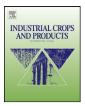
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New metal catalysts active for thermal polymerization of vegetable oils

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ABSTRACT

The catalytic activity of several low-toxic metal compounds was tested in the polymerization of soybean oil to produce biobased resins suitable to be used as binder in printing inks (offset). Soybean was polymerized in the absence and presence of different complexes of the type $M(Carboxylate)_2$ (M = Ni, Fe, Co, Cu and Sn) and all compounds showed activity. The best result was obtained using Ni(II), when was observed an apparent kinematic constant up to 2.4 times higher than when in the absence of any metal compound. It was also observed that the catalytic activity of the Ni(II) strongly depends upon the metal content and the reaction temperature. Testing different vegetable oils was observed that the catalytic activity was dependent on the number of double-bonds of the oil.

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1. Introduction

In the formulation of inks, paints and coatings there are different components, such as binders, pigments, solvents and additives. The binder forms a recovering thin film in the surface where the ink, paint or coating is applied and its first role is to keep the pigments agglutinated and glued to the surface. However, depending on the coating or paint, the film may also protect the surface from corrosion, temperature or moisture, as well as any other specific desired properties (Mello and Suarez, 2012). Along the history different materials have been used as binder, being the most important natural polymers such as proteins and polymerized lipids. Nevertheless. in the last century different petrochemical based resins with tuned physical-chemical properties have dominated the binder market in all fields of coatings, paints and inks. Recently, as in many other fields (Doll and Erhan, 2006; Sharma and Kundu, 2006; Suarez et al., 2007; Sharma et al., 2007), environmental concerns and increasing demand for petroleum had leaded researchers to develop new technologies to produce binders using renewable raw materials (Erhan and Bagby, 1991).

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One example is the use vegetable oils and their polymers as binder for printing inks (offset), especially to print newspapers and magazines. The former works published in the literature appeared in the 1970s and 1980s and were related to the use of gilsonite oil and tall oil blends (Kobayashi and Nozaki, 1978; Koritala et al., 1987; Kuzuwata, 1988; Moynihan, 1985). Unfortunately, these works resulted in unsuitable binders from both technical and economical points of view. Indeed, the limitations of this approach were associated to its high cost and also to availability of the raw materials, as well as printing equipment clean-up difficulties because of the use of gilsonite.

In sequence, by using soybean oil blended with thermally polymerized soybean oil was possible to produce black and colored printing inks with equal or better physical-chemical properties than when using petrochemical resins as vehicle. Indeed, when compared with petrochemical based ones, the biobased printing inks showed better friction resistance coefficient, improved degradability, higher compatibility with carbon Black pigment and light vehicle color that allowed the use of less pigment amount (Erhan and Bagby, 1993, 1994, 1995). The high performance of the soybean based ink, called Soyink[®], became competitive from an economical point of view in the last decade and several important newspaper and magazines in US are currently printed using this technology. However, its price is still high and the improving the process in order to reduce costs is still a great challenge to researchers.

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In this sense, it is well known that the main cost of vegetable oil based inks is associated with the thermal polymerization. Indeed, the thermal processing of the oils occurs in temperatures above 280 °C and takes long reaction times. The only approach published in the literature to reduce the reaction time during thermal polymerization of vegetable oils was the use of organic catalysts, such as quinones (Archer, 1938). However, Erhan and co-worker have published an elegant paper showing these catalysts have low activity, being necessary to use high amount of quinones. For instance, the use of 5 mass% of antraquinone could reduce only from 10 to 20% of the reaction time (Erhan and Bagby, 1991). Besides, a further step to take out this catalyst from the polymer was needed because of its low solubility in the ink leaded to undesired properties, which would obviously increase production costs (Erhan and Bagby, 1992, 1994).

As far as our knowledge, there are no processes in the literature describing efficient catalysts that could diminish the reaction time when used in low catalytic amounts. Thus, the aim of this work was to study the catalytic activity of different low-toxic metal compounds in the thermal polymerization of vegetable oils and the main goal was to found a catalyst able to significantly reduce the reaction time even when used in small amounts.

2. Materials and methods

2.1. Materials

Reagents FeCl₂·4H₂O, CoCl₂·6H₂O, SnCl₂·6H₂O, NiCl₂·6H₂O, CuCl₂·2H₂O, HCl, NaOH, Na₂SO₄ and hexane were purchased from Vetec Química Fina Ltda. Alkali-refined soybean, canola, corn and sunflower oils were obtained from Bunge Alimentos. Palm oil was purchased from Master Food Ltda. All materials were used as received without any further purification.

2.2. Instrumental

The DRIFT FT-IR spectra (diffuse reflectance infrared Fourier transform) were obtained from powder samples on a Bruker Equinox 55 interferometer (Ettlingen, Germany). The FT–IR spectra were stored in the Kubelka–Munk mode and are the average of 32 scans at a nominal spectral resolution of $4 \, \mathrm{cm^{-1}}$. The thermal analysis (TGA and DTA) was performed on a DTG-60 Shimadzu instrument under N₂ flow (50 mL min⁻¹). The samples were analyzed in a platinum pan from 25 to 800 °C with 10 °C/min heating rate.

2.3. Preparation of metal complexes

Fe(II), Ni(II), Co(II), Cu(II) and Sn(II) were complexed with Carboxylate ligants derived from palm oil fatty acids. In a Becker flask were added palm oil fatty acids (0.02 mol) and NaOH (0.025 mol) and the mixture was kept under stirring for 3 h. Then, one of the metal chlorides (0.01 mol) was added and left under stirring for 4 h, maintaining pH in 8. The obtained precipitated was dissolved in hexane and the solution was washed three times with distilled water. The solvent was then removed under reduced pressure in a rotaevaporator and the obtained metallic complex characterized using FT-IR, TGA. The metal content was gravimetrically determined by calcinating the complexes at 800 °C for 24 h.

2.4. Vegetable oil thermal polymerization

Alkali-refined vegetable oil (500 g) was polymerized in a 1.0L five necked reaction flask equipped with a mechanic stirrer, reflux condenser, nitrogen atmosphere and heater, as shown in Fig. 1.

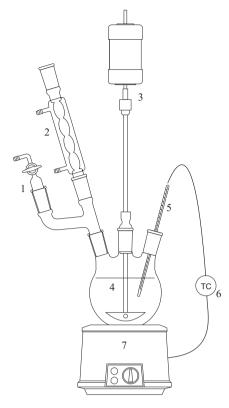


Fig. 1. Thermal polymerization system: (1) nitrogen flow; (2) reflux condenser; (3) mechanical stirrer; (4) reactor; (5) thermopar; (6) temperature control; and (7) heater.

Samples were taken in 0.0, 1.0, 1.5, 2.0, 2.5 and 3.0 h and their kinematic viscosities were estimated using an ubbelohde viscosimeter according to ASTM D445. For each reaction, the apparent kinematic viscosity constants (*k*) were determined plotting Ln (kinematic viscosity) *versus* time, according to the linear function $\ln \eta = k.t.$

3. Results and discussion

3.1. Complexes synthesis and characterization

Divalent metal ions complexes with the general formula $M(Carboxylate)_2$ were synthesized according to Fig. 2. The molecular formula was confirmed by gravimetric analysis after calcinating the complexes at 800 °C for 24 h under oxygen atmosphere. Indeed, it was obtained 7, 8, 9, 12 and 19 mass%, respectively, for the Ni, Fe, Co, Cu and Sn complexes.

The complexes were analyzed by FT-IR and in Fig. 3 is shown their spectra. As can be depicted from Fig. 3, the main important change in the spectra after the complexation is the absorption at 1708 cm^{-1} due to fatty acid carboxylic group, which diminished its intensity, and a new absorption at 1600 cm^{-1} that may be attributed to the complexed carboxylic group.

The TGA thermal analyses of the complexes are shown in Fig. 4. As can be depicted from this figure, the decomposition of all complexes start at 250 °C and, different from the starting fatty acids

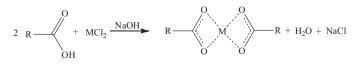


Fig. 2. Preparation of metal complexes of the type $M(Carboxylate)_2$ (M = Ni, Fe, Co, Cu and Sn; Carboxylate = palm-tree oil fatty acids carboxylates).

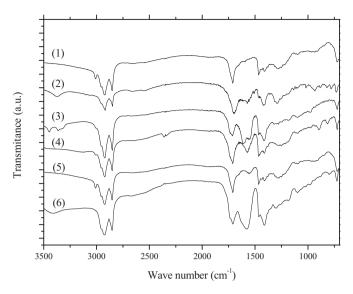


Fig. 3. FT-IR spectra of palm-tree oil fatty acids (1) and its complexes of the type M^{+2} (palm-tree oil carboxylates)₂, where M = Co (2), Cu (3), Fe (4), Sn (5) and Ni (6).

mixture, behaves a complicated mechanism with different steps. These different steps are probably related to the decomposition of the alkyd chains of the carboxylate ligands. This result strongly indicates that the catalysts are partially decomposed in the reaction conditions. However, the main importance of using these complexes instead of the stable starting divalent ion salts is their high solubility in the vegetable oil, homogenizing the reaction media.

3.2. Catalytic studies in polymerization

There are some mechanistic studies published in the literature about thermal polymerization of vegetable oils (Archer, 1938; Sims, 1957). These studies suggest the thermal polymerization may have different step-reactions. One possible path is the isomerization of double bonds into *trans* conjugated systems, followed by cyclization *via* Diels–Alder reaction of the formed conjugated dienes with double bonds from other chains acting as dienenophile. This reaction leads to the formation of tetrasubstituted cyclohexenes which links different alkyl chains. Another possible pathway is the radicals

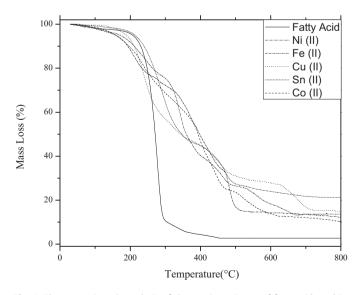


Fig. 4. Thermogravimetric analysis of the starting mixture of fatty acids and its complexes with Ni (II), Fe (II), Co (II), Cu (II) e Sn (II).

Table 1

Apparent kinematic viscosity constant and viscosity after 3 h of thermal polymerization of soybean oil at 300 °C.

Entry	Catalysts	$k \cdot 10 \mathrm{h}^{-1a}$	$k_{(\text{Cat.})}/k_{(\text{No Cat.})}^{\text{b}}$	Viscosity after 3 h (cSt)
01	No catalyst	3.86	1.00	113
02	Ni (II)	9.20	2.39	455
03	Fe (II)	8.83	2.29	446
04	Cu (II)	8.70	2.25	445
05	Sn (II)	6.95	1.80	286
06	Co (II)	6.35	1.65	234

^a k is the apparent kinematic viscosity constant.

^b $k_{(Cat.)}/k_{(No Cat.)}$ corresponds to the relationship between the constant obtained with $(k_{(Cat.)})$ and without $(k_{(No Cat.)})$ catalyst.

polymerization process. It is worth mentioning that these reactions may occur simultaneously and that it is rough to determine the importance of each one in the polymer formation. Thus, our first approach was study complexes of metal know in the literature as active for regular Diels–Alder reactions, such as Ni⁺², Fe⁺², Cu⁺², Sn⁺² and Co⁺²(Wender and Smith, 1998; Ruff et al., 1995; Liu et al., 2011.). Note that cobalt and cupper complexes are also known in the literature as promoters of redox processes and radical polymerization (Mallegol et al., 2000; Kickelbick et al., 1999).

In sequence, soybean oil was thermally polymerized in the absence and presence of all prepared $M(Carboxylate)_2$ (M = Ni, Fe, Co, Cu and Sn) and in Fig. 5a are presented the viscosity of the reaction bulk during these polymerizations. Note that the viscosity is proportional to the polymerization degree. It means, as the oil chains are linked, either by radicals polymerization or Diels-Alder cyclization, and, thus, the molecular weight increases, the viscosity of the media gets higher. Plotting the natural logarithm of the kinematic viscosity versus time leaded to a linear plot and the apparent kinematic constant was obtained (Fig. 5b and values are listed in Table 1). As become clear from the results presented in Fig. 5 and Table 1, all tested complexes showed activity for the polymerization as far as the kinematic viscosity in similar times and temperature are always higher than when the reaction was carried out in the absence of metal ions (no catalyst added). Comparing the different catalysts we found out that Ni(II) presented the highest activity. Indeed, when comparing with the reaction carried out in the absence of catalyst, the polymerization assisted by Ni(II) showed after 3 h an apparent kinematic constant up to 2.4 times higher and the viscosity increased up to 4 times. Note that Cu(II) and Fe(II) exhibit comparable activity than Ni(II).

Because of its higher activity when compared with the other complexes Ni(II) was chosen for further studies. At first the metal amount was varied from zero to 0.2 mass% and the kinematic viscosity apparent constant (k) was determined (see results in Table 2). It becomes clear from Table 2 that k increases with the metal complex concentration, strongly indicating a catalytic activity of the metal compound. It is important to highlight that even when using tinny amounts of the catalyst 0.0002 mass% a high activity was observed, doubling k when compared with the non-catalyzed reaction.

Table 2

Apparent kinematic viscosity constant (k) of soybean oil polymerization at 300 °C varying the amount of Ni (II) carboxylate complex from zero to 0.2 mass%.

Entry	Ni(II) variation (w/w)	$k \cdot 10 \mathrm{h}^{-1}$	Viscosity after 3 h
01	0	3.86	113
07	0.0002	6.80	257
08	0.001	7.32	312
09	0.04	8.56	429
02	0.1	9.20	455
10	0.2	9.32	468

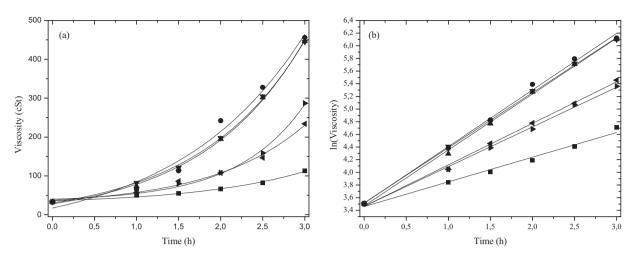


Fig. 5. Soybean oil thermal polymerization in the absence of catalyst (■) and in the presence of M⁺²(Carboxylate)₂ [M = Ni (●), Fe(▲), Cu(♥), Sn(◀), Co(►)]: (A) viscosity versus time and (B) Ln (viscosity) versus time.

Table 3

Apparent kinematic viscosity constant (k) of soybean oil polymerization at 280, 300 and 310 °C in the presence of 0.1 mass% of Ni(II) carboxylate complex.

Entry	Temperature (C°)	Catalyst	$k \cdot 10 \mathrm{h}^{-1}$	Viscosity after 3 h
11	280	-	1.97	63
01	300	-	3.86	113
12	310	-	8.55	560
13	280	Ni (II)	3.58	98
02	300	Ni (II)	9.20	455
14	310	Ni (II)	13.8	2100

In sequence, the Ni(II) amount was fixed in 0 and 0.1 mass% and the temperature was varied from 280 to 310 °C and the k for the different reactions are listed in Table 3. It was observed that the k strongly increases in this temperature range, either for the noncatalyzed or the catalyzed reactions. It was also observed that for the same temperature k is always higher when Ni(II) is used.

Finally, the Ni(II) complex catalytic activity was evaluated for other vegetable oils containing different unsaturation degrees (double-bonds content). Indeed, the unsaturation degree of the oils increases from canola < corn < sunflower < soybean. It was tested the polymerization of the oils at 300 °C in the presence of Ni(II) (0.1 mass%) and the calculated k for the reactions are listed in Table 4. It becomes clear from the results presented in Table 4 that as expected there is a direct relation between the unsaturation degree and k.

Table 4

Apparent kinematic viscosity constant (k) of different oils polymerization at 300 $^\circ C$ in the presence of 0.1 mass% of Ni(II) carboxylate complex.

Entry	Vegetable oil	Catalyst	$k \cdot 10 \mathrm{h}^{-1}$	Viscosity after 3 h
01	Soybean	-	3.86	113
15	Sunflower	-	3.71	106
16	Corn	-	3.43	100
17	Canola	-	2.23	80
02	Soybean	Ni (II)	9.20	455
18	Sunflower	Ni (II)	9.01	434
19	Corn	Ni (II)	8.60	381
20	Canola	Ni (II)	5.96	239

4. Conclusions

In summary, we found out that different metal complexes of the type $M(Carboxylate)_2$ are active for vegetable oils polymerization. The Ni(II) complex showed a high catalytic activity even when a tiny amount of the catalyst was added. Indeed, we could polymerize oils with a high energy saving, since the reaction occurs in high temperature (300 °C) and the presence of only 0.1 mass% of Ni(II) reduced 60% of the time needed to achieve a kinematic viscosity of the resin of 113 cSt. This is an important result because it can improve the economical viability of producing printing inks using vegetable oils.

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