



# Selective electrochemical CO<sub>2</sub> reduction to formate at industrial current densities using 2D Bi<sub>2</sub>O<sub>2</sub>CO<sub>3</sub> nanosheets

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## ABSTRACT

Electrochemical CO<sub>2</sub> reduction to formate (HCOO<sup>-</sup>) represents an efficient strategy to mitigate CO<sub>2</sub> emissions while producing value-added chemicals. However, the reaction typically requires high overpotential and suffers from low selectivity and current density. This work reports the development of Bi<sub>2</sub>O<sub>2</sub>CO<sub>3</sub> (BOC) nanosheets synthesized hydrothermally with urea at 90 °C (BOC-90) and 150 °C (BOC-150), evaluated in a flow-cell configuration with gas diffusion electrodes. A Bi<sub>2</sub>O<sub>2</sub>CO<sub>3</sub> sample calcined at 400 °C (Bi<sub>2</sub>O<sub>3</sub>-400) was also investigated for comparison. Both BOC-90 and BOC-150 outperformed Bi<sub>2</sub>O<sub>3</sub>-400 and a commercial BOC sample in HCOO<sup>-</sup> production. Notably, BOC-150 achieved a current density of -140 mA cm<sup>-2</sup> and a Faradaic efficiency (FE) of 95% for HCOO<sup>-</sup> at -1.2 V vs. RHE in 0.5 M KOH. Optimizing the electrolyte concentration (1.0 M KOH) and electrode composition (75% BOC-150, 25% carbon black) further enhanced performance, yielding -250 mA cm<sup>-2</sup> with FE for HCOO<sup>-</sup> (FE<sub>HCOO-</sub>) above 90%. EIS showed that BOC-150 has the lowest charge-transfer resistance, while ECSA measurements confirmed its highest active surface area, jointly explaining its enhanced ECR performance. NIR and XPS analyses revealed that strongly adsorbed water and Bi dissolution reduced BOC-90 stability, while BOC-150 maintained structural integrity and favorable surface composition. The electrode exhibited stable operation for 6 h, maintaining a Faradaic efficiency above 80% throughout the electrolysis. These findings demonstrate that BOC nanosheets, particularly those obtained under optimized hydrothermal conditions, are highly efficient and durable electrocatalysts for CO<sub>2</sub> reduction to HCOO<sup>-</sup> under industrially relevant conditions.

## 1. Introduction

The intensification of global energy consumption, historically sustained by the burning of fossil fuels, has caused a concerning increase in the atmospheric concentration of carbon dioxide (CO<sub>2</sub>), the main greenhouse gas responsible for global warming [1–10]. Faced with this environmental challenge, the electrochemical CO<sub>2</sub> reduction (ECR) emerges as a promising route, allowing the conversion of CO<sub>2</sub> into value-added chemical compounds such as HCOOH/HCOO<sup>-</sup>, carbon monoxide (CO), methane (CH<sub>4</sub>), methanol (CH<sub>3</sub>OH), and ethylene (C<sub>2</sub>H<sub>4</sub>) using electricity, preferably from renewable sources, as an

energy input [10–17]. Among these products, HCOO<sup>-</sup> stands out for its industrial value, versatility as a chemical feedstock, and potential as an energy carrier in fuel cells [18].

However, the high thermodynamic stability of the CO<sub>2</sub> molecule poses significant challenges to its electrochemical conversion. The ECR process requires the formation of the radical anion CO<sub>2</sub><sup>-</sup>, a highly unstable intermediate, which demands considerable overpotentials, significantly more negative than the theoretical potentials and favors parasitic reactions, especially hydrogen evolution reaction (HER) [2,10,19–26].

Various materials have been explored as catalysts for ECR, including

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metals, metal oxides and molecular complexes. Among them, p-block metals-based electrocatalysts, such as bismuth (Bi), tin (Sn), lead (Pb), and indium (In), stand out for their high selectivity towards  $\text{HCOO}^-$  formation [17,25–27]. However, the practical use of Pb and In based catalysts is hindered by significant drawbacks: Pb presents high toxicity and environmental hazards, while, In suffers from scarcity and high cost, which limit large-scale applications. Sn based electrocatalysts exhibit remarkable activity and selectivity for  $\text{HCOO}^-$  production, but their stability under prolonged operation remains a critical challenge due to surface restructuring and dissolution phenomena [6,7,28]. Among these metals, Bi has emerged as a particularly attractive candidate owing to its low toxicity, environmental benignity, and high selectivity towards  $\text{HCOO}^-$ . Nevertheless, conventional Bi based catalysts still face important limitations, including low electrical conductivity, restricted surface area, and intrinsically low exposure of active sites, which result in modest catalytic activity, especially under severe operating conditions [22,29].

The challenges described above highlight the critical need to advance catalytic systems for the ECR. To address several limitations described, a promising approach involves the use of two-dimensional (2D) nanostructures, such as bismuth oxycarbonate (BOC) nanosheets. These materials offer a significantly higher surface to volume ratio, thereby increasing the density of catalytically active sites. Furthermore, their integration into gas diffusion electrodes (GDEs) within flow cell reactors is crucial, as this configuration overcomes mass transport limitations and allows for operation at industrially relevant current densities, while also facilitating the suppression of the competing HER ( $>200 \text{ mA cm}^{-2}$ ) [22,30–34].

Therefore, in this work, we aim to develop and evaluate 2D bismuth oxycarbonate ( $\text{Bi}_2\text{O}_2\text{CO}_3$ , BOC) nanostructures synthesized under controlled hydrothermal conditions as efficient electrocatalysts for the  $\text{CO}_2$  reduction reaction to  $\text{HCOO}^-$ . The synthesized materials will be characterized and applied in an electrochemical flow cell equipped with gas diffusion electrodes to assess their catalytic activity, selectivity, and stability under conditions relevant to industrial applications. Additionally, the influence of synthesis temperature and structural transformation to  $\text{Bi}_2\text{O}_3$  on the electrochemical performance will be systematically investigated. Through this approach, we seek to establish structure activity relationships and elucidate the factors governing the superior performance of BOC nanosheets, contributing to the rational design of next generation bismuth based catalysts for efficient and selective  $\text{CO}_2$  electroreduction to  $\text{HCOO}^-$ .

## 2. Materials and methods

### 2.1. Synthesis of $\text{Bi}_2\text{O}_2\text{CO}_3$ and $\text{Bi}_2\text{O}_3$ samples

$\text{Bi}_2\text{O}_2\text{CO}_3$  was synthesized via a hydrothermal method [35]. 6.066 g of urea ( $\text{NH}_2)_2\text{CO}$ ) was dissolved in 40 ml of methanol ( $\text{CH}_3\text{OH}$ ), while 0.97014 g of  $\text{Bi}(\text{NO}_3)_3 \cdot 5\text{H}_2\text{O}$  was dissolved in 40 mL of deionized water. Then, both solutions were mixed and stirred at room temperature for 30 min, then transferred to a Teflon-lined autoclave and treated hydrothermally at 90, 150 °C for 240 min with a heating rate of 5 °C/min. After hydrothermal treatment, the products were washed three times (10 min each) and dried at 70 °C for 12 h. The sample treated at 90 and 150 °C were denoted as BOC-90 and BOC-150, respectively. For comparison, BOC-90 was annealed at 400 °C to obtain  $\text{Bi}_2\text{O}_3$ , denoted as  $\text{Bi}_2\text{O}_3$ -400. Commercial  $\text{Bi}_2\text{O}_2\text{CO}_3$  powder (Sigma-Aldrich) (denoted as BOCCOM) was used as a reference material in all structural, physicochemical, and electrochemical analyses.

### 2.2. Preparation of gas diffusion electrodes

Gas diffusion electrodes were prepared by spray coating onto a carbon paper substrate (GDL-Sigracet, 39B) using an airbrush (Vonder). The ink was composed of 7.5 mg of catalyst (BOC or  $\text{Bi}_2\text{O}_3$ ), 7.5 mg of

carbon black (amorphous carbon, CAS #1333–86–4), 17  $\mu\text{L}$  of an ionomer (Sustainion XA-95% in Ethanol, Dioxide Materials Inc.), 1 mL of deionized water, and 1 mL of isopropanol (Vetec 99.5%). Different weight ratios of the electrocatalyst and carbon black were evaluated: 25, 50 and 75%. The mixture was placed in a 10 mL beaker within a cold water bath and then subjected to 30 min of sonication using an ultrasonic tip sonicator (Sonics & Materials INC, VCX130) with a power of 130 W. Subsequently, the homogenized solution was uniformly deposited onto a 16  $\text{cm}^2$  area of carbon paper using an airbrush and then dried in an oven at 80 °C for 24 h. The prepared electrodes exhibited a loading of 0.19  $\text{mg cm}^{-2}$ . Finally, a 1  $\text{cm}^2$  piece of the electrode was cut and applied as the working electrode for the ECR.

### 2.3. Materials characterization

The crystalline structure of the synthesized materials was investigated using X-ray diffraction (XRD) with a Shimadzu XRD600 powder diffractometer operating at 40 kV and 30 mA, employing  $\text{Cu K}\alpha$  radiation. Data were collected over a  $2\theta$  range of 10° to 70° with a scan rate of 0.02°  $\text{min}^{-1}$ . Crystallite size information was extracted from the XRD patterns and calculated using the Scherrer equation (Eq S1). The short range structure of the BOC samples was characterized by Raman spectroscopy using a HORIBA LabRAM HR Evolution confocal spectrometer equipped with a customized CCD detector (OSD Sincerity) and four laser lines, operated with HORIBA Scientific's LabSpec software. A 532 nm excitation laser was employed, delivering 50 mW at the sample (corresponding to 78 mW before the objective), as measured with a power meter. Attenuated total reflectance Fourier-transform infrared (ATR FTIR) spectra were recorded using a PerkinElmer Frontier spectrometer with a diamond crystal, to identify the functional groups present in the samples. Measurements were performed with 128 scans and a resolution of 4  $\text{cm}^{-1}$  over the range of 200 to 2400  $\text{cm}^{-1}$ .

The surface morphology of the materials was characterized by field emission scanning electron microscopy (FESEM) using a JEOL 6701F instrument. For sample preparation, small amounts of the powders were individually suspended in isopropanol, drop-cast onto Si substrates, and subsequently mounted on stubs with carbon tape for imaging of BOC and  $\text{Bi}_2\text{O}_3$ .

Thermogravimetric analysis (TGA) was performed using a Shimadzu DTG-60H instrument to evaluate the thermal stability and compositional changes of both the synthesized and commercial samples as a function of temperature. The analysis was conducted on a sample weight of 10 mg under a synthetic air flow of 50  $\text{mL min}^{-1}$ , with a heating rate of 10 °C  $\text{min}^{-1}$  over a temperature range of 30 to 600 °C. The specific surface area of the samples was determined by nitrogen ( $\text{N}_2$ ) physisorption at 77 K using a Micromeritics ASAP 2000 instrument (Norcross, Georgia, USA). The Brunauer-Emmett-Teller (BET) model was applied to estimate the surface area. Prior to the measurements, the samples were degassed at 80 °C under vacuum until a pressure below 10  $\mu\text{mHg}$  was achieved. Near-infrared spectroscopy (NIR) was employed to assess the surface coverage of  $\text{OH}^-$  groups on the samples by qualitatively determining the adsorption of water molecules, using a PerkinElmer Spectrum 100 spectrometer. X-ray photoelectron spectroscopy (XPS) was employed to determine the chemical states of the synthesized BOC samples. The measurements were carried out on a Scienta Omicron ESCA+ spectrometer equipped with a high-performance EA 125 hemispherical analyzer, using monochromatic  $\text{Al K}\alpha$  radiation ( $h\nu = 1486.6 \text{ eV}$ ) as the excitation source. During data acquisition, the ultra-high vacuum chamber was maintained at a base pressure of  $2 \times 10^{-9}$  mbar. Survey spectra and high-resolution spectra were collected with energy steps of 0.50 eV and 0.05 eV, respectively. Quantitative analysis was performed using the O 1 s, C 1 s, F 1 s, and Bi 4f core levels. The binding energy scale was calibrated by setting the C–C component of the adventitious carbon C 1 s peak to 284.8 eV. Spectral deconvolution was performed in CasaXPS software using Shirley and Tougaard background subtraction, with peak fitting based on mixed Gaussian-Lorentzian

functions.

#### 2.4. ECR performance evaluation

All electrochemical measurements were performed on a potentiostat/galvanostat (*Autolab PGSTAT204, Metrohm*). The ECR experiments were carried out in a commercial flow cell (Micro Flow Cell, Electrocell) with three compartments. BOC and Bi<sub>2</sub>O<sub>3</sub>-based electrodes with 1 cm<sup>2</sup> were used as working electrodes, nickel foam as the counter electrode, a leak-free Ag/AgCl (3 M) as the reference electrode, and an anion exchange membrane (FAB-PK-130, Fumasep) to separate the cathode and anode. KOH solutions at different concentrations (0.5 to 2.0 mol L<sup>-1</sup>) were used as the electrolyte and circulated through the cell using a peristaltic pump at a flow rate of 6 mL min<sup>-1</sup>. CO<sub>2</sub> (99.99%) was purged through the back and across the GDE at a flow rate of 30 mL min<sup>-1</sup>, controlled by a rotameter (Aalborg, Orangeburg). The electrochemical performance was evaluated from the material linear sweep voltammetry (LSV) in the potential window of -0.4 to -1.2 V vs RHE. Potentials were converted to the RHE scale using the following equation:

$$E \text{ (V vs RHE)} = E \text{ (V vs Ag/AgCl)} + 0.197 \text{ V} + 0.0592 \times \text{pH}$$

Electrolysis was performed at different applied potentials (-0.8, -1.0, and -1.2 V vs. RHE), with the gaseous and liquid products of the reaction being analyzed every 30 min. To investigate the electrode stability, chronopotentiometry experiment was performed at a constant current of -40 mA for 6 h. The potential and FE was monitored throughout the experiment to evaluate operational stability under steady-state conditions. For the stability experiment the catalyst was deposited onto a PTFE-based gas diffusion electrode (GDE), which was used as the cathode, to overcome the flooding problem.

The gaseous products exiting the cell were transported by the continuous CO<sub>2</sub> flow to a gas collection bag, where aliquots were collected with a syringe and injected into a gas chromatograph equipped with a thermal conductivity detector (GC-TCD, PerkinElmer Clarus 580) for quantification of CO and H<sub>2</sub> concentrations.

HCOO<sup>-</sup> quantification was performed by high-performance liquid chromatography (HPLC) using a Shimadzu system, operated with Lab-Solutions software. Samples were prepared from 5 mL aliquots of electrolyte, adjusted to pH 2.0, filtered through a 0.22 μm syringe filter, and transferred into vials. Separation was carried out on an Aminex HPX-87H column (Bio-Rad), maintained at 60 °C, using 2.5 mmol L<sup>-1</sup> H<sub>2</sub>SO<sub>4</sub> as the mobile phase under isocratic mode and pumped at a flow rate of 0.7 mL min<sup>-1</sup>. Detection was performed at 210 nm, with HCOO<sup>-</sup> identification confirmed by comparing retention times with authentic standards. Quantification was achieved by integrating the peak area and interpolating against a calibration curve constructed from standard solutions of known concentrations.

The FE was determined by the following equation:

$$\text{FE} = \frac{2nF}{Q} \times 100\%$$

Where 2 is the number of electrons involved in the reaction, n is the number of moles of the product HCOO<sup>-</sup> or H<sub>2</sub> calculated according to HPLC and GC data, respectively. F is the Faraday constant, with a value of 96,485 C mol<sup>-1</sup> and Q is the total charge passed during the electrolysis.

The partial current density (*j*<sub>HCOO<sup>-</sup></sub>) was calculated according to the equation:

$$j_{\text{HCOO}^-} = j \times \text{FE}$$

where *j* is the total current density and FE is the Faradaic efficiency for HCOO<sup>-</sup>. This parameter reflects the effective current density associated specifically with HCOO<sup>-</sup> production, providing a direct measure of the catalytic activity toward the target product.

### 3. Results and discussion

#### 3.1. Characterization of the Bi<sub>2</sub>O<sub>2</sub>CO<sub>3</sub> samples

The XRD patterns of the synthesized samples (BOC-90, BOC-150, and Bi<sub>2</sub>O<sub>3</sub>-400) were obtained to evaluate their crystalline phase and degree, and to compare them with the commercial BOC (Fig. 1a). The hydrothermally treated Bi<sub>2</sub>O<sub>2</sub>CO<sub>3</sub> samples displayed a typical XRD pattern attributed to the tetragonal crystalline phase (PDF No 041-1488) with no detectable secondary phases, similar to the commercial BOC [10,36,37]. Bi<sub>2</sub>O<sub>3</sub>-400 sample exhibits all the peaks corresponding to the α-Bi<sub>2</sub>O<sub>3</sub> phase (PDF No 01-071-2274) with the presence of the main peak of Bi<sub>2</sub>O<sub>2</sub>CO<sub>3</sub>, which indicates that the thermal treatment was not able to completely convert the BOC into Bi<sub>2</sub>O<sub>3</sub> [38]. Hydrothermal synthesis at low temperatures (90 °C and 150 °C) led to the formation of phase pure Bi<sub>2</sub>O<sub>2</sub>CO<sub>3</sub>, albeit with distinct degrees of crystallinity. The sample synthesized at 90 °C exhibited broader XRD peaks, indicating lower crystallinity degree/reduced crystallite size compared to the sample synthesized at 150 °C. Conversely, the calcined sample (Bi<sub>2</sub>O<sub>3</sub>-400) presented sharper and more intense diffraction peaks relative to the hydrothermally synthesized samples, evidencing enhanced crystallinity as a result of the thermal treatment [37-40].

TGA analysis (Fig. 1b) exhibits mass losses that occur due to processes such as dehydration, decomposition, and volatilization. The synthesized samples of BOC-90, BOC-150, and BOCCOM show several stages of mass loss. The first stage, at low temperatures (below 200 °C), is attributed to the loss of adsorbed water and other volatile species adsorbed on the samples surface. The second stage, at higher temperatures (between 200 °C and 400 °C), corresponds to the decomposition of carbonate groups and the release of CO<sub>2</sub>. The differences in the intensities and temperatures of the mass loss stages indicate changes in the sample's crystallinity degree, composition, and the presence of impurities [3,36,41]. Bi<sub>2</sub>O<sub>3</sub>-400 sample exhibit greater thermal stability, due to the decomposition of the carbonate and formation of Bi<sub>2</sub>O<sub>3</sub>. The commercial sample serves as a reference to comparing the thermal properties of the synthesized and calcined samples.

The detailed analysis of Raman and ATR-FTIR spectra of the synthesized Bi<sub>2</sub>O<sub>2</sub>CO<sub>3</sub> samples revealed crucial information about the short-range structure and the presence of the functional groups on the materials surface, respectively. The Raman spectra, presented in Fig. 1c, demonstrated the typical behavior of Bi<sub>2</sub>O<sub>2</sub>CO<sub>3</sub> for all synthesized samples, except the calcined one. Characteristic bands were identified at 1063 cm<sup>-1</sup>, attributed to the symmetric stretching of the CO<sub>3</sub><sup>2-</sup> ion, and below 400 cm<sup>-1</sup>, corresponding to the vibrational modes of Bi-O bonds. The similarity of the profiles of the synthesized samples with that of the commercial Bi<sub>2</sub>O<sub>2</sub>CO<sub>3</sub> sample suggests a comparable short-range structure. The lower intensity of the peaks in BOC-90 and BOC-150, compared to BOCCOM, suggests a lower crystallinity in these samples, as observed by XRD. The Raman spectrum of the Bi<sub>2</sub>O<sub>3</sub>-400 showed the disappearance or weakening of peaks associated with C—O bonds (specifically the 1063 cm<sup>-1</sup> peak of CO<sub>3</sub><sup>2-</sup>) and the appearance of characteristic peaks of the Bi-O bonds present in Bi<sub>2</sub>O<sub>3</sub>. Specifically, the observed peaks at 120, 214, 317, and 447 cm<sup>-1</sup> are in good agreement with the literature for the monoclinic α-Bi<sub>2</sub>O<sub>3</sub> phase. The intensity and sharpness of these bands indicate a high degree of crystallinity [4,36,42].

ATR-FTIR analysis (Fig. 1d) reveals characteristic bands primarily associated with Bi-O vibrations, confirming the structural evolution of the samples as a function of thermal treatment. For the BOCCOM sample, an absorption band at 1740 cm<sup>-1</sup> is assigned to the C = O stretching vibration, while the typical vibrational modes of CO<sub>3</sub><sup>2-</sup> appear at 1370 cm<sup>-1</sup> (antisymmetric stretching, ν<sub>3</sub>), 1066 cm<sup>-1</sup> and 670 cm<sup>-1</sup> (symmetric stretching, ν<sub>1</sub>, and in-plane bending, ν<sub>4</sub>, respectively), and at 843 cm<sup>-1</sup> (out-of-plane bending, ν<sub>2</sub>), clearly indicating the formation of Bi<sub>2</sub>O<sub>2</sub>CO<sub>3</sub>. These signals can be observed for the samples treated at 90 and 150 °C, which confirm the formation of Bi<sub>2</sub>O<sub>2</sub>CO<sub>3</sub> as observed by XRD and

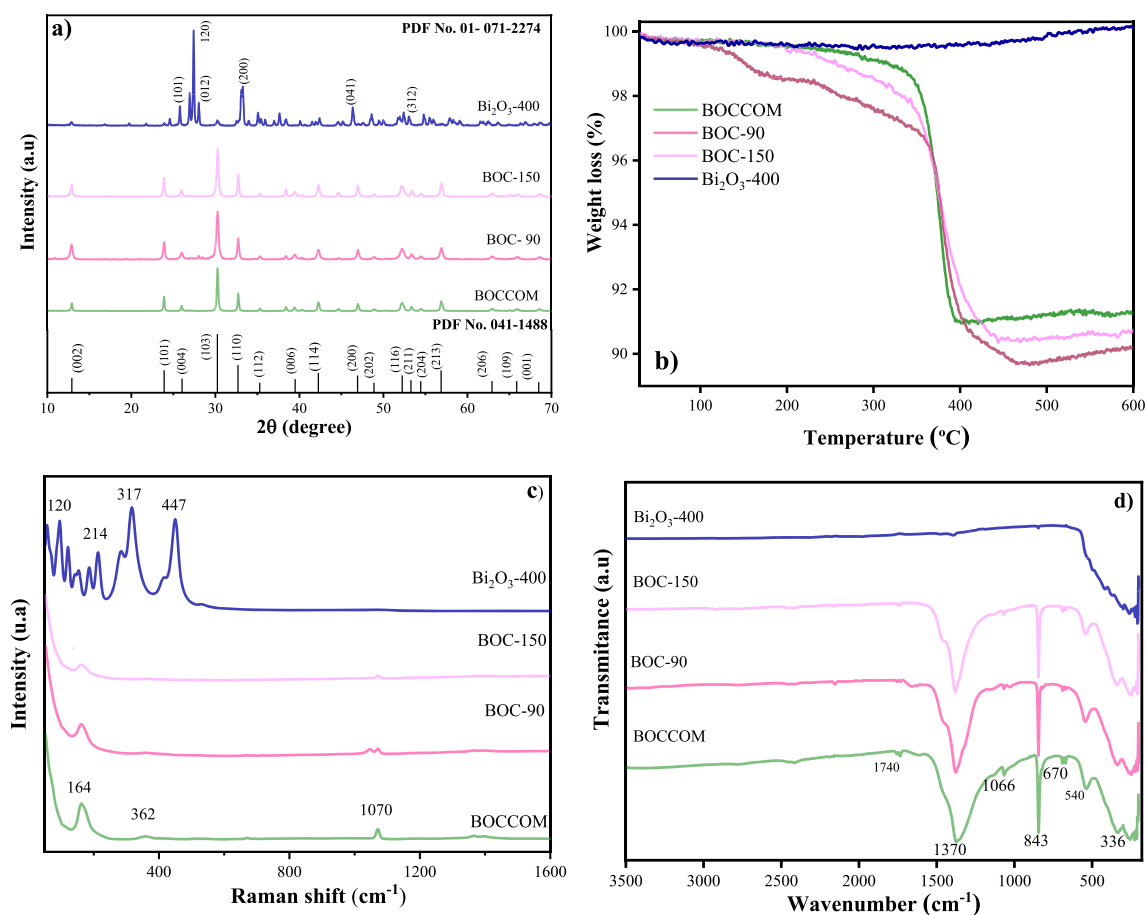


Fig. 1. a) XRD patterns b) TGA analysis c) Raman scattering spectra and d) ATR-FTIR spectra of the BOCCOM, BOC-90, BOC-150, and  $\text{Bi}_2\text{O}_3$ -400 samples.

Raman analyses. In contrast, the sample calcined at 400 °C ( $\text{Bi}_2\text{O}_3$ -400) no longer exhibits carbonate-related bands, being dominated by broad absorptions below 500  $\text{cm}^{-1}$  that are attributed to Bi-O vibrations, thereby confirming the complete conversion of  $\text{Bi}_2\text{O}_2\text{CO}_3$  into  $\text{Bi}_2\text{O}_3$ , in agreement with TGA and Raman data [36,42,4,43]. It is important to note that although FTIR spectra suggest complete decomposition of carbonate species at 400 °C, XRD analysis reveals a small residual crystalline fraction of  $\text{Bi}_2\text{O}_2\text{CO}_3$ , which can be attributed to the higher sensitivity of XRD to minor crystalline phases compared to FTIR.

The material's morphology was investigated by SEM, illustrated in Fig. 2. The hydrothermal synthesis carried out at low temperatures (90 °C and 150 °C) resulted in the formation of particles with varied morphologies, including nanosheets and microspheres. The particles synthesized at these temperatures exhibited micrometric sizes and nanometric thicknesses, where the sample BOC-90 exhibited particle size smaller than BOC-150. In contrast, the sample calcined at 400 °C exhibits relatively larger sizes, characterized by agglomerated particles. Additionally, it can be observed that BOC-90 and BOC-150 exhibited particle size smaller than the commercial sample.

The analysis of  $\text{N}_2$  adsorption-desorption isotherms using the Brunauer-Emmett Teller (BET) method for the BOC-90, BOC-150,  $\text{Bi}_2\text{O}_3$ -400, and BOCCOM samples (Fig. S1) reveals significant differences in their specific surface areas (SSA), pore volumes, and average pore sizes (Table 1). The  $\text{Bi}_2\text{O}_3$ -400 sample exhibited the largest surface area (30.86  $\text{m}^2 \text{g}^{-1}$ ) and the highest pore volume (0.06  $\text{cm}^3 \text{g}^{-1}$ ). Although its average pore size (3.04 nm) is intermediate, the combination of high area and volume indicates a well-developed and accessible porous structure. The BOCCOM sample served as a reference point for the lowest porosity in this study. With the smallest surface area (11.96  $\text{m}^2 \text{g}^{-1}$ ) and the lowest pore volume (0.015  $\text{cm}^3 \text{g}^{-1}$ ), in addition to a very

reduced pore size (1.92 nm), BOCCOM suggests a less porous and less accessible structure for nitrogen adsorption. The BOC-90 and BOC-150 samples exhibit intermediate characteristics but with important distinctions. BOC-90 exhibits a SSA value of 21.6  $\text{m}^2 \text{g}^{-1}$ , 0.048  $\text{cm}^3 \text{g}^{-1}$  of pore volume, and 3.59 nm pore size, demonstrating considerable porosity that surpasses BOCCOM in all aspects. BOC-150 exhibits a smaller surface area (7.4  $\text{m}^2 \text{g}^{-1}$ ) than BOCCOM, while it compensates with a larger pore volume (0.029  $\text{cm}^3 \text{g}^{-1}$ ) and, notably, the largest pore size (6.83 nm) among all samples. This characteristic suggests a structure with wider pores, which can be advantageous for the diffusion or adsorption of larger molecules that would not be able to access smaller pores [44-47].

### 3.2. Electrocatalytic performance of BOC samples for ECR

The electrocatalytic performance of BOC samples for  $\text{CO}_2$  reduction were analyzed by LSV curves and by electrolysis experiments at different applied potential (chronoamperometry) to assess the selectivity for  $\text{HCOO}^-$  production ( $\text{FE}_{\text{HCOO}^-}$ ). A comparative analysis of the results (Fig. 3) revealed distinct catalytic activities among the evaluated materials under the same reaction conditions. The  $\text{Bi}_2\text{O}_3$ -based sample, calcined at 400 °C, showed the lower performance for  $\text{HCOO}^-$  production, with a current density of approximately 90  $\text{mA cm}^{-2}$  (Fig. 3a) and a  $\text{FE}_{\text{HCOO}^-}$  of about 72% at -1.2 V vs. RHE, using a 0.5 M KOH electrolyte (Fig. 3b). The synthesized BOC samples demonstrated superior performance in the conversion of  $\text{CO}_2$  to  $\text{HCOO}^-$ . The BOC-90 catalyst exhibited a current density of approximately -125  $\text{mA cm}^{-2}$  and a  $\text{FE}_{\text{HCOO}^-}$  of 94% under the same conditions. Notably, the BOC-150 catalyst stood out as the most promising among the synthesized samples, achieving a current density of -140  $\text{mA cm}^{-2}$  and  $\text{FE}_{\text{HCOO}^-}$  of 95% at

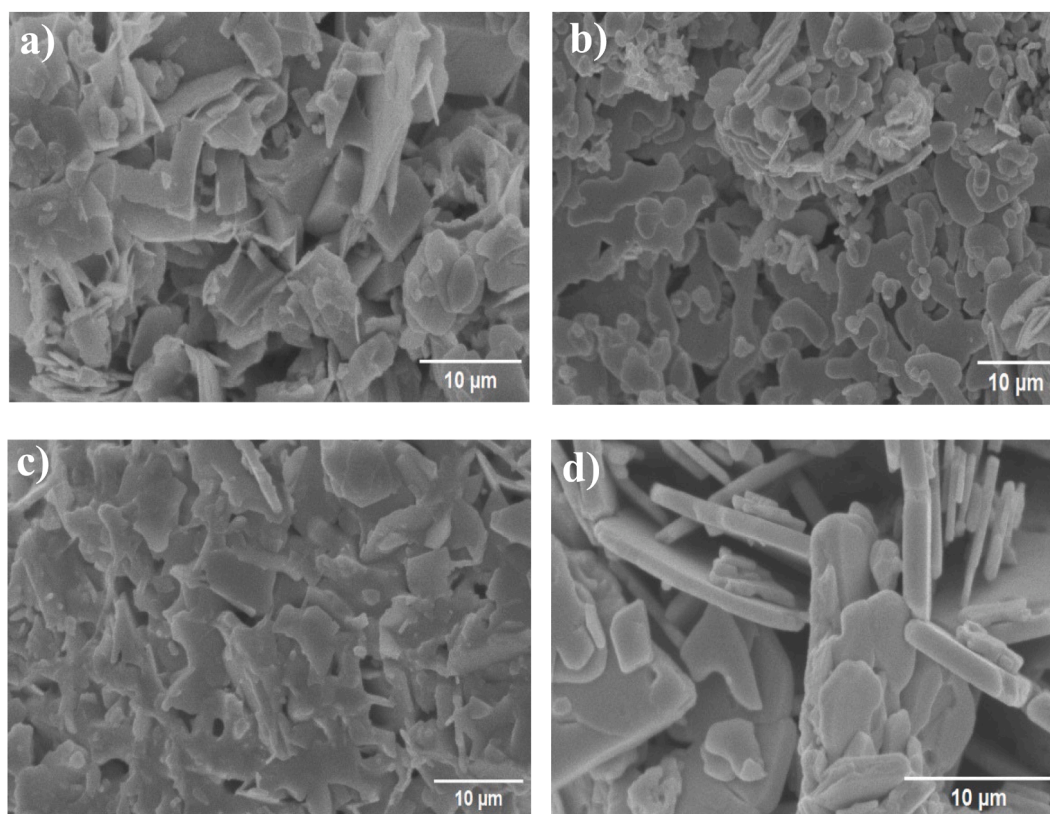


Fig. 2. SEM images of the synthesized samples (a) BOC-90, (b) BOC-150, (c) Bi<sub>2</sub>O<sub>3</sub>-400, and (d) BOCCOM.

Table 1

Nitrogen adsorption-desorption data of the BOC-90, BOC-150, Bi<sub>2</sub>O<sub>3</sub>-400, and BOCCOM samples.

Samples	SSA (m <sup>2</sup> g <sup>-1</sup> )	Pore volume (cm <sup>3</sup> g <sup>-1</sup> )	Pore size (nm)
BOC-90	22	0.05	3.6
BOC-150	7	0.03	6.8
Bi <sub>2</sub> O <sub>3</sub> -400	31	0.06	3.0
BOCCOM	12	0.02	1.9

the same potential and electrolyte concentration. These results confirm the effectiveness of the 2D materials approach, which, according to the literature, substantially increases current density [48]. The high FE for HCOO<sup>-</sup>, greater than 90%, is consistent with expectations for Bi based electrocatalysts [42,49]. The commercial BOC material presented a current density of about -100 mA cm<sup>-2</sup> and a FE<sub>HCOO<sup>-</sup></sub> of 78% at a potential of -1.2 V vs. RHE. This evidence the effectiveness of the synthesis methodology employed in this study for obtaining BOC catalysts with enhanced catalytic performance and greater selectivity to produce HCOO<sup>-</sup> from CO<sub>2</sub> reduction compared to the commercial material, in a flow-cell system with gas diffusion electrodes.

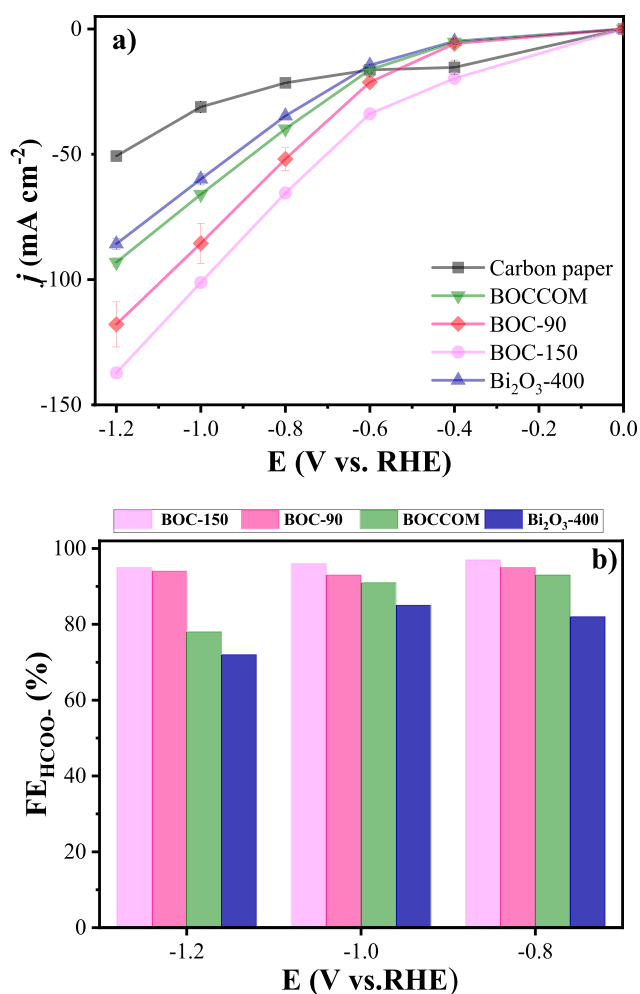
Additionally, the carbon paper used as the gas diffusion electrode substrate was systematically evaluated by both LSV and 30 min chronoamperometry experiments under identical conditions to those applied for the BOC electrodes (Fig. 3). In the LSV curves, the bare carbon paper exhibited a significantly lower current density, reaching approximately -50 mA.cm<sup>-2</sup> at -1.2 V vs RHE, which is markedly inferior to that obtained for the synthesized BOC samples. More importantly, product analysis after electrolysis revealed that, in the absence of BOC samples, no HCOO<sup>-</sup> or any other carbon-containing product was detected in either the liquid or gas phase. The only product identified by GC-TCD was H<sub>2</sub>, with a Faradaic efficiency of 100% within experimental accuracy at all investigated potentials. Because no formate was formed on the

bare substrate, these data were not included in Fig. 3b, which focuses on formate production.

These control experiments clearly demonstrate that the carbon paper itself does not exhibit intrinsic activity toward ECR and acts solely as an HER-active conductive support under the studied conditions. Therefore, the selective formation of HCOO<sup>-</sup> observed in the catalyst-coated electrodes can be unequivocally attributed to the intrinsic catalytic properties of the BOC and Bi<sub>2</sub>O<sub>3</sub> phase, ruling out any contribution from the gas diffusion substrate to the reported activity and selectivity.

Electrochemical impedance spectroscopy (EIS) measurements were performed before and after electrolysis in order to evaluate possible interfacial and structural reconstruction effects induced under cathodic operation. The EIS results recorded prior to the electrolysis (Fig. 4a-b) reveal clear differences in the area-normalized charge-transfer resistance (R<sub>ct</sub>) among the samples investigated. As we can see in Table S2, the higher R<sub>ct</sub> observed for BOC-90 and BOCCOM suggests more hindered electron-transfer kinetics, which may be associated with lower electrical conductivity and/or the presence of surface species formed during the milder hydrothermal synthesis conditions. In contrast, BOC-150 exhibited the lowest R<sub>ct</sub> value, consistent with its superior ECR performance [23].

After electrolysis at -1.0 V vs RHE for 10 min (Fig. 4c-d), a decrease in R<sub>ct</sub> was observed for all samples. This behavior is expected, since partial reduction of Bi<sup>3+</sup> to metallic Bi under cathodic polarization can increase the electrical conductivity of the catalyst surface. Under these conditions, BOC-150 maintained the lowest R<sub>ct</sub> (followed by BOCCOM, Bi<sub>2</sub>O<sub>3</sub>-400, and BOC-90 (Table S2 and S3). The consistently lower R<sub>ct</sub> of BOC-150 indicates more favorable interfacial charge-transfer kinetics under operational conditions, in agreement with previous reports correlating reduced R<sub>ct</sub> values with enhanced electrocatalytic performance [50]. Additionally, BOC-150 displays the highest constant phase element (CPE) value, suggesting a larger effective interfacial capacitance, which is typically associated with a higher electrochemically



**Fig. 3.** (a) LSV curves for carbon paper and BOC samples in 0.5 M KOH electrolyte in an electrochemical flow cell, applying potential range of  $-0.4$  to  $-1.2$  vs. RHE. (b)  $FE_{HCOO^-}$  obtained at corresponding applied potential ( $-0.8$  to  $-1.2$  V) during 30 min. Carbon paper is not included in panel (b) because no  $HCOO^-$  production was detected.

active surface area and improved electrode–electrolyte interaction [51]. Overall, although reconstruction occurs under cathodic polarization, the comparable impedance features before and after electrolysis and the consistently lower  $R_{ct}$  of BOC-150 confirm its superior charge-transfer properties, which directly contribute to its improved catalytic performance.

The evaluation of ECSA through cyclic voltammetry is essential to rationalize the catalytic performance, since a larger electrochemically accessible surface correlates with higher activity in  $CO_2$  reduction. This ECSA was estimated by calculating the double-layer capacitance ( $C_{dl}$ ), as shown in Fig. 5, from the current response obtained at different scan rates (Fig. S2). The synthesized samples (BOC-90, BOC-150,  $Bi_2O_3$ -400) exhibited higher  $C_{dl}$  values compared to the BOCCOM sample, evidencing the effectiveness of structural modification and thermal treatments. Among them, BOC-90 presented the largest ECSA, attributed to a more favorable morphology and phase composition that increased surface area and electroactive sites. BOC-150 also showed an enhanced ECSA relative to the reference, though slightly lower than BOC-90, which may be associated with partial agglomeration or pore collapse induced by higher temperature treatment, in agreement with SSA analysis.  $Bi_2O_3$ -400 displayed improved ECSA compared to BOCCOM, but lower than the BOC samples, indicating that excessive crystallization at elevated temperature reduced surface area and ion accessibility.

These results confirm that moderate treatments, such as  $90^\circ C$ , provide the most suitable balance between crystallinity and surface exposure, explaining the superior catalytic performance of BOC-90 and BOC-150 in ECR [24,25].

The XPS analysis (Fig. 6a) revealed significant differences between the BOC-90 and BOC-150 samples before and after the ECR. High-resolution spectra (Fig. S3 a, b and c) indicated a higher proportion of  $Bi^{2+}$  species and oxygen vacancies in the BOC-90 powder (Fig. S3), which remained nearly unchanged after the reaction, suggesting partial poisoning of these sites. In contrast, BOC-150 exhibited complete surface oxidation to  $Bi^{3+}$  during electrocatalysis, evidencing active surface reconstruction and improved accessibility of catalytic sites. This process explains its higher FE and partial current density for  $HCOO^-$ , even with a lower surface area and porosity compared to BOC-90. It can be observed that the bismuth signals decreased dramatically for BOC-90 after the ECR, indicating that this sample exhibits low stability, probably due to a cathodic dissolution process. In contrast, the BOC-150 sample retained a significant amount of bismuth on the electrode surface after the reaction, which explains its higher catalytic activity. Additionally, the F 1s signals (Fig. S4) can be ascribed to the carbon paper substrate, which exhibits hydrophobic characteristics because of the PTFE treatment. This feature becomes particularly pronounced for the BOC-90 sample after the ECR, likely due to the exposure of the carbon paper surface following Bi leaching into the electrolyte. These findings corroborate that surface reconstruction ability and the regeneration of active  $Bi^{3+}$  species are key factors determining the superior electrocatalytic performance of BOC-150 [52,53].

The NIR spectra of the as-synthesized powders (Fig. 6b) exhibit distinct signatures of hydroxyl species and adsorbed water, with detailed assignments provided in Table S2 (SI). Bands at  $4330$  and  $4500\text{ cm}^{-1}$  are attributed to structural OH groups and lattice-bound hydroxyls [54], while features in the  $4900$ – $5200\text{ cm}^{-1}$  range correspond to different hydrogen-bonding states of water molecules adsorbed on the surface [55,56]. At higher energies ( $7000\text{ cm}^{-1}$ ), the observed bands originate from surface hydroxyls in distinct coordination environments [55–57]. Notably, BOC-150 displayed only a broad feature near  $7000\text{ cm}^{-1}$ , indicating the presence of weakly adsorbed hydroxyls and the absence of strongly bonded water. This unique surface state prevents site blocking and explains the superior electrocatalytic activity of BOC-150 toward  $CO_2$  to  $HCOO^-$  conversion. In contrast, BOC-90 exhibits pronounced contributions from strongly adsorbed water, which likely hinders charge transport by acting as an insulating component.

The electrolyte concentration and the ration between catalyst and carbon paper are parameters relevant in the optimization of the electrode performance for any electrocatalytic application. Therefore, both parameters were evaluated using the sample with the best performance, BOC-150, as can be seen in (Fig. 7). The current density is strongly influenced by KOH concentration. A positive correlation was observed between KOH concentration and current density, with the 2.0 M KOH electrolyte exhibiting the highest values ( $-185\text{ mA cm}^{-2}$  at  $-1.2$  V vs. RHE). This increase can be attributed to two main factors: (i) the improvement in the ionic conductivity of the solution, which facilitates charge transport and minimizes ohmic losses; and (ii) the favoring of the formation of electroactive carbon species, such as bicarbonate, in more alkaline solutions, making them more available at the electrode–electrolyte interface for the reduction reaction [17,58,59].

Selectivity for  $HCOO^-$  (Fig. 7b) showed strong dependence on electrolyte concentration, with the 0.5 M KOH solution being the most favorable condition, with FE of about 95% at  $-1.2$  V vs. RHE and 80% at  $-0.8$  and  $-1.0$  V, in addition to high partial current density. At higher concentrations (1.0 M and 2.0 M KOH), despite the increase in total current density, selectivity was reduced, indicating that higher overall activity does not necessarily imply higher charge conversion to  $HCOO^-$  [60–62]. Additionally, in alkaline systems, increasing KOH concentration can intensify  $OH^-$  ion crossover through anionic membranes, modifying the local pH at the cathode and contributing to the loss of

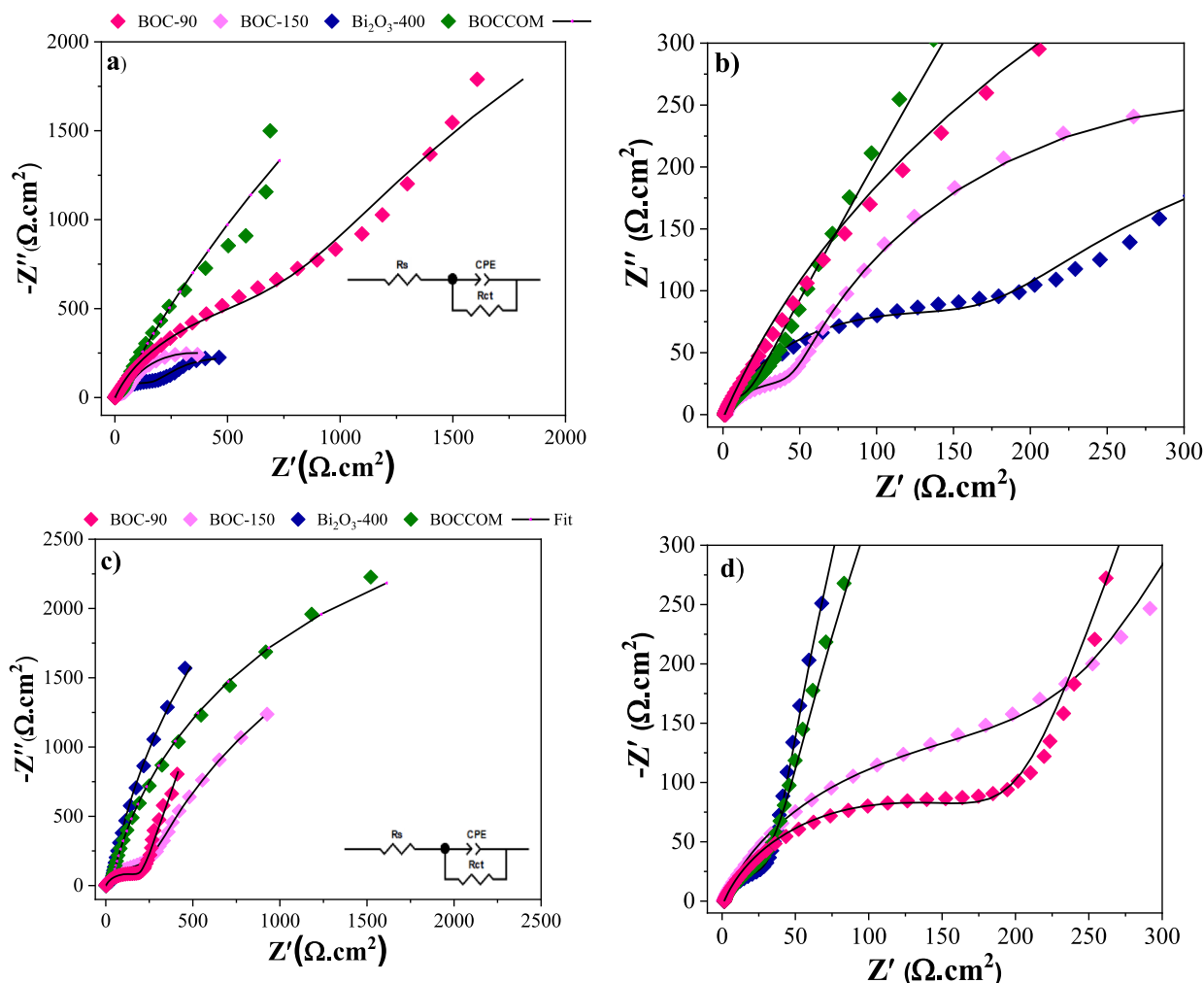


Fig. 4. Electrochemical impedance spectra of BOCCOM, BOC-90, BOC-150 and BOC-400 samples in 1.0 M KOH electrolyte (Nyquist plots); before electrolysis (A) and (B), and after electrolysis (C) and (D).

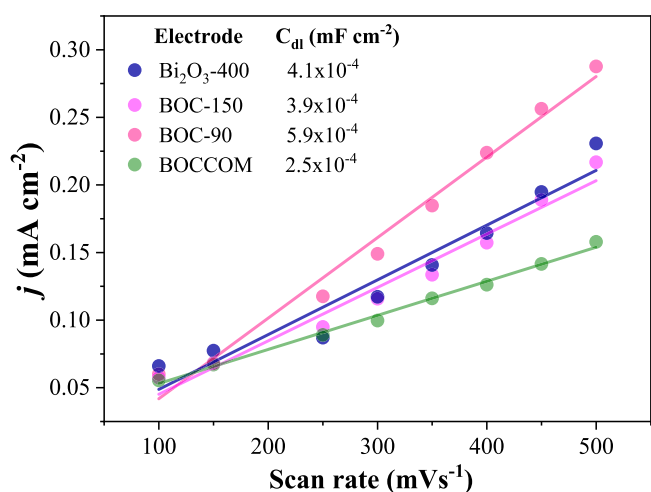


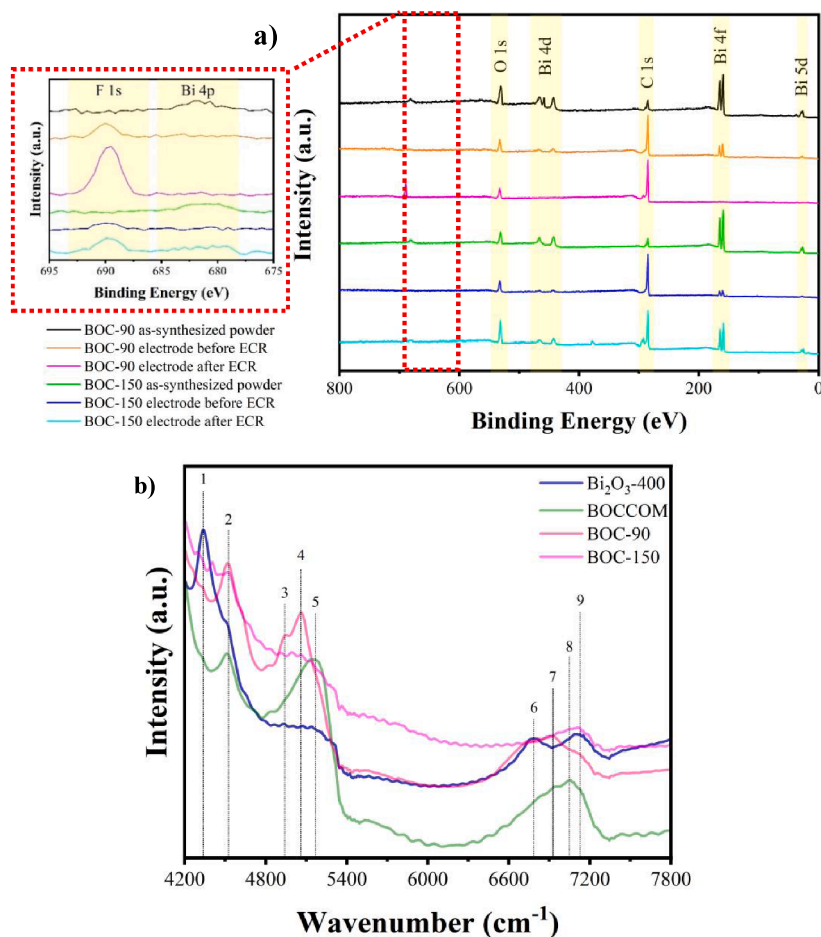
Fig. 5. Double-layer capacitance ( $C_{dl}$ ) obtained by cyclic voltmetry studies at different scan rates from 100 to 500  $\text{mVs}^{-1}$  of BOCCOM, BOC-90, BOC-150 and  $\text{Bi}_2\text{O}_3$ -400 samples.

selectivity observed at high alkalinities [49,63]. In this context, the use of proton exchange membranes has been recommended to decouple the

intrinsic effects of electrolyte concentration from those associated with anionic transport, allowing a more accurate assessment of the selectivity and mechanisms of ECR [49,64].

Fig. 7c-d showed the electrocatalytic activity of the different electrodes modified with the BOC-150 catalyst in different proportions of carbon black in a 1 M KOH. The electrode prepared with 75% of BOC-150 demonstrates the best performance in terms of current density and FE. At  $-1.2$  V vs. RHE, this electrode achieves a current density around  $-250$   $\text{mA cm}^{-2}$  and  $\text{FE}_{\text{HCOO}^-}$  of about 99%. This value is superior to that obtained with 50% BOC-150 ( $-160$   $\text{mA cm}^{-2}$ ) and 100% BOC-150 ( $-190$   $\text{mA cm}^{-2}$ ) at the same potential. This result meets the requirement for commercially relevant current densities ( $>200$   $\text{mA cm}^{-2}$ ) [65,66]. The 75% BOC-150 composition exhibited the best electrocatalytic performance, resulting from a favorable balance between the high density of active sites and the adequate electrical conductivity provided by carbon, as reflected in its lowest  $R_{ct}$  value (Fig. S6). In contrast, the 50% BOC-150 formulation, although benefiting from a higher conductive fraction, is limited by the reduced number of catalytic sites, while the electrode composed of 100% BOC-150 displays an even higher  $R_{ct}$ , highlighting the lack of efficient conductive pathways and optimal interfaces. Therefore, the 75% composition represents the most favorable condition, combining catalytic activity, conductivity, and mass transport, which ultimately leads to the highest current density.

Preliminary experiments using carbon paper as the electrode support showed satisfactory stability performance only during the initial 30 min



**Fig. 6.** a) XPS survey spectra of BOC-90 and BOC-150 powders (as-synthesized) and electrodes before and after the ECR reaction. Near-infrared spectrum (NIR) of the as-synthesized powders (Bi<sub>2</sub>O<sub>3</sub>-400, BOC-90, BOC-150) and commercial Bi<sub>2</sub>O<sub>2</sub>CO<sub>3</sub> (BOCCOM).

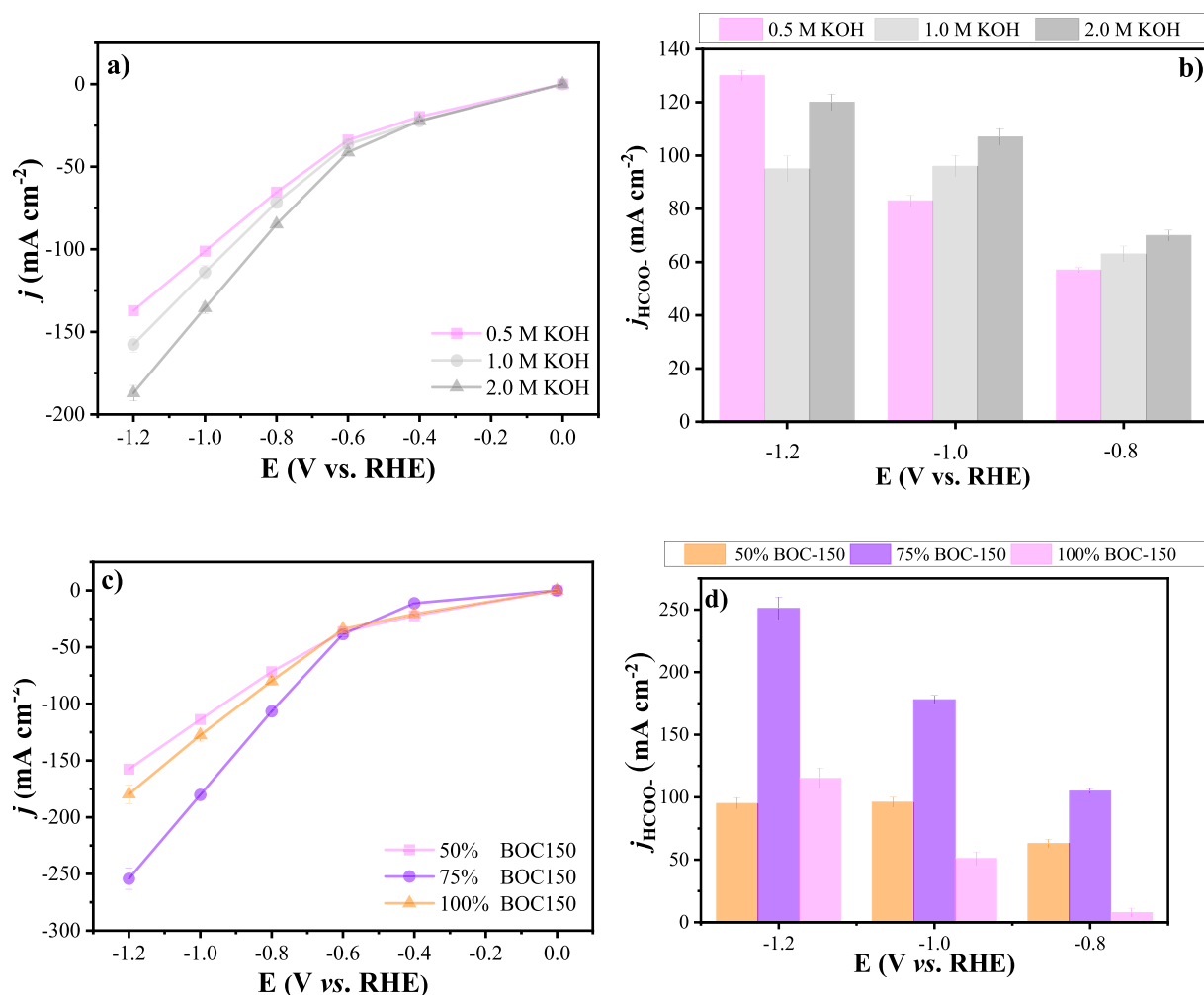
of operation. Subsequently, a rapid deterioration in electrochemical stability was observed, which is attributed to progressive electrode flooding, as observed by contact angle measurements (Fig. S7). This phenomenon severely restricts CO<sub>2</sub> mass transport to the active sites and promotes competing reactions, particularly HER, leading to potential instability and a marked decrease in FE<sub>HCOO</sub><sup>-</sup>. Similar flooding-induced limitations in carbon-based gas diffusion electrodes under alkaline CO<sub>2</sub> reduction conditions have been widely reported in the literature. In contrast, when the BOC-150 catalyst was directly deposited onto a PTFE membrane, the electrochemical stability was significantly improved. Chronopotentiometric measurements conducted at a constant current of -40 mA in 0.5 M KOH demonstrated stable operation over 6 h, with the FE<sub>HCOO</sub><sup>-</sup> remaining consistently high, predominantly in the range of 80 and 90%. The potential time profiles over the 6 h operation, as well as the stability behavior as a function of the applied current can be seen in the Fig. S8. These results clearly indicate that the stability loss observed with carbon paper does not arise from the intrinsic properties of the BOC-150 catalyst, but rather from electrode architecture related flooding effects. The PTFE based configuration effectively mitigates electrolyte accumulation, ensures efficient reactant transport, and enables sustained and selective CO<sub>2</sub> electroreduction under alkaline conditions.

The electrochemical stability of the BOC-150 catalyst was evaluated by chronopotentiometry at a constant current of -40 mA for 6 h in 0.5 M KOH, using an electrode configuration in which the catalyst was directly deposited onto a PTFE membrane (Fig. 8). After a brief initial conditioning period, the electrode potential stabilized and remained nearly constant throughout the entire operation time, with no noticeable drift, indicating high electrochemical stability under alkaline conditions. The

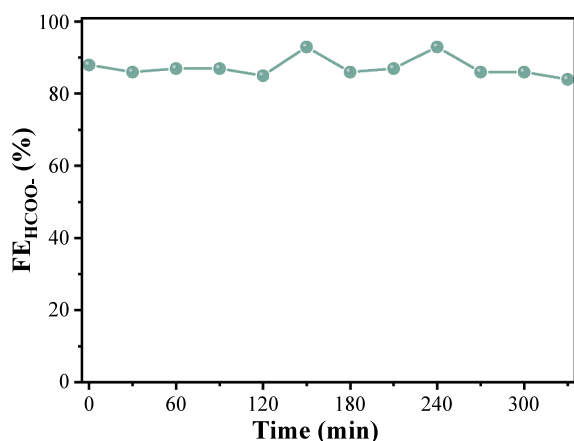
FE<sub>HCOO</sub><sup>-</sup> remained high, around 80%, over the 6 h test, demonstrating sustained catalytic selectivity and effective suppression of competing reactions, particularly HER. The PTFE based configuration effectively mitigates electrolyte accumulation, ensures efficient reactant transport, and enables sustained and selective CO<sub>2</sub> electroreduction under alkaline conditions [67].

#### 4. Conclusion

In this study, we successfully developed highly efficient and selective electrocatalysts for the ECR to HCOO<sup>-</sup> under industrially relevant conditions. BOC-150 nanosheets emerged as the superior catalyst, demonstrating the highest current density for HCOO<sup>-</sup> production. Optimizing the electrolyte concentration to 1.0 M KOH and the electrode composition to 75% BOC-150 catalyst and 25% carbon black further boosted performance, achieving an impressive current density of -250 mA cm<sup>-2</sup> and a FE<sub>HCOO</sub><sup>-</sup> higher than 90%. BOC-150 consistently showed the best overall performance in terms of both HCOO<sup>-</sup> production rate and selectivity. EIS confirmed that BOC-150 exhibited lowest charge transfer resistance, indicating favorable reaction kinetics. Complementary spectroscopic analyses provided further insight into the structure-performance relationship. NIR spectra revealed the presence of strongly adsorbed water species on the BOC-90 sample, which likely hindered CO<sub>2</sub> adsorption and charge transfer, explaining its inferior catalytic performance. Moreover, XPS analysis after the ECR confirmed the instability of BOC-90, evidenced by the significant decrease in bismuth signals due to partial dissolution in the electrolyte. BOC-150 prepared on PTFE membrane as GDE was stable during 6 h with



**Fig. 7.** (a) LSV curves and (b)  $\text{FE}_{\text{HCOO}^-}$  obtained at different potentials after 30 min using 50% BOC-150 sample evaluated under varying KOH electrolyte concentrations (0.5 M, 1.0 M, and 2.0 M). (c) LSV curves and (d) FE obtained at different potentials after 30 min using BOC-150 sample with different ratio between catalyst and carbon black (50%, 75%, and 100%).



**Fig. 8.** Chronopotentiometric stability of the BOC150 catalyst at  $-40$  mA in 0.5 M KOH, showing  $\text{FE}_{\text{HCOO}^-}$  over time.

$\text{FE}_{\text{HCOO}^-}$  higher than 80%. The exceptional performance of the 2D BOC nanosheets, particularly those synthesized under optimized hydrothermal conditions, is attributed to their unique morphological and electronic properties. These properties provide a high density of active sites

and significantly facilitate charge transfer, underscoring their considerable potential as advanced electrocatalysts for CO<sub>2</sub> conversion.

#### CRediT authorship contribution statement

**Mateus J. Tomas:** Writing – original draft, Methodology, Investigation, Formal analysis. **Daniel R. Sevene:** Writing – original draft, Methodology, Investigation, Formal analysis. **Gonçalves J. Marrenjo:** Writing – original draft, Methodology, Investigation, Formal analysis. **Cleiton P.M. Silva:** Writing – original draft, Methodology, Investigation. **Jessica A. de Oliveira:** Writing – original draft, Supervision, Formal analysis, Data curation. **Caue Ribeiro:** Writing – review & editing, Supervision, Funding acquisition. **Osmando F. Lopes:** Writing – review & editing, Validation, Supervision, Resources, Project administration, Data curation, Conceptualization.

#### Declaration of competing interest

The authors declare the following financial interests/personal relationships which may be considered as potential competing interests:

Osmando F. Lopes reports financial support was provided by Minas Gerais State Foundation of Support to the Research. Osmando F. Lopes reports financial support was provided by National Council for Scientific and Technological Development. If there are other authors, they declare

that they have no known competing financial interests or personal relationships that could have appeared to influence the work reported in this paper.

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## Supplementary materials

Supplementary material associated with this article can be found, in the online version, at [doi:10.1016/j.electacta.2026.148623](https://doi.org/10.1016/j.electacta.2026.148623).

## Data availability

Data will be made available on request.

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