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Improved Purification Process of β - and α -Trypsin Isoforms by Ion-Exchange Chromatography

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ABSTRACT

The purpose of this work was to improve the separation and yield of pure β - and α -trypsin isoforms by ionexchange chromatography and to characterize some physical–chemical properties of these isoforms. Purification of trypsin isoforms was performed by ion-exchange chromatography in 0.1 mol/L tris-HC buffer, pH 7.10 at 4°C. The sample loading, salt concentration, flow rate and pH of mobile phase were varied to determine their effects on the resolution of the separation. The resolution was optimized mainly between β - and α -trypsin. Pure isoforms were obtained by chromatographying 100 mg of commercial trypsin during seven days, yielding 51 mg of high purity β trypsin and 13 mg of α -trypsin partially pure, with small amounts of contaminating of ψ -trypsin. Thus, time and resolution of purification were optimized yielding large amounts of pure active enzymes that are useful for several research areas and biotechnology.

Key words: Trypsin isoforms, resolution, ion-exchange chromatography, purification, specific activity, mass spectrometry

INTRODUCTION

Trypsin is the first discovered and probably the best characterized enzyme. It has been known for more than 130 years that pancreatic juice is able to digest proteins (Graf and Szilágyi, 2003). This protein was among the first proteolytic enzymes isolated in pure form in enough amounts for exact chemical and enzymological studies.

The structure of trypsin molecule and the mechanism of its action have been studied in

considerable detail. Therefore, it provides an important and widely used model system for kinetic as well as physical and biophysical studies. Such studies require a well-defined form of trypsin, preferably the uncleaved, single chain β -trypsin which retains full enzymatic activity. Most commercial trypsin preparations contain some inactive isoforms and ψ -trypsin with low amidasic activity (Schroeder and Shaw, 1968 and Smith and Shaw, 1969), in addition to the two most active forms, β -trypsin and α -trypsin, and some autolysis

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products. The content of the individual constituents is often unknown and variable, and small amounts of pure β - and α -trypsin are obtained.

Various chromatographic methods have been developed for purification of trypsin and their isoforms including ion-exchange (Schroeder and Shaw, 1968 and Gooding and Schmuck, 1983), hydrophobic interaction (Strop and Cechová, 1981), reversed-phase (Titani et al., 1982) and affinity chromatography (Feinstein, 1970 and Chang Shi et al., 1996). The method developed by Schroeder and Shaw (Schroeder and Shaw, 1968) using ion-exchange chromatography on SE-Sephadex at neutral pH with benzamidine in the elution buffer has proved to be the most successful and is frequently employed. Despite this previous methodology has shown to be able to separate trypsin isoforms, it presents low yield, requires a long time of purification and supplies impure isoforms with low resolution among their main peaks. In this paper we show an optimization of the methodology developed by Schroeder and Shaw by increasing the separation effectiveness of β -and α -trypsin based on differences of salt concentrations, sample loading, flow rate and pH. Optimal conditions for analytical as well as preparative scale separations were developed.

MATERIALS AND METHODS

Proteins and Chemicals

Tris(hydroxymethyl) aminomethane, benzamidinehydrochloride, bovine trypsin type III (T8253) LOT 125HO676 EC 3.4.21.4, Nα-benzoyl-_{DL}arginine-p-nitroanilide (BApNA) were purchased from Sigma (St. Louis, MO, USA). Calcium chloride was purchased from Merck (Darmstadt, Germany). Sodium chloride and acetonitrile (HPLC grade) were purchased from Carlo Erba (Rodano, MI. Italy). Acetic acid and hydrochloride acid were purchased from Synth (Diadema, SP. Brazil). Formic acid was purchased from Reagen (Rio de Janeiro, RJ, Brazil). p-Nitro phenyl pguanidino benzoate-HCl (NPGB) was purchased from INC Pharmaceuticals (Cleveland, Ohio. USA). Diethylbarbituric acid (Veronal) was purchased from Riedel - De Haen (Seelze-SE-SEPHADEX-C50 Hannover, Germany). matrix cation exchanger (capacity: 2.3 meq/g and particle size: 40.0-120.0 µm) was purchased from Pharmacia Fine Chemicals INC (Uppsala, Sweden). Type I water was purified with a Barnstead nanopure DiamondTM Ultrapure water system (Barnstead International, Dubuque, USA).

Equipments

The following equipaments were employed UVvisiblerecording spectrophotometer UV-160-A-Shimadzu (Kyoto, Japan), automatic fraction collector LKB-Frac-100-Pharmacia (Uppsala, Sweden), Q-Tof Micromass Mass Spectrometer (Manchester, UK), freeze dry system Labconco (Kansas City, USA).

Mobile phase preparation

A 0.10 mol/L tris(hydroxymethyl) aminomethane buffer, pH 7.10 or 7.69, containing 90-150 mmol/L NaCl and 20.0 mmol/L CaCl₂, 1.0 mmol/L benzamidine-hydrochloride and other buffers were prepared in deionized water using hydrochloride acid to adjust the pH. All preparations were adjusted at room temperature. The mobile phase was prepared considering chromatographic temperature, in such a way that at 4°C the value of pH increased to the desired pH. This was possible due to the knowledge of temperature coefficient (-0.028/°C) dpK/dT of tris (Beynon and Easterby, 1996).

Stationary phase preparation and packing of the column

In order to improve the method developed by Schroeder and Shaw (Schroeder and Shaw, 1968), we reproduced the chromatographic system used in 1968 by these authors, with small modifications in the ionic strength of mobile phase. The chromatographic system used a stationary phase SE-Sephadex (C-50 beaded) (Pharmacia, 1977) that was prepared in the same way described in the classical article by Schroeder and Shaw (Schroeder and Shaw, 1968).

To be sure that the matrix was equilibrated, the pH and absorbance of the applied buffer were compared to those of the eluent. To avoid the matrix compression during the chromatographic process or by different buffer conditions, resulting in low resolution, for each experiment testing different flow rates, salt concentrations, pH and sample loading the processes of matrix removal from the column followed by regeneration and repacking was repeated before of the next separation (Bollag, et al., 1996). Column efficiency was monitored in each test group by measuring the level of variation of the stationary phase and peak symmetry (Harris, 2001 and Skoog, 1980).

Sample preparation and application

Commercial trypsin samples of 100-300 mg were dissolved in 30 mL of the mobile phase in an ice bath and applied to the top of the column.

Ion-exchange chromatography

Enzymes were purified by workbench cationic ion-exchange chromatography at 4°C, with isocratic elution in a column with 85.0 x 2.2 cm internal diameter (i.d), 323 mL volume. The column worked under hydrostatic pressure (20 cm of water column) and it was operated with the solvent reservoir bellow the head of the column to avoid packing. The fractions (3.5 mL/tube) were colleted after elution with 140 mL of buffer using a LKB-Frac-100 with tubes containing 250 µL of 1.5 mol/L of aqueous solution of formic acid to preserve enzymatic activity after chromatography. The eluate was monitored by measurements of optical density at 280 nm. The fractions were pooled, dialyzed against 1.0 mmol/L HCl at 4°C, by a dilution factor of 10⁶ times sample volume for 24 h, lyophilized, aliquoted, (Everse and Stolzenbach, 1971) and stored at 4°C.

Test conditions

The following variables that could affect the chromatographic resolution were tested:

- Flow rates of 60, 70, 100, 120, 130, 140 and 150 µL/min;
- NaCl of 90, 100, 125, 150, mmol/L;
- Sample loadings of 100, 150, 200, 250 and 300, mg of commercial trypsin;
- pH of 7.10 and 7.69 at 4°C.

All tests were done in triplicate for each point.

Data analysis

Calculation of chromatographic resolution was performed by the following equation (Harris, 2001).

R= [(PEAK VR2 – PEAK VR1) / 0.5 X (W2 + W1)]

where:

- peak Vr = retention volume of peak
- w = width of the base of the peak

The values of w and peak Vr were obtained by deconvolution analysis of chromatograms using by the Origin[®] 5.0 software.

Protein concentration determination

The protein concentration was determined spectroscopically using the trypsin molar extinction coefficient at 280 nm of $\xi = 40,000 \text{ mol}^{-1}\text{L.cm}^{-1}$ (Walsh and Wilcox, 1971). Measurements were done in a 1.0 mmol/L HCl solution in triplicate.

Molecular mass determination

Molecular masses and purity of proteins were determined by electrospray mass spectrometry using a Q-ToF MicroTM (Micromass, UK) equipped with an electrospray ionization source operated in the positive ion mode. Samples (20 µL) from aliquots of 1.0 mL at 1.0 mg/mL concentration spectroscopically measured in HCl 1.0 mmol/L were resuspended in 20 μ L of the aqueous solution of 50% (v/v) of acetonitrile plus 0.2 % (v/v) formic acid. Samples were injected directly into the electrospray source via a loop injector at a solvent flow rate of 10 µL/min. Experimental conditions were: source (capillary = 3000 V, sample cone = 70 V, and extraction cone = 2 V) ToF (flight tube = 2500 V and MCP detector= 5630 V). Mass spectrometer calibrations were performed using sodium iodide in the 100-3000 m/z range. The spectrum data obtained was the result from 30 scans (2.5 s) combined. Original data (m/z) were treated (baseline subtraction, smoothing and centering) and analyzed by the MassLynx 4.0 software.

Enzyme assays

All enzymatic activities were measured at 37°C in a final volume of 1.0 mL. Isoforms of trypsin were assayed with the chromogenic synthetic substrate N, α -Benzoyl-p-Nitroanilide (BApNA) 10 mmol/L in dimethyl sulphoxide (DMSO) in 0.1 mol/L tris (hydroxymethyl) aminomethane buffer, pH 8.0, containing 20 mmol/L CaCl₂. (Erlanger et al., 1961).

Determination of active enzyme concentration

The concentration of active trypsin in the samples was determinated by active-site-titration with the chromogenic synthetic substrate NPGB (Chase and Shaw, 1967). The assay methodology underwent minor modifications, such as the used buffer being changed sometimes from Diethyl barbituric acid (Veronal) to tris (hydroxymethyl) aminomethane.

RESULTS AND DISCUSSION

In a classical paper (Schroeder and Shaw, 1968) SE-Sephadex-C50 matrix with buffer near neutrality was showed to provide a good method for separation of trypsin isoforms, but with low yield and low resolution between α - and β -trypsin isoforms. The initial goal of our work was to analytically study the conditions of the chromatographic processes described by Schroeder and Shaw and to try to develop new conditions to improve the separation of β - and α trypsin isoforms.

The procedure chosen to monitor the efficacy of the separation methods were: resolution among isoforms (R) and mass spectrometry for the determination of identity and purity of the trypsin isoforms.

Preliminary tests with the column

The first step was to decrease the flow rate of the chromatography due to excessive packing of stationary phase at the flow rate described by Schroeder and Shaw. This parameter was monitored by visual analysis (measurement of height variation of stationary phase during the process) and loss of peak symmetry.

The flow rate average of 290 μ L/min (Schroeder and Shaw, 1968) was divided by approximately 5 (60 μ L/min), 4 (70 μ L/min), 3 (100 μ L/min) and 2 (150 μ L/min) their chromatographic profiles were compared.

Preliminary results (data not shown) showed that flow rates of 60, 70 and 100 μ L/min caused small modifications in the level of stationary phase and in peak symmetry of α -and β -trypsin isoforms. But with a flow rate of 150 μ L/min, the modifications in the chromatographic profiles were remarkable (loss of peak symmetry, data not shown) and a significant column stationary phase packing was observed. Therefore, the initial working condition chosen was a method with a low flow rate of 60 μ L/min, aiming to allow an equilibration between adsorbing sites and the proteins.

Salt concentration dependence of $\beta\text{-}$ and $\alpha\text{-}$ trypsin separation

Trypsin is a protein that has a strong adsorption to SE-Sephadex and salt addition to the elution buffer is needed for deadsorption and elution in an isocratic mode. Different experimental conditions were tested aiming better resolution between β - and α -trypsin. The NaCl concentration in elution buffer was varied in the 90 – 150 mmol/L range. The main results are listed in Table 1.

Table 1 - Effect of salt concentration on chromatographic resolution. Conditions for the analyses were as follows: SE-Sephadex column, 85.0 x 2.2 cm (i.d), mobile phase 0.1 mol/L tris-HCl buffer, pH 7.69, 0.02 mol/L CaCl₂, 1.0 mmol/L benzamidine and NaCl; sample loading, 100 mg; flow rate of 60 μ L/min at 4°C. Experiments were performed in triplicate. SD refers to standard deviation.

performed in inplicate. DD fefers to standard de flation.			
Salt concentration (NaCl, mol/L)	Resolution (β - α trypsin)	SD	
0.090	0.42	0.01	
0.100	0.95	0.01	
0.125	0.81	0.01	
0.150	0.61	0.01	

The best results were obtained with a concentration of 100mmol/L NaCl. Runs made with NaCl concentrations of 125 and 150 mmol/L showed a decrease in resolution between α - and β -trypsin (Table.1). Runs made with a NaCl concentration of 90mmol/L were less efficient, due to a strong adsorption of the isoforms onto the matrix that were slowly deadsorptioned with a lower resolution. Other disadvantages of working with low salt concentration (smaller than 90

mmol/L NaCl) are a higher elution volume and a longer time for separation of isoforms. Thus, the best salt concentration for this separation was 100mmol/L NaCl.

Second flow rate test

Theoretically ideal chromatography operates slowly enough for complete equilibration between protein and matrix. In practice this is not possible; but diffusion effects must be minimized, and chromatographic time should be decreased (Scopes, 1996). Thus a fast flow rate can reduce the time for the chromatography experiment. However, it is preferable to start experiments with low flow rate increasing to high flow rate, to avoid the excessive packing of the stationary phase. Monitoring of packing was done by noticing the following parameters: shape of peaks and visual observation of stationary phase level variation. A flow rate of 60 μ L/min caused problems with diffusion effects and with long time of purification, thus larger flow rates were tested (100 –150 μ L/min).

The best chromatographic resolution was observed with a flow rate of 120 μ L/min, as listed in table.2. Flow rates of 100 and 110 μ L/min showed low resolution and chromatographic times are still unacceptable long.

Table 2 - Effect of flow rate on chromatographic resolution. Conditions for the analyses were as follows: SE - Sephadex column, 85.0 x 2.2 cm (i.d), mobile phase 0.1 mol/L tris-HCl, 0.02 mol/L CaCl₂, 1.0 mmol/L benzamidine and 0.1 mol/L NaCl, pH 7.69; sample loading, 100.0 mg. Runs were made at 4°C. Experiments were performed in triplicate. SD refers to standard deviation.

Flow rate (µL/min)	Resolution (β - α trypsin)	SD
100.0	1.05	0.01
110.0	1.10	0.01
120.0	1.28	0.01
130.0	1.17	0.02
140.0	1.08	0.01

With 130 and 140 µL/min, flow rate profiles were similar (data not shown), displaying a good separation between β - and α -trypsin isoforms (Table.2). Nevertheless, the flow rates of 130 and 140 µL/min caused packing of stationary phase of about 1.0 - 2.0 cm, while at 120 µL/min only small alterations were noticed in the level of matrix in column at the end of the chromatographic process. Chromatography with a flow rate of 120 µL/min showed better separation of trypsin isoforms. The retention time of β -trypsin changed from 12 days (at 60 µL/min) to about 3 days (at 120 µL/min) and the peaks became more symmetrical. A possible explanation for this phenomenon is that at moderate flow rates, the protein solution has an adequate time to equilibrate and adsorb to the ion exchanger. Fast flow rates can reduce peak resolution for some such as an: excessive matrix packing leading to a decrease in the number of theoretical plates resulting in low resolution among isoforms. Additionally, it decreases the time of interaction between protein and matrix

Influence of sample loading

Once the best flow rate and salt concentration were determined, it was necessary to investigate how much protein could bind to a given volume of matrix and also the loading capacity of the column for trypsin. Sample loadings tested were: 100 mg (3.33 mg/mL), 150 mg (5.0 mg/mL), 200 mg (6.6 mg/mL), 250 mg (8.3 mg/mL) and 300 mg (10.0 mg/mL) of commercial trypsin (Walsh and Wilcox, 1971). The influence of sample loading upon chromatographic resolution of β - and α -trypsin is shown in Table 3.

Table 3: Effect of loading capacity on chromatographic resolution. Conditions for the analyses were as follows: SE -Sephadex collumn, 85.0 x 2.2 cm (i.d), mobile phase 0.10 mol/L tris-HCl buffer, 0.02 mol/L CaCl₂, 1.0 mmol/L benzamidine and 0.10 mol/L NaCl, pH 7.69; flow rate 120 μ L/min at 4°C. Experiments were done in triplicate. SD refers to standard deviation.

Sample load (mg)	Resolution (β - α trypsin)	SD
65.0	1.27	0.01
80.0	1.28	0.01
100.0	1.28	0.02
150.0	1.16	0.02
200.0	1.03	0.01
250.0	0.86	0.02
300.0	0.62	0.01

Analyzing Table 3 it can be noticed that a sample loading of 100 mg results in acceptable resolution of individual trypsin isoforms (β - α). Loading 80 or 65 mg results in resolutions almost identical to the obtained when 100 mg are loaded. Thus, it is more advantageous to use 100 mg instead of 80 or 65 mg, for yield and time reasons. When sample loading is in the range of 150-300 mg, the resolution is worst, resulting in the obtention of greater amounts of impure B-trypsin (omitted data). At sample loading in the range of 150-250 mg of commercial trypsin it was noticed that the retention time decreased and peaks have lost their Gaussian shape, as typical of overloading. With values over 250 mg of commercial trypsin the peaks became totally flat and lost symmetry (Gooding and Schmuck, 1983). Thus, the best resolution was obtained with maximum sample loading of 100.0 mg of commercial trypsin.

Influence of pH in the chromatographic process

In the article of Schroeder and Shaw (Schroeder and Shaw, 1968) it was mentioned that "all pH adjustments were made at room temperature, and the values cited in this paper refer to such measurements regardless of the temperature of chromatography, which was often 2- 4 °C...".

All previous experiments in this paper were performed considering chromatographic temperature. The buffer used for chromatography was tris (hydroxymethyl) aminomethane and it has a dpK_a / dT= $-0.028/^{\circ}$ C (Beynon and Easterby, 1996). In pH range from 3 to 11 the change in proton concentration will usually be smaller compared to the concentration of buffer species, and the pH shift is to a first approximation, equal to the change in the pK_a (Beynon and Easterby, 1996). When solutions were adjusted at room temperature (25°C) to pH 7.10 and were used in chromatographic processes at 4 °C, as it was done by Schroeder and Shaw (Schroeder and Shaw, 1968), the pH shifted to 7.69. When the chromatographic process is conducted in pH 7.10 at 4°C, it leads to significant modifications in the chromatographic resolution, as can be seen in Fig.1 and Table 4.



Figure 1 - Effect of pH on the chromatography. The conditions were as follows: flow rate 120 μL/min, sample loading, 100 mg, mobile phase 0.1 mol/L tris-HCl buffer, pH 7.69 at 4 °C (O) and 7.10 at 4 °C (—), 0.02 mol/L CaCl₂ 1.0 mmol/L benzamidine and 100 mmol/L NaCl on the stationary phase SE-Sephadex. Fractions of 3.5 mL were collected. The reported pH values are the calculated ones at 4°C and the corresponding pH values at 25°C are 7.10 and 6.51, respectively.

Table 4 - Effect of pH on chromatographic resolution. Conditions for the analyses were as follows: SE-Sephadex column, 85.0 x 2.2 cm (i.d), mobile phase 0.1 mol/L tris-HCl buffer, 0.02 mol/L CaCl₂, 1.0 mmol/L benzamidine and 0.1 mol/L NaCl; sample loading, 100 mg; flow rate 120 μ L/min. The reported pH values are the ones at 4°C. Experiments were performed in triplicate. SD refers to standard deviation.

рН	Resolution (β - α trypsin)	SD
7.69	1.28	0.08
7.10	1.60	0.05

The change from pH 7.69 to 7.10 at 4°C in the stationary phase results in an increase in the retention of both β - and α - trypsins (Fig.1). This is due to the fact that the isoforms of trypsin are more protonated at pH 7.10 than at pH 7.69. Running the chromatography at pH 7.10 is a much better experimental condition, with higher resolution mainly for β -trypsin that is totally separated from α -trypsin, after about seven days (Fig.1 and Table.4). In order to investigate if ψ and α -trypsing separation could be improved at a pH smaller than 7.10, a run was made at pH 6.90. The resolution between β - and α -trypsins decreased to 1.47 and the retention time of β trypsin shifted to nine days; the resolution between Ψ - and α -trypsins did not show any significant improvement. Thus, the best condition for isolating ψ -trypsin is probably between pHs 6.90 and 7.10, but the separation between α - and ψ trypsin in a run performed at pH 7.10 was already satisfactory in comparison to previous results, yielding enough amounts of nearly pure proteins.

Besides, theses isoforms can be further purified by re-chromatography of these samples.

Reproducibility test

In order to test the reproducibility (precision) of the improved chromatographic process (0.1 mol/L tris-HCl, pH 7.10, 0.1 mol/L NaCl, 0.02 mol/L CaCl₂, 1.00 mmol/L benzamidine, sample loading of 100 mg of commercial trypsin and flow rate of 120 μ L/min at 4°C), ten consecutive runs were performed, without column regeneration and repacking for the next separation. As one can observed in Table 5 the maximum number of consecutive runs with acceptable resolution (resolution \geq 1.50 (Harris, 2001) were six.

After six runs the resolution dropped to 1.42 and β - and α -trypsin were not totally separated anymore. So, this column and method were standardized to operate at optimal conditions only for five consecutive runs.

Table 5 - Effect of reproducibility on the chromatographic resolution. Conditions for the analyses were as follows: SE-Sephadex column, 85.0 x 2.2 cm (i.d), mobile phase 0.10 mol/L tris-HCl buffer, 0.02 mol/L CaCl₂, 1.0 mmol/L benzamidine and 0.1 mol/L NaCl, pH 7.10; sample loading, 100 mg and flow rate of 120 μ L/min at 4°C. Experiments were performed in triplicate. SD refers to standard deviation.

Run test (Number)	Resolution (β - α trypsin)	SD
1	1.63	0.02
2	1.60	0.01
3	1.59	0.02
4	1.59	0.03
5	1.56	0.02
6	1.50	0.03
7	1.42	0.03
8	1.32	0.04
9	1.12	0.03
10	1.03	0.02

Molecular mass determination and purity

Molecular mass and purity of proteins were determined by electrospray mass spectrometry and results are given in Figs.2 and 3. These figures show the distribution patterns of ion peaks of

purified β - and α -trypsin isoforms. There is only one Gaussian distribution (Fig.2) with single peaks for β -trypsin profile (from 9+ to 19+). This result shows that β - trypsin is free of contaminants or other isoforms. Fig.3 shows the distribution patterns of ions peaks for α -trypsin. It shows small contaminating amounts of ψ -trypsin. Molecular mass values of β -, α - and ψ -trypsins were calculated by manual method in MassLynx[®] 4.0 software and the results were M (β) = 23,294.49 \pm 0.03 Da, M (α) = 23,312.07 \pm 0.01 Da and M (ψ) = 23,330.25 \pm 0.01 Da. It is important to notice that the difference between M (α) and M (β) is 17.58 Da due to the addition of one water molecule (18 Da) when β -trypsin is converted to α -trypsin. These values are in accordance with the values described by Ashton (Ashton et al., 1994). Thus, the identity and the purity of the isoforms were satisfactorily confirmed, validating our optimized method of chromatography.

Other characterization parameters of the improved chromatographic methodology

When 100 mg of commercial protein was applied to the column, under these optimized conditions, the recovery yield was about 85 mg of protein, of the total purified protein, 60 % is β -trypsin, 15 % is α -trypsin, 5 % is ψ - trypsin and the remaining 20 % is composed of minor isoforms (gama, delta and zeta) and other peptides.

In order to discover the active site concentration before and after the chromatography, commercial protein was dialyzed against 1.0 mmol/L HCl at 4° C with a dilution factor of 10^{6} times and assayed by active–site titration with NPGB (Scopes, 1996). The results were the following: 71.0 ± 2.0 % for commercial trypsin (before chromatography), 96.0 ± 1.5% for purified β -trypsin and 95.0 ± 1.8% for purified α - trypsin. These results show that, in the new optimized chromatographic process, autolysis is inhibited during the chromatography and the enzyme activity is kept high.

Determination of specific activities of commercial and purified trypsin isoforms was made using BApNA (Erlanger, et al., 1961), and the results are shown in fig.4.



Figure 2 - Mass spectrometry of purified β -trypsin. The conditions were: source (capillary = 3000 V, sample cone = 70 V, and extraction cone = 2 V) and ToF (flight tube = 2500 V and MCP detector = 5630 V). Analyzed spectrogram yielded an average mass for β - trypsin of 23,294.49 ± 0.03 Da.



Figure 3 - Mass spectrometry of purified α -trypsin. Experimental conditions are the same as in fig.2. Average mass of α - trypsin was 23,312.07 \pm 0.01 Da.



Figure 4 - Amidasic specific activity assay of commercial (1), β - (2), α - (3) and Ψ (4) trypsin isoforms. Experiments were performed in triplicate.

The results are in accordance to Foucault (Foulcault, et al., 1974a and Foulcault, et al., 1974b). The low specific activity found with commercial trypsin is due to factors unstabilizing the sample, as peptides inhibitors in the commercial trypsin preparation, storage time or storage at very low temperatures, possibly leading to cold denaturation.

These results showed that the enzyme isoforms were not modified during the process of separation. During all steps in the purification process the specific activity of the enzymes did not change significantly.

CONCLUSIONS

The optimized separation methodology of the main trypsin isoforms (β and α) by cationic chromatography developed in this work offers many quantitative and qualitative advantages when compared to previous methodologies using ionexchange or other chromatographic methods. This improved methodology, using 0.1 mol/L tris-HCl, 0.1 mol/L NaCl, 0.02 mol/L CaCl₂, 1.0 mmol/L benzamidine, pH 7.1 at 4°C with flow rate of 120 µL/min and sample loading of 100 mg of commercial trypsin, results in a chromatographic profile with total resolution between β - and α trypsins, with β -trypsin showing high purity and activity levels, while α - trypsin is partially pure, with insignificant amounts of contaminating Ψ trypsin. In addition, the improved methodology gives high yield of pure amounts of those enzymes at small purification time. Thus, the method proposed can be very useful in the routine of purification of trypsin isoforms which can be used in basic and applied research, for instance, largescale proteomic projects requiring extensive use of high-quality trypsinolysis for sample analysis.

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RESUMO

O propósito deste trabalho foi melhorar a separação e o rendimento das isoformas puras β - e α - tripsina por meio de cromatografia de troca iônica e caracterizar algumas propriedades físicoquímicas dessas isoformas. A purificação de isoformas de tripsina foi realizada em SE Sephadex, com tampão tris-HCl, pH 7,10 a 4°C. A quantidade de amostra, a concentração salina, o fluxo e o pH da fase móvel foram variados para determinar o efeito sobre a resolução da separação. A resolução foi otimizada principalmente entre βe α -tripsina, utilizando o pH 7.10 a 4°C. Isoformas puras foram obtidas a partir de 100 mg de tripsina comercial bovina depois de sete dias de cromatografia, fornecendo 51,0 mg de β-tripsina totalmente pura e 13,0 mg de α -tripsina parcialmente pura, com quantidades pequenas de contaminação por *v*-Tripsina. Assim, tempo e resolução da purificação foram otimizados redendo grandes quantidades de enzimas puras e ativas que são úteis em várias áreas de pesquisa e ciências biotecnológicas.

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