t_{0h}$  concentrations of bioavailable glucose and fructose. The activity of the  $\epsilon$ fosEp on GJ (media 2) yielded the highest concentration of fructose (36.8[ $\pm$ 4.1] mg/ml); this equates to >15 mg/ml (72.2%) more fructose than was measured in untreated GJ. Conversely, the combined action of commercial exo- and endo-inulinases on GJ (media 6, GJ + Exo/Endo-1), resulted in the highest initial concentration of glucose (8.8[ $\pm$ 0.5] mg/ml);

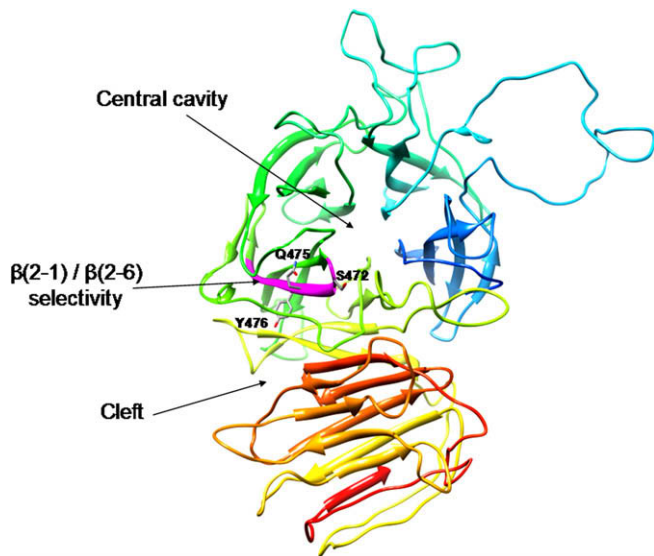
**Table 2**

Summary of automated growth and fermentation experiments: A = total glucose and total fructose concentrations in media at  $t_{0h}$ ; B = ethanol concentration,  $\Delta$ OD and population density measurements at  $t_{75h}$  (maximum values emboldened). All (mean %) increases were calculated relative to untreated GJ (media 1). No residual glucose or fructose was detectable in fermented media at  $t_{75h}$ .

		Media					
		1 GJ	2 GJ + $\epsilon$ fosEp	3 GJ + <sup>hd</sup> $\epsilon$ fosEp	4 GJ + Exo-I	5 GJ + Endo-I	6 GJ + Exo/Endo-I
A	Glucose (mg/ml)						
	Total[ $\pm$ SD]	7.9[0.4]	8.3[0.5]	8.0[0.4]	8.0[0.5]	8.5[0.5]	8.8[0.5]
	Increase (%)	–	(+5%)	(+1.3%)	(+1.3%)	(+7.6%)	(+11.4%)
	Fructose (mg/ml)						
Total[ $\pm$ SD]	21.5[2.7]	36.8[4.1]	20.6[1.6]	30.5[1.6]	21.5[2.7]	27.8[1.6]	
Increase (%)	–	(+72.2%)	–	(+41.9%)	–	(+29.3%)	
Total fructose:total glucose	2.7:1	4.4:1	2.6:1	3.8:1	2.5:1	3.2:1	
B	Total ethanol (mg/ml)	28.2[2.7]	36.5[4.3]	29.3[2.6]	32.1[3.5]	25.1[3.0]	31.6[4.0]
	Increase (%)	–	(+25.9%)	(+3.9%)	(+13.8%)	–	(+12.1%)
	$\Delta$ OD (600 nm)	1.43	1.5	1.44	1.52	1.39	1.52
	Density (cells/ml)	$1.76 \times 10^8$	$2.07 \times 10^8$	$1.66 \times 10^8$	$1.89 \times 10^8$	$1.64 \times 10^8$	$1.96 \times 10^8$



**Fig. 4.** Changes in optical density during automated growth and bioethanol fermentation experiments: A = growth of Turbo yeast on grass juice (GJ) pre-treated with the  $\epsilon$ fosEp, commercial exo-inulinase or a mixture of commercial exo- and endo-inulinases; B = growth of Turbo yeast on untreated GJ, GJ pre-treated with heat-denatured  $\epsilon$ fosEp or GJ treated with a commercial endo-inulinase. Broken line highlights maximum OD.



**Fig. 5.** Structural model of *Lactobacillus paracasei* (*fosE*)  $\beta$ -fructosidase showing the larger domain, (top, residues 150–580) with the characteristic central cavity and the smaller domain (bottom, residues 581–700), separated by the cleft that appears to be found in all fructanases (Nagem et al., 2004). The region implicated in substrate specificity (residues 471–479) is coloured in magenta with residues believed to be associated with breakage of  $\beta(2-6)$  linkages shown.

this corresponds to  $\approx 1$  mg/ml (11.4%) more glucose than was measured in untreated GJ. The highest ( $t_{0h}$ ) total fructose:total glucose ratio was found in media 2 (GJ +  $\iota$ -*fosEp*) followed by GJ + Exo-I, GJ + Exo/Endo-I, GJ, GJ +  $^{hd}$  $\iota$ -*fosEp* and finally GJ + Endo-I (ratios of 4.4, 3.8, 3.2, 2.7, 2.6 and 2.5:1, respectively). Bioavailable monosaccharides were utilised to completion for yeast growth and fermentation processes; no residual glucose or fructose were detectable in any of the GJ media at the end of fermentation studies ( $t_{75h}$ ).

### 3.5. Growth and ethanol production on pre-treated and non-hydrolysed grass juice

As anticipated, GJ supplemented with the active  $\iota$ -*fosEp* (GJ +  $\iota$ -*fosEp*), exo-inulinase (GJ + Exo-I) and the exo/endo-inulinase enzyme mixture (GJ + Exo/Endo-I) supported greater yeast growth than untreated GJ, GJ +  $^{hd}$  $\iota$ -*fosEp* and GJ + Endo-I (Fig. 4A and B). Addition of  $^{hd}$  $\iota$ -*fosEp* to the feedstock (Table 2, media 3) did not result in higher OD values than those recorded on unsupplemented GJ; this indicates that  $^{hd}$  $\iota$ -*fosEp* itself was not used as a growth substrate. Highest ethanol production was observed in growth experiments with GJ +  $\iota$ -*fosEp* followed by GJ + Exo-I, GJ + Exo/Endo-I, GJ +  $^{hd}$  $\iota$ -*fosEp*, untreated GJ and finally GJ + Endo-I (mean ethanol concentrations of 35.5, 32.1, 31.6, 29.3, 28.2 and 25.1 mg/ml, respectively). Growth parameters ( $\Delta$ OD values and cell counts) for Turbo populations grown on GJ +  $\iota$ -*fosEp*, GJ + Exo-I, and GJ + Exo/Endo-I were all significantly higher (Student's *t*-test,  $P < 0.05$ ,  $n = 3$ ) than those recorded on untreated GJ. However, only ethanol production on GJ +  $\iota$ -*fosEp* (not GJ + Exo-I or GJ + Exo/Endo-I) was found to be significantly higher than that seen on untreated GJ. A 25.9% increase in ethanol yield (relative to ethanol production on untreated GJ) was recorded with the GJ +  $\iota$ -*fosEp* feedstock; this equates to nearly double the next-highest increase (13.8%) seen in fermentation experiments with GJ + Exo-I (Table 2).

## 4. Discussion

Given the industrial applications and desirability of microbial inulinases (Chi et al., 2009), our results suggest that the  $\iota$ -*fosEp* is worthy of further investigation. Following successful expression

as a cytosolic protein in *E. coli*, the purified  $\iota$ -*fosEp* was observed to hydrolyse chicory inulin, nystose and 1-kestose; all of these fructans comprise (inulin-series) chains of  $\beta(2-1)$  linked fructose. Enzymatic cleavage of bacterial (*Zymomonas mobilis*) levan ( $\beta[2-6]$  fructose linkages) and the  $\alpha$ - $\beta$ -1-2 bond (linking glucose [glc] and fructose [fru]) in sucrose was also seen. A part of the catalytic region between the cavity and the cleft (Fig. 5, residues 471–479) appears to be of particular interest in light of these activities as it contains seven residues conserved in  $\beta(2-1)$  linkage cleaving enzymes. Three of these residues, corresponding to Ser 472, Gln 475 and Tyr 476, are conspicuously different in *Aspergillus fumigatus* inulinase that is believed to only cleave  $\beta(2-6)$  linkages. This region may play an important role in determining substrate specificity of the enzyme, and emphasises the structural disposition of the *L. paracasei* enzyme toward wider substrate specificity.

That sucrose but not melezitose was hydrolysed (Table 1) suggests that the fructose unit in melezitose (glu<sub>2</sub>:fru) might be shielded from  $\iota$ -*fosEp* activity by the presence of the second glucose unit linked (to fructose) at the C3 position. That hydrolysis of stachyose (a tetrasaccharide consisting of two  $\alpha$ -galactose units, one  $\alpha$ -glucose and one  $\beta$ -fructose) was not observed (Table 1) indicates that the  $\iota$ -*fosEp* possesses little or no  $\alpha$ -galactosidase activity. Alpha-galactosidases cleave terminal  $\alpha(1-6)$  linked galactose units from galacto-oligosaccharides of the raffinose family (Ulezlo and Zaprometova, 1982). Here, the minor hydrolytic activity observed on raffinose (a trisaccharide of glucose, fructose and galactose – formed by cleavage of one galactose from stachyose) suggests that the central fructose unit in raffinose might be accessible to the  $\iota$ -*fosEp* because it is not completely masked by the two terminal galactose moieties present in stachyose. Alternatively, it is possible that the  $\iota$ -*fosEp* acted upon sucrose impurities in the raffinose substrate.

Owing to its thermostability (10–50 °C) and pH optima (5.0–5.5), the  $\iota$ -*fosEp* displayed strong hydrolytic activity (at 37 °C for 18 h) on the fructan-rich grass juice feedstock (pH 5.5–5.7) used in growth and bioethanol fermentation experiments. Consideration of the ( $t_{0h}$ ) glucose and fructose content of feedstock (media 1–6, Table 2) provides further information about both the saccharide composition of grass juice and the hydrolytic activity of  $\iota$ -*fosEp*. That proportionally more fructose than glucose was detected in media 3 (GJ +  $\iota$ -*fosEp*) suggests that the  $\iota$ -*fosEp* acted on fructan polymers (glc:fru<sub>n</sub> and/or fru<sub>n</sub>) and not simply free sucrose (glc:fru) in grass juice (theoretically, the hydrolysis of just sucrose would result in 1:1 increases of fru and glc). Moreover, (when compared to the commercial *A. niger* exo-inulinase used in this study) pre-treatment of grass juice with the  $\iota$ -*fosEp* resulted in the highest increase (relative to untreated GJ) in bioavailable fructose (increases of 72.2% and 41.9% for GJ +  $\iota$ -*fosEp* and GJ + Exo-I, respectively). Because the  $\iota$ -*fosEp* hydrolyses inulin- and levan-series fructans ( $\beta[2-1]$  and  $\beta[2-6]$  bonds respectively), its action on grass biomass which contains a mixture of these (Bonnett et al., 1994, 1997) is superior to (and in an industrial setting, might be preferable over) more specific commercial exo- and endo-inulinases. The addition of a commercial *A. niger* endo-inulinase (Endo-I) to grass juice (media 5) failed to increase the amount of free fructose available for fermentation at  $t_{0h}$  (Table 2). Endo-inulinases cleave non-terminal fructose-fructose bonds (i.e. in the middle of inulin chains); the by-product/s of endo-inulinase activity are thus short chain fructans and/or fructose dimers (Vogel, 1993). Importantly, these are neither detectable using the colorimetric assay employed in this study nor readily bioavailable for yeast growth and bioethanol production. This result indicates that the increased fructose content (at  $t_{0h}$ ) in media 2, 4 and 6 owed primarily to exo-inulinase and (in the case of  $\iota$ -*fosEp*) invertase enzyme activity.

The experimental results from growth and fermentation studies reported here support our original hypothesis: that the addition of

the  $\epsilon$ fosEp to GJ should result in (i) hydrolysis of polyfructose moieties (increasing fructose bioavailability), (ii) elevated levels of yeast population growth and (iii) an increased yield of bioethanol. The ethanol yield (at  $t_{75h}$ ) from fermentation of GJ +  $\epsilon$ fosEp was significantly higher (Student's *t*-test,  $P < 0.05$ ,  $n = 3$ ) than that from untreated GJ (35.5 and 28.2 mg ethanol/ml respectively, Table 2). That ethanol production in control experiments (with GJ +  $\epsilon$ hd $\epsilon$ fosEp) was no higher than production seen on untreated GJ indicates that the  $\epsilon$ fosEp itself was not utilised as a growth and fermentation substrate. It is noteworthy that (like GJ +  $\epsilon$ fosEp) media 4 and 6 (GJ + Exo-I and GJ + Exo/Endo-I) supported significantly higher yeast growth (cell counts and  $\Delta$ OD readings) but not ethanol production. This implies that the extra glucose and fructose made bioavailable by enzymatic hydrolysis of fructans in media 4 and 6 was sufficient to support yeast growth to stationary phase ( $\approx 2.0 \times 10^8$  cells/ml), but not ethanol production during this phase. Conversely, the additional fructose released by the  $\epsilon$ fosEp (>6.0 mg and 10 mg/ml more fructose than released by Exo-I and Exo/Endo-I) was adequate to support population growth to stationary phase and ethanol production thereafter.

The enzyme kinetics data and results from growth and fermentation experiments reported here, demonstrate the commercial potential of the  $\epsilon$ fosEp as an enzyme capable of enhancing bioethanol yield from grass fructans. Given its broad substrate spectrum, pH optimum, thermostability and high fructose turnover rates the  $\epsilon$ fosEp could also find application in alternative (e.g. food or pharmaceutical) industries (Chi et al., 2009). Obviously, the extent to which  $\epsilon$ fosEp might increase bioethanol yield from grass juice is ultimately dependent on the composition of initial feedstock. Because the fructan content of ryegrass is under metabolic control, varying seasonally and with anthropogenic environmental stress (Cairns et al., 2008; Udén, 2006), experiments addressing the pre-treatment requirement/s of a variety of grass feedstocks are now needed. Work is also required to optimise fermentation conditions (e.g. the potential need for nutrient supplements) and to explore fermentation technologies (immobilised yeast strains, large-scale high gravity systems, etc.) that could enhance bioethanol yields from grass juice. Although this study focuses specifically on harnessing energy from the polyfructose component of ryegrass biomass, the emphasis of longer-term research is the utilisation of all (including fibrous) fractions of the grass crop for optimal bioethanol production. Attempts to achieve simultaneous saccharification and fermentation of grass juice using recombinant yeast that express microbial fructanases are currently underway.

## Acknowledgements

Funding for this study was provided by the Welsh Energy Research Centre (WERC, UK) and the European Regional Development Fund of the European Union. Technical assistance was provided by Nicola Rolley (Swansea University, UK).

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